

**THERMODYNAMIC PROPERTIES OF  
LIQUEFIED PETROLEUM GASES**

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16. Abstract  The thermodynamic properties of several liquefied petroleum gases (with particular emphasis on propane) are discussed in detail. It is concluded that the widely used propane data by Stearns and George are too inconsistent and too inaccurate to be used for mass flow calculations of propane and propane mixtures through safety valves of rail tank cars. Accordingly, the thermodynamic properties of propane, propylene, n-butane, and a mixture of 65% (by mole) propane, 25% propylene, and 10% n-butane are recalculated using equations of states proposed by Benedict-Webb-Rubin (BWR) and by Starling. It is shown that Starling's equation results in thermodynamic properties which are more consistent and compare better with measured values than the BWR equation. Thermodynamic data for the four liquefied petroleum gases discussed above are calculated and presented in tabular form. In addition, predictions of pure propane mass flow rates (based upon isentropic), homogeneous equilibrium flow) are given. The influence of the thermodynamic data upon the predicted mass flow rates is demonstrated.		13. Type of Report and Period Covered  Interim Report 8-15-75 to 1-31-77
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## Preface

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## METRIC CONVERSION FACTORS

### Approximate Conversions to Metric Measures

Symbol	When You Know	Multiply by	To Find	Symbol
			<b>LENGTH</b>	
	inches	2.5	centimeters	cm
	feet	30	centimeters	cm
	yards	0.9	meters	m
	miles	1.6	kilometers	km
			<b>AREA</b>	
	square inches	6.5	square centimeters	cm <sup>2</sup>
	square feet	0.09	square meters	m <sup>2</sup>
	square yards	0.8	square meters	m <sup>2</sup>
	square miles	2.5	square kilometers	km <sup>2</sup>
	acres	0.4	hectares	ha
			<b>MASS (weight)</b>	
	ounces	28	grams	g
	pounds	0.45	kilograms	kg
	short tons (2000 lb)	0.9	tonnes	t
			<b>VOLUME</b>	
	teaspoons	5	milliliters	ml
	tablespoons	15	milliliters	ml
	fluid ounces	30	liters	l
	cups	2.4	liters	l
	pints	0.47	liters	l
	quarts	0.95	liters	l
	gallons	3.8	cubic meters	m <sup>3</sup>
	cubic feet	0.03	cubic meters	m <sup>3</sup>
	cubic yards	0.78	cubic meters	m <sup>3</sup>
			<b>TEMPERATURE (exact)</b>	
	Fahrenheit temperature	5/9 (after subtracting 32)	Celsius temperature	°C
			5/9 (then add 27)	
			Fahrenheit temperature	°F

### Approximate Conversions from Metric Measures

Symbol	When You Know	Multiply by	To Find	Symbol
			<b>LENGTH</b>	
	millimeters	0.04	inches	in
	centimeters	0.4	inches	in
	meters	3.3	feet	ft
	meters	1.1	yards	yd
	kilometers	0.6	miles	mi
			<b>AREA</b>	
	square centimeters	0.18	square inches	in <sup>2</sup>
	square meters	1.2	square yards	yd <sup>2</sup>
	square kilometers	0.4	square miles	mi <sup>2</sup>
	hectares (10,000 m <sup>2</sup> )	2.5	acres	ac
			<b>MASS (weight)</b>	
	grams	0.035	ounces	oz
	kilograms	2.2	ounces	oz
	tonnes (1000 kg)	1.1	short tons	t
			<b>VOLUME</b>	
	milliliters	0.03	fluid ounces	fl oz
	liters	2.1	pints	pt
	liters	1.06	quarts	qt
	liters	0.26	gallons	gal
	cubic meters	35	cubic feet	cu ft
	cubic meters	1.3	cubic yards	cu yd
			<b>TEMPERATURE (exact)</b>	
	°C	Celsius temperature	5/9 (then add 27)	
			Fahrenheit temperature	°F

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## Nomenclature

A	= Gibbs free energy
$\bar{A}$	= Residual work content, Btu/lb
$C_p$	= Constant pressure specific heat, Btu/lb-°F
$C_v$	= Constant volume specific heat, Btu/lb-°F
E	= Internal energy, Btu/lb
G	= Mass flux, lb/ft <sup>2</sup> -sec
$G_c$	= Critical mass flux, lb/ft <sup>2</sup> -sec
$g_c$	= Newton constant, 32.2 lb-ft/lbf-sec <sup>2</sup>
H	= Enthalpy, Btu/lb
J	= Mechanical to thermal energy conversion factor, 778 ft-lbf/Btu
K	= Slip ratio, $U_g/U_\ell$ , dimensionless
P	= Pressure, lbf/ft <sup>2</sup>
Q	= Heat added, Btu/ft <sup>2</sup> -sec
R	= Gas constant, 1.987 Btu/lb-mole-°R
S	= Entropy, Btu/lb-°F
$S_0$	= Stagnation entropy, Btu/lb-°F
$S_\ell$	= Liquid phase entropy, Btu/lb-°F
$S_g$	= Vapor phase entropy, Btu/lb-°F
$S_{eg}$	= Entropy of evaporation, Btu/lb-°F
T	= Temperature, °R
U	= Internal energy, Btu/lb
V	= Specific volume, ft <sup>3</sup> /lb
$W_g$	= Mass of gas phase, lb
$W_\ell$	= Mass of liquid phase, lb
X	= Quality, $X = W_g/(W_g + W_\ell)$ , dimensionless
$\alpha$	= Constant of state equation

### Nomenclature (Cont.)

$\rho$  = Density,  $\text{lb}/\text{ft}^3$

$\rho_g$  = Vapor phase density,  $\text{lb}/\text{ft}^3$

$\rho_l$  = Liquid phase density,  $\text{lb}/\text{ft}^3$

## Chapter 1. Executive Summary

The thermodynamic properties of propane, propylene, and n-butane and of a mixture consisting of 65% (by mole) propane, 25% propylene, and 10% n-butane were calculated using virial equations of state. The particular virial equations chosen for the calculations were those by Benedict-Webb-Rubin and by Starling. All experimental input into these semi-empirical equations was reevaluated using numerical techniques to achieve the best possible accuracy. Starling's equation results in thermodynamic properties which are most consistent and compare best with measured values. It was found that the widely used propane data by Stearns and George are too inconsistent and too inaccurate to be used for mass flow calculations of propane and propane mixtures. This report includes extensive saturation temperature tables for propane, propylene, n-butane, and a pseudo-fluid consisting of a mixture of propane, propylene, and n-butane which approximates commercial propane. While the Benedict-Webb-Rubin and the Starling equation were used for the calculation of the properties of pure propane and the respective results listed in separate tables, the results given for propylene, n-butane, and the hydrocarbon mixture are based on Starling's equation. Thermodynamic data of pure propane in the compressed liquid region were calculated and are given in extensive tables. Temperature-entropy diagrams for propane, propylene, and n-butane based on Starling's equation of state were constructed. In addition, predictions of pure propane mass flow rates based upon isentropic, homogeneous equilibrium flow are given. To demonstrate the importance of accuracy and consistency of the thermodynamic data, the mass flow rate prediction calculations were performed twice, once using the propane data as reported by Stearns and George, and one using calculated propane properties based on Starling's equation.

## Chapter 2. Introduction

The flow of commercial propane through safety valves is being studied at the University of Maryland under the sponsorship of the Department of Transportation. The aim of this study is to provide industry and the Department of Transportation with accurate valve sizing equations or charts. The program includes interpretation and evaluation of already completed full scale propane flow tests and future active participation of full scale propane flow tests. The main thrust of the Safety Valve Study at the University of Maryland, however, is the formulation of valve sizing equations and their verification.

The flow rate prediction of propane through safety valves is very complex because of three fundamentally different reasons:

1. Two-phase flow occurs during the discharge of the propane (most of the existing fluid flow prediction equations are only valid for one-phase flow).
2. The thermodynamic data of commercial propane are at present not known with sufficient accuracy to give reasonably accurate flow-rate predictions based on homogeneous flow.
3. The flow path (stream line picture) through a safety valve is very complex and its influence on the mass flow rates for a given pressure gradient across the valve will vary with the different two-phase flow regimes.

The different two-phase flow regimes which may occur are vapor flow, mist and spray flow, bubble and slug flow, annular flow, liquid flow, and flashing flow. The establishing of the particular flow regime which will govern the maximum possible mass discharge through the safety valve is dependent upon the individual accident condition; e.g., the position of the safety valve, the rate of heat input into the tank car, the amount of propane in the tank car, etc.

Any mathematical description of flow of real fluid includes the continuity equation, the momentum equation, the energy equation, and the equation of state of the fluid. Without an accurate equation of state, correct modeling of the flow, such as predicting the mass flow rates is not possible. During

the early part of the investigation of propane flow through safety valves a lack of accurate and consistent thermodynamic data of propane was found to exist. This lack of data prompted the study which is described in this report.

## Chapter 3. Thermodynamic Properties of Propane

### 3.0 Background and Development of Virial Equations of State

The first systematic investigation of the thermodynamic properties of propane is that by Dana et al (6) in 1926. Dana et al (6) made vapor pressure measurements and published pressure-temperature tables for the saturated liquid and saturated vapor of propane. Since then, a number of researchers have made additional contributions in this field. Among them, Sage, Schaafsma, and Lacey (8) and Burgoyne (5) published the pressure-volume-temperature relations and thermal properties such as enthalpy and internal energy of propane. Beattie, Kay and Kaminsky (2) made additional P-V-T measurements. Beattie, Poffenberger, and Hadlock (3) measured the critical constants ( $T_c$  and  $P_c$ ) of propane. Stearns and George (10) summarized all of the above and other available experimental data in 1943. To this date, the thermodynamic tables and diagrams by Stearns and George (10) are the most often referenced propane data. This data, however, will lead to large inconsistent fluctuation in calculated mass flow rates as is discussed in Chapter 4. For this reason, it was necessary to find or develop a more accurate equation of state for propane. Two semi-empirical equations of state for propane were found in the literature and were further investigated in detail in this study, namely, the Benedict - Webb-Rubin (B-W-R) equation (4) and Starling's (9) equation. Starling's work is essentially an extension of the approach taken by Benedict et al. The above two semi-empirical equations are virial equations in which the virial coefficients are obtained by determining the deviation between the Helmholtz free energy of the real gas and that of an ideal gas. The introduction of empirical data requires curve fitting of this data which significantly influences the consistency of the calculated thermodynamic values. For this reason, both the calculations of B-W-R and that of Starling's were repeated, improved and expanded. A discussion of the development of the B-W-R equation of state is given in the following paragraph.

The work content, also known as the Helmholtz free energy or the Gibb's  $\psi$ -function, is related to the internal energy E, the absolute temperature T, and the entropy S by the equation

$$A = E - TS \quad (3-1)$$

The residual work content  $\bar{A}$  is defined as the difference between the work

content of a mole of hydrocarbons at molar density  $\rho$ , absolute temperature  $T$  and its work content in the hypothetical ideal gas state at the same density and temperature. The residual work content is defined by

$$\bar{A} = A - RT \ln \rho - \lim_{\rho \rightarrow 0} (A - RT \ln \rho) \quad (3-2)$$

The above equation is considered as a fundamental equation because a number of thermodynamic properties of the medium may be computed from it. For instance, an equation of state in which the pressure  $P$  is expressed as a function of the density and temperature may be obtained by the relation:

$$P = \rho RT + \rho^2 \left[ \frac{\partial \bar{A}}{\partial \rho} \right]_T \quad (3-3)$$

Ursell (11) and Mayor (7) showed that the residual work content  $\bar{A}$  of a stable gas can be expressed by the series:

$$\bar{A} = Q_1(T)\rho + Q_2(T)\rho^2 + \dots \quad (3-4)$$

where  $Q_1$  and  $Q_2$  are functions of the temperature.

In developing the equation of state, attention was first directed to the constant density line (isometrics) when the quantity  $(P - \rho RT)/\rho^2$  is plotted against temperature; these isometrics are very nearly straight lines. It was found that for most hydrocarbons including propane the isometrics could be represented by an equation of the form:

$$(P - \rho RT)/\rho^2 = RTB(\rho) - A(\rho) - C(\rho)/T^2 \quad (3-5)$$

where  $A$ ,  $B$ , and  $C$  are functions of density.  $B(\rho)$  in turn could be represented by the simple linear equation:

$$B(\rho) = B_0 + b\rho \quad (3-6)$$

The plots of  $A(\rho)$  and  $C(\rho)$  against density, however, showed marked curvature;  $A(\rho)$  was represented by an equation of the form

$$A(\rho) = A_0 + a\rho(1 - \alpha\rho^3) \quad (3-7)$$

and  $C(\rho)$  by an equation of the form:

$$C(\rho) = C_0 - c\rho(1 + \gamma\rho^2) \exp(-\gamma\rho^2) \quad (3-8)$$

When the expressions (3-5), (3-6), (3-7), and (3-8) are combined, the equation of state is obtained. The equation of state is

$$\begin{aligned} P &= \rho RT + \rho^2 RT(B_0 + \rho b) - (A_0 + a\rho + a\alpha\rho^4) \\ &\quad + (1/T^2)(C_0 - c\rho(1 + \gamma\rho^2) \exp(-\gamma\rho^2)) \end{aligned} \quad (3-9)$$

or

$$\begin{aligned} P &= \rho RT + (B_0 RT - A_0 - C_0/T^2)\rho^2 + (bRT - a)\rho^3 \\ &\quad + a\alpha\rho^6 + \frac{c\rho^3(1 + \gamma\rho^2) \exp(-\gamma\rho^2)}{T^2} \end{aligned} \quad (3-10)$$

The numerical values of the parameters  $A_0$ ,  $B_0$ ,  $C_0$ ,  $a$ ,  $b$ ,  $c$ ,  $\alpha$ , and  $\gamma$  can be determined from experimental P-V-T data. Benedict-Webb-Rubin (4) describe at length the manner in which this is done; Table 3-1a gives a listing of these values for the B-W-R equation.

An equation of state similar to the B-W-R equation was recently developed by Starling (9). Starling's equation of state has more virial coefficients and, according to its author, is more accurate than B-W-R equation in the liquid region. Corresponding to the coefficients of the B-W-R equation, Starling gives the following equation of state for hydrocarbons:

$$\begin{aligned} P &= \rho RT + \left( B_0 RT - A_0 - \frac{C_0}{T^2} + \frac{D_0}{T^3} - \frac{E_0}{T^4} \right) \rho^2 \\ &\quad + \left( bRT - a - \frac{d}{T} \right) \rho^3 + \alpha \left( a + \frac{d}{T} \right) \rho^6 \\ &\quad + \frac{c^3}{T^2} (1 + \gamma\rho^2) \exp(-\gamma\rho^2) \end{aligned} \quad (3-11)$$

The coefficients of the above equation as derived by Starling are given in Table 3-1b.

### 3.1 Thermodynamic Properties of Pure Propane

Thermodynamic properties such as enthalpy, entropy, etc. of a pure substance can be derived from an equation of state of the substance which relates pressure, volume, and temperature by means of Maxwell's relations. Thermodynamic properties of primary importance in flow predictions are specific volume (or density), enthalpy, entropy, and specific heat in addition to temperature and pressure. The derivation of these properties are discussed in detail below for both the B-W-R equation and the equation of state proposed by K. E. Starling.

#### 3.1.1 Density

The B-W-R equation is written as

$$P = \rho RT + \left[ B_0 RT - A_0 - \frac{C_0}{T^2} \right] \rho^2 + (bRT - a)\rho^3 + a\alpha\rho^6 + \frac{C_p^3}{T^2} (1 + \gamma\rho^2) \exp(-\gamma\rho^2) \quad (3-12)$$

Similarly, Starling's equation is of the form

$$P = \rho RT + \left[ B_0 RT - A_0 - \frac{C_0}{T^2} + \frac{D_0}{T^3} - \frac{E_0}{T^4} \right] \rho^2 + (bRT - a - \frac{d}{T})\rho^3 + \alpha(a + \frac{d}{T})\rho^6 + \frac{C^3}{T^2} (1 + \gamma\rho^2) \exp(-\gamma\rho^2) \quad (3-13)$$

The density  $\rho$  can only be obtained by an iterative procedure. It should be pointed out that the derivative of pressure with respect to density in the liquid phase is extremely large so that a very slight change in liquid density can cause a dramatic change in pressure of the liquid phase. It was found that in order to match the calculated values of the liquid pressure with those given by Starling (9), more than the significant figures given by Starling's tabulated values of liquid density are required. In other words, when the values of temperature and liquid density tabulated by Starling in reference (9) are substituted into his equation of state, the calculated pressure values do not agree with the tabulated pressures (see Figure 3-1). Instead,

if the values of the liquid density which were computed using 18 significant figures are used to compute the corresponding pressures for any given temperature and density, the values of computed and tabulated pressures are in close agreement. Two additional curves were plotted in Figure 3-1 to show the sensitivity of  $dP/d\rho$  liquid. Curves (1) and (2) were constructed using the values of liquid pressure calculated from saturation temperatures and specific volume values which were either slightly smaller or slightly larger than those tabulated by Starling, i.e., ( $V - 0.00005$ ) and ( $V + 0.00004$ ). Figure 3-1 shows the effect of the significant figures of liquid density on the pressure values. The great difference in calculated saturation pressure due to the small variation in liquid density (+0.00004 or -0.00005) is very significant, since all the thermodynamic properties required for critical mass flow rate predictions are functions of temperature and pressure. The fluctuations in maximum flow rate predictions which are obtained by using Stearns and George's thermodynamic data (see Chapter 4) is in part due to the lack of accuracy in density which also influences other thermodynamic properties. Since thermodynamic properties are tied to density predictions, poor accuracy in the density prediction will cause inaccuracies in calculating enthalpy, entropy, and specific heat values. It was found that inaccuracies of thermodynamic properties were magnified when mass flow rates were computed.

### 3.1.2 Enthalpy

The enthalpy of a real substance (e.g., Propane) at any temperature and pressure can be obtained from the relation

$$H = (H - H^0) + (H^0 - H_0^0) + H_0^0 \quad (3-14)$$

where  $H_0^0$  is the standard enthalpy of formation of that substance from the elements (i.e., carbon and hydrogen) at 0°R and 0 psia.  $(H^0 - H_0^0)$  is the difference in the enthalpy of the substance in the ideal gas state at the temperature of interest and the enthalpy of the reference state of 0°R.  $(H - H^0)$  is the enthalpy departure, that is, the difference in the enthalpy of the substance at the temperature and pressure of interest and the enthalpy of the substance in the ideal gas state at the same temperature. From classic thermodynamics, one can write

$$\begin{aligned} dH &= TdS + VdP \\ &= T \left[ \left( \frac{\partial S}{\partial P} \right)_T dP + \left( \frac{\partial S}{\partial T} \right)_P dT \right] + VdP \end{aligned} \quad (3-15)$$

Applying the Maxwell's relation

$$\left( \frac{\partial S}{\partial T} \right)_P = \frac{C_p}{T} \quad (3-16)$$

results in

$$dH = d(PV) + \left[ T \left( \frac{\partial P}{\partial T} \right)_V - P \right]_T dV \quad (3-17)$$

Integrating yields

$$H - H^0 = \frac{P}{\rho} - RT + \int_0^\rho \left[ P - T \left( \frac{\partial P}{\partial T} \right)_P \right]_T \frac{dp}{\rho^2} \quad (3-18)$$

Substituting the B-W-R equation of state into equation (3-1) results in

$$\begin{aligned} H - H^0 &= \left[ B_0 RT - 2A_0 - 4 \frac{C_0}{T^2} \right] \rho + \frac{1}{2} \left[ 2bRT - 3a \right] \rho^2 \\ &\quad + \frac{6}{5} \alpha a \rho^5 + \frac{c}{\gamma T^2} \left[ 3 - \left( 3 + \frac{1}{2} \gamma \rho^2 - \gamma^2 \rho^4 \right) \exp(-\gamma \rho) \right] \end{aligned} \quad (3-19)$$

Likewise, by substituting Starling's equation of state to equation (3-1), the following expression is obtained:

$$\begin{aligned} (H - H^0) &= \left[ B_0 RT - 2A_0 - \frac{4C_0}{T^2} + \frac{5D_0}{T^3} - \frac{6E_0}{T^4} \right] \rho \\ &\quad + \frac{1}{2} \left[ 2bRT - 3a - \frac{4d}{T} \right] \rho^2 + \frac{1}{5} \alpha \left( 6a + \frac{7d}{T} \right) \rho^5 \\ &\quad + \frac{c}{T^2} \left[ 3 - \left( 3 + \frac{1}{2} \gamma \rho^2 - \gamma^2 \rho^4 \right) \exp(-\gamma \rho^2) \right] \end{aligned} \quad (3-20)$$

The differences between the enthalpy of propane in the ideal gas state at the temperature of interest and the enthalpy at the reference state of 0°C ( $H^0 - H_0^0$ ) are given in reference (1) as a function of temperature. Since

$dH = dQ + VdP$ , the change in enthalpy during an isobaric process is equal to the heat that is transferred. That is,

$$H^0 - H_0^0 = Q \quad (3-21)$$

or

$$H^0 - H_0^0 = \int_i^f C_p dT \quad (3-22)$$

The data given by reference (1) are tabulated values over a range of temperatures. In order to obtain values between these tabulated values, curve-fitting becomes necessary. The degree of the polynomial chosen for curve-fitting strongly influences the accuracy of the finally computed enthalpies. Figure 3-2a shows the data points of  $(H^0 - H_0^0)$  (see reference (1)) and a third order polynomial curve-fitting. As a general rule of curve-fitting, as long as the predicted values do not start to oscillate, the higher the degree of polynomial, the better the curve-fitting. It was found that a ninth order curve-fitting is necessary in order to obtain a consistent prediction of the maximum mass flux of propane. The ninth order curve-fitting of  $(H^0 - H_0^0)$  is shown on Figure 3-2b. It is difficult to visually detect an improvement in going from a third degree polynomial to a 9th degree polynomial. Yet the effect of the degree of polynomial used in curve-fitting upon maximum mass flow rate is very severe.

The equation representing the ninth order polynomial is

$$H^0 - H_0^0 = \sum_{n=1}^{N=9} C_e(n) P(n)(T)$$

with  $P_0 = 0$

$$P_1 = 1.0$$

$$P_{(j)}(T) = T P_{(j-1)}(T) - \alpha_{e(j-1)} P_{(j-1)} - \beta_{e(j-1)} P_{(j-2)}$$

where  $j = 2, 3, \dots, N$ .

The numerical values of  $\alpha_{e(j-1)}$ ,  $\beta_{e(j-1)}$ ,  $C_{e(n)}$ , and  $H_0^0$  are given in Table 3-2.

### 3.1.3 Entropy

Gibbs' function is defined by

$$A = U - TS \quad (3-23)$$

The work content of a gaseous state may be obtained from the equation of state by the relation

$$A = RT \ln \rho RT + E_0 - TS_0 + \int_0^\rho \left[ \frac{P - \rho RT}{\rho^2} \right] d\rho \quad (3-24)$$

The first three terms represent the work content of an ideal gas at the density and temperature of the actual condition.  $E_0$  and  $S_0$  are, respectively, the internal energy and the entropy of one mole of the substance in the ideal gas state at unit pressure. The integral represents the difference between the work content of the actual compound and that of an ideal gas.

Entropy is related to the work content by the following expression:

$$S = -(\partial A / \partial T)_{\rho, x} \quad (3-25)$$

Substituting equation (3-24) into (3-25) yields

$$S = S_0 - R \ln(\rho RT) - \int_0^\rho \left[ -\rho R + \left( \frac{\partial P}{\partial T} \right)_\rho \right] \frac{d\rho}{\rho^2} \quad (3-26)$$

and finally

$$S - S_0 = -R \ln(\rho RT) + \int_0^\rho \left[ \rho R - \left( \frac{\partial P}{\partial T} \right)_\rho \right] \frac{d\rho}{\rho^2} \quad (3-27)$$

when the B-W-R equation of state is employed, the following equation is obtained

$$\begin{aligned} S - S_0 &= -R \ln \rho RT - \left( B_0 R + 2 \frac{C_0}{T^3} \right) \rho \\ &\quad - \frac{bR\rho^2}{2} + \frac{2C_p^2}{T^3} \left[ \frac{1 - e^{-(\gamma\rho)^2}}{\gamma\rho^2} - \frac{e^{-\gamma\rho^2}}{2} \right] \end{aligned} \quad (3-28)$$

where  $S - S_0$  is often called "entropy departure."

A parallel development for Starling's equation gives

$$S - S_0 = -R \ln pRT - \left[ B_0 R + \frac{2C_0}{T^3} - \frac{3D_0}{T^4} + \frac{4E_0}{T^5} \right] p - \frac{1}{2} \left( bR + \frac{d}{T^2} \right) p^2 + \frac{\alpha p^5 d}{5T^2} + \frac{2C}{\gamma T^3} \left[ 1 - \left( 1 + \frac{1}{2} \gamma p^2 \right) \exp(-\gamma p^2) \right]. \quad (3-29)$$

The entropies of propane in the ideal gas state at unit pressure and various temperatures are given in reference (1); this report contains most of the available experimental thermodynamic data on hydrocarbons in the literature up to the year of 1952. Similar to the polynomial curve-fitting for enthalpy departure, the entropy departure of propane is fitted to polynomials ranging from the second order to the ninth order. Figure 3-3a shows the data points obtained from reference (1) and a third order polynomial curve-fitting, while Figure 3-3b gives the finally chosen ninth order polynomial representing  $(S_0 - S_0^0)$  values.

The equation representing  $(S_0 - S_0^0)$  is

$$S_0 - S_0^0 = \sum_{n=1}^{N=9} C_{e(n)} P_{(n)}(T) \quad (\text{Btu/lb-moles } ^\circ\text{F})$$

with  $P_1(T) = 1.0$

$$P_j(T) = T P_{(j-1)}(T) - \alpha_{e(j-1)} P_{(j-1)} - \beta_{e(j-1)} P_{(j-2)}$$

where  $j = 2, 3, \dots, N$

The numerical values of  $\alpha_{e(j-1)}$ ,  $\beta_{e(j-1)}$ ,  $C_{e(n)}$  are given in Table 3-b.

### 3.1.4 Heat Capacity

From classical thermodynamics, the following relations are obtained:

$$\left[ \frac{\partial S}{\partial T} \right]_V = \frac{C_V}{T} \quad (3-30)$$

$$dS = - \left[ \frac{\partial V}{\partial T} \right]_P dP + \frac{C_P}{T} dT \quad (3-31)$$

Going through a proper limiting process yields

$$\left(\frac{\partial S}{\partial T}\right)_V = - \left(\frac{\partial V}{\partial T}\right)_P \left(\frac{\partial P}{\partial T}\right)_V + \frac{C_p}{T} \quad (3-32)$$

Combining with equation (3-30), and then substituting for  $(\partial P/\partial T)_V$  according to

$$\left(\frac{\partial Z}{\partial X}\right)_Y = - \left(\frac{\partial Y}{\partial X}\right)_Z \left(\frac{\partial Z}{\partial Y}\right)_X = - \frac{(\partial Y/\partial X)_Z}{(\partial Y/\partial Z)_X}$$

gives

$$(C_p - C_v) = T \left(\frac{\partial V}{\partial T}\right)_P \left(\frac{\partial P}{\partial T}\right)_V = -T \left(\frac{\partial V}{\partial T}\right)_P^2 \left(\frac{\partial P}{\partial V}\right)_T \quad (3-33)$$

The specific heat departure  $(C_p - C_p^*)$  can be estimated as follows:

$$C_p - C_p^* = C_p - C_v^\infty - R \quad (3-34)$$

or

$$C_p - C_p^* = (C_p - C_v) + (C_v - C_v^\infty) - R \quad (3-35)$$

where  $C_p^*$  is the specific heat of the gas exhibiting ideal gas behavior

$C_p$  is constant pressure heat capacity of the real gas

$C_v$  is the constant volume heat capacity of the real gas

$C_v^\infty$  is the constant-volume specific heat at zero pressure or infinite volume of the real gas.

Relations for  $C_p - C_v$  and  $C_v - C_v^\infty$  in terms of the equation of state may be developed from the following relationships:

$$C_p - C_v = -T \left(\frac{\partial P}{\partial T}\right)_V^2 / \left(\frac{\partial P}{\partial V}\right)_T \quad (3-36)$$

$$\left(\frac{\partial C_v}{\partial V}\right)_T = T \left(\frac{\partial^2 P}{\partial T^2}\right)_V \quad (3-37)$$

$$C_v - C_v^\infty = \Delta(C_v)_T = \int_{\infty}^V \left(\frac{dC_v}{dV}\right)_T dV \quad (3-38)$$

Combining equations (3-34), (3-35), and (3-36) gives

$$C_p - C_p^* = \frac{-T \left( \frac{\partial P}{\partial T} \right)_V^2}{\left( \frac{\partial P}{\partial V} \right)_T} + \int_V^\infty \left( \frac{\partial C_V}{\partial V} \right)_T dV - R \quad (3-39)$$

$$= \frac{-T \left( \frac{\partial P}{\partial T} \right)_V^2}{\left( \frac{\partial P}{\partial V} \right)_T} + \int_V^\infty \left( \frac{\partial^2 P}{\partial T^2} \right)_V dV - R \quad (3-40)$$

Applying the B-W-R equation of state results in

$$\begin{aligned} C_p - C_p^* &= -R + \frac{6C_0}{T^3} \rho + \frac{6C}{T^3 \gamma} \left( e^{-\gamma \rho^2} - 1 \right) + \frac{3C}{T^3} \rho^2 e^{-\gamma \rho^2} \\ &\quad + \frac{T \left[ R + \left( B_0 R + \frac{2C_0}{T^3} \right) \rho + (bR\rho^2) - \frac{2C_0^2}{T^3} (1 + \gamma \rho^2) \exp(-\gamma \rho^2) \right]^2}{\text{denominator}} \end{aligned} \quad (3-41)$$

where the denominator is

$$\begin{aligned} &\{RT + 2\rho \left( B_0 RT - A_0 - \frac{C_0}{T^2} \right) + 3\rho^2 (bRT - a) \\ &\quad + 6a\rho^5 + \frac{C_0^2}{T^2} (3 + 3\gamma^2 \rho - 2\gamma^2 \rho^4) \exp(-\gamma \rho^2)\} \end{aligned}$$

When employing Starling's equation, the specific heat departure becomes

$$\begin{aligned} C_p - C_p^* &= -R + \left[ \frac{6C_0}{T^3} - \frac{12D_0}{T^4} - \frac{20E_0}{T^5} \right] \rho + \frac{d}{T^2} \rho^2 \\ &\quad + \frac{2}{5} \frac{\alpha d}{T^2} \rho^5 + \frac{6C}{\gamma T^3} \left( e^{-\gamma \rho^2} - 1 \right) + \frac{3C}{T^3} \rho^2 e^{-\gamma \rho^2} + (\bar{P}) \end{aligned} \quad (3-42)$$

where  $(\bar{P})$  is

$$\frac{T \left[ R + \rho \left( B_0 R + \frac{2C_0}{T^3} - \frac{3D_0}{T^4} + \frac{4E_0}{T^5} \right) + \rho^2 \left( bR + \frac{d}{T^2} \right) - \frac{\alpha d \rho^5}{T^2} - \frac{2C_0^2}{T^3} (1 + \gamma \rho^2) \exp(-\gamma \rho^2) \right]^2}{\text{denominator}}$$

where the denominator is

$$\begin{aligned} & \left\{ RT + 2 \left[ B_0 RT - A_0 - \frac{C_0}{T^2} + \frac{D_0}{T^3} - \frac{E_0}{T^4} \right] \rho + 3\rho^2 \left[ bRT - a - \frac{d}{T} \right] \right. \\ & \quad \left. + 6\alpha\rho^2 \left( a + \frac{d}{T} \right) + \frac{C_p^2}{T^2} (3 + 3\gamma\rho^2 - 2\gamma^2\rho^4) \exp(-\gamma\rho^2) \right\} \end{aligned}$$

Experimentally found values for the heat capacity  $C_p^*$  are given in reference (1); again, curve fitting was employed to make interpolation between the given data points possible. The results of the third and ninth order polynomial curve-fitting of the reference value  $C_p^*$  are shown in Figures 3-4a and b. The final equation adapted to represent the specific heat of propane exhibiting ideal gas behavior is the ninth order polynomial of the form

$$C_p^*(T) = \sum_{n=1}^N C_{e(n)} P_n(T) \quad (\text{Btu/lb-mole-}^\circ\text{F})$$

with  $P_0(T) = 0$

$$P_1(T) = 1.0$$

$$\text{and } P_j(T) = T P_{(j-1)}(T) - \alpha_{e(j-1)} P_{(j-1)} - \beta_{e(j-1)} P_{(j-2)}$$

where  $j = 2, 3, 4, \dots, N$

The numerical values of the coefficients  $\alpha_{e(j-1)}$ ,  $\beta_{e(j-1)}$ , and  $C_{e(n)}$  are given in Table 3-4.

Tables 5 and 6 give the thermodynamic properties of pure propane as obtained from the B-W-R equation and Starling's equation, respectively. The calculations for these two equations were extended into the subcooled region. To make a comparison easier, a listing of the already existing data by Stearns and George is also given (see Table 3-7). Figure 3-5, 3-6, and 3-7 are temperature-entropy diagrams for pure propane as obtained from the B-W-R equation, Starling's equation, and Stearns and George's data, respectively.

### 3.1.5 Fugacity

It is seen that the saturation temperatures and pressures of these three tables are different from one another. The saturation temperatures and their corresponding saturation pressures given by Stearns and George are the measured values while those by Benedict-Webb-Rubin and by Starling are the

predicted values. It is known from thermodynamics, that at saturation conditions the following two conditions must be satisfied.

$$P(\rho_\ell, T) = P(\rho_g, T) = P \quad (3-42)$$

and

$$f(\rho_\ell, T) = f(\rho_g, T) = f \quad (3-43)$$

The procedure adopted in calculating the saturation pressure for a given saturation temperature is as follows: For a chosen saturation temperature, guess a saturation pressure  $P$ . Apply the equation of state (B-W-R or Starling's equation of state) to calculate the density ratio  $\rho_\ell/\rho_g$ . Substituting the values of  $T$  and  $\rho$  into the appropriate equation relating fugacity  $f$  to  $T$  and  $\rho$ , one obtains the value of  $f_\ell/f_g$ . The new value of pressure for this iterative calculation is the product of the first guessed  $P$  and the fugacity ratio ( $f_\ell/f_g$ ). The calculation continues until the value of  $P$  converges. The expression for the fugacity for Starling's equation is

$$\begin{aligned} RT \ln f &= RT \ln(R\rho T) + 2 \left( B_0 RT - A_0 - \frac{C_0}{T^2} + \frac{D_0}{T^3} - \frac{E_0}{T^4} \right) \rho \\ &\quad + \frac{3}{2}(bRT - a - \frac{d}{T})\rho^2 + \frac{6\alpha}{5}(a + \frac{d}{T})\rho^5 \\ &\quad + \frac{C}{\gamma T^2} [1 - (1 - \frac{1}{2}\gamma\rho^2 - \gamma^2\rho^4) \exp(-\gamma\rho^2)] \end{aligned} \quad (3-44)$$

The corresponding expression for the B-W-R equation is

$$\begin{aligned} RT \ln f &= RT \ln(\rho RT) + 2 \left( B_0 RT - A_0 - \frac{C_0}{T^2} \right) \rho + \frac{3}{2}(bRT - a)\rho^2 \\ &\quad + \frac{6}{5}\alpha\rho^5 + \frac{C}{\gamma T^2} [1 - (1 - \frac{1}{2}\gamma\rho^2 - \gamma^2\rho^4) \exp(-\gamma\rho^2)] \end{aligned} \quad (3-45)$$

The saturation pressure predictions of Starling's equation are much closer to measured values than the predictions by the B-W-R equation of state.

### 3.2 Thermodynamic Properties of Commercial Propane (A Mixture of Propane, Propylene, and N-Butane)

Commercial grade propane has a minimum purity of 65 percent by mole of propane. The major component of the impurities are propylene and butane.

Although the purity may vary from lot to lot, the typical composition of the commercial or industrial grade propane is of 65% propane, 25% propylene, and 10% butane.

The Benedict-Webb-Rubin and the Starling's equation of state for multi-component mixtures are of the same form as that for the single component case.

The coefficients of Benedict-Webb-Rubin's equation of state for propane mixtures are

$$B_0 = \left[ \sum_i X_i B_{0i} \right] \quad (3-46)$$

$$A_0 = \left[ \sum_i (X_i A_{0i}^{1/2}) \right]^2 \quad (3-47)$$

$$C_0 = \left[ \sum_i (X_i C_{0i}^{1/2}) \right]^2 \quad (3-48)$$

$$b = \left[ \sum_i (X_i b_i^{1/3}) \right]^3 \quad (3-49)$$

$$a = \left[ \sum_i (X_i a_i^{1/3}) \right]^3 \quad (3-50)$$

$$c = \left[ \sum_i (X_i c_i^{1/3}) \right]^3 \quad (3-51)$$

$$\alpha = \left[ \sum_i (X_i \alpha_i^{1/3}) \right]^3 \quad (3-52)$$

$$\gamma = \left[ \sum_i (X_i \gamma_i^{1/2}) \right]^2 \quad (3-53)$$

The additional coefficients for Starling's equation are

$$D_0 = \sum_i \sum_j X_i X_j D_{0i}^{1/2} D_{0j}^{1/2} \quad (3-54)$$

$$E_0 = \sum_i \sum_j X_i X_j E_{0i}^{1/2} E_{0j}^{1/2} \quad (3-55)$$

$$d = \left[ \sum_i X_i d_i^{1/3} \right]^3 \quad (3-56)$$

where i and j are indices for the components and the summations range from

$i = 1$  to  $i = n$  and  $j = 1$  to  $j = n$ , with  $n$  being the total number of components.  $x_i$  is the molar fraction of the  $i$ th component of the mixture. The propane mixture thermodynamic property calculation using both the B-W-R and Starling's equation of state are discussed below.

The enthalpy of a propane mixture can be written as

$$H = \left[ H - \sum_{i=1}^n x_i H_i^0 \right] + \sum_{i=1}^n (H_i^0 - H_0^0) x_i + \sum_{i=1}^n H_0^0 x_i \quad (3-57)$$

where  $\left( H - \sum_{i=1}^n x_i H_i^0 \right)$  is the enthalpy departure of the mixture.

Applying the B-W-R equation,  $H - \sum_{i=1}^n x_i H_i^0$  becomes

$$\begin{aligned} \left( H - \sum_{i=1}^n x_i H_i^0 \right) &= \left( B_0 RT - 2A_0 - \frac{4C_0}{T^2} \right)_p + \left( 2bRT - 3a \right)_p \frac{\rho^2}{2} \\ &\quad + \frac{6a\alpha\rho^5}{5} + \frac{C_p^2}{T^2} \left[ 3 \frac{(1 - \exp(-\gamma\rho^2))}{\gamma\rho^2} \right. \\ &\quad \left. - \frac{\exp(-\gamma\rho^2)}{2} + \gamma\rho^2 \exp(-\gamma\rho^2) \right] \end{aligned} \quad (3-58)$$

The corresponding expression using Starling's equation of state is

$$\begin{aligned} \left( H - \sum_{i=1}^n x_i H_i^0 \right) &= \left( B_0 RT - 2A_0 - \frac{4C_0}{T^2} + \frac{5D_0}{T^3} - \frac{6E_0}{T^4} \right)_p \\ &\quad + \frac{1}{2} \left( 2bRT - 3a - \frac{4d}{T} \right)_p \frac{\rho^2}{2} + \frac{1}{5} \alpha \left( 6a + \frac{7d}{T} \right) \rho^5 \\ &\quad + \frac{C_p^2}{\gamma T^2} \left[ 3 - \left( 3 + \frac{1}{2} \gamma \rho^2 - \gamma \rho^4 \right) \exp(-\gamma\rho^2) \right] \end{aligned} \quad (3-59)$$

The entropy of a propane mixture can be calculated by

$$\begin{aligned} S &= \sum x_i [S_i^0 - R \ln(\rho RT x_i)] - \left( B_0 R + \frac{2C_0}{T^3} \right)_p \rho \frac{\rho^2}{2} \\ &\quad + \frac{2C_p^2}{T^3} \left[ \frac{1 - e^{-\gamma\rho}}{\gamma\rho^2} - \frac{e^{-\gamma\rho^2}}{2} \right] \end{aligned} \quad (3-60)$$

or

$$S = \sum X_i [S_i^0 - R \ln RTX_i] - \left[ B_0 R + \frac{2C_0}{T^3} - \frac{3D_0}{T^4} + \frac{4E_0}{T^5} \right] \rho - \frac{1}{2} \left[ bR + \frac{d}{T^2} \right] \rho^2 + \frac{\alpha \rho^5 d}{5T^2} + \frac{2C}{\gamma T^3} [1 - (1 + \frac{1}{2}\gamma \rho^2) \exp(-\gamma \rho^2)] \quad (3-61)$$

corresponding to equations (3-26) and (3-27), respectively, for pure propane.

The specific heat of a propane mixture can be obtained by applying the equation

$$C_p = \sum X_i C_p^* - \sum X_i R + \frac{6C_0 \rho}{T^3} + \frac{6C}{\gamma T^3} \left( e^{-\gamma \rho^2} - 1 \right) + \frac{3C}{T^3} \rho^2 e^{-\gamma \rho^2} + \frac{T \left[ R + \left( B_0 R + \frac{2C_0}{T^3} \right) \rho + (bR \rho^2) - \frac{2C_0^2}{T^3} (1 + \gamma \rho^2) \exp(-\gamma \rho^2) \right]^2}{\text{denominator}} \quad (3-62)$$

where the denominator is

$$\begin{aligned} & \{RT + 2\rho \left( B_0 RT - A_0 - \frac{C_0}{T^2} \right) + 3\rho^2 (bRT - a) + 6a\alpha \rho^5 \\ & + \frac{C_0^2}{T^2} (3 + 3\gamma \rho^2 - 2\gamma^2 \rho^4 \exp(-\gamma \rho^2)) \end{aligned}$$

for B-W-R equation of state and

$$C_p = \sum X_i C_p^* - \sum X_i R + \left( \frac{6C_0}{T^3} - \frac{12D_0}{T^4} - \frac{20E_0}{T^5} \right) \rho + \frac{d}{T^2} \rho^2 + \frac{2}{5} \frac{\alpha d}{T^2} \rho^5 + \frac{6C}{\gamma T^3} (e^{-\gamma \rho^2} - 1) + \frac{3C}{T^3} \rho^2 e^{-\gamma \rho^2} + \bar{A} \quad (3-63)$$

using Starling's equation of state where

$$\bar{A} = \frac{T \left[ R + \rho \left( B_0 R + \frac{2C_0}{T^3} - \frac{3D_0}{T^4} + \frac{4E_0}{T^5} \right) + \rho^2 \left( bR + \frac{d}{T^2} \right) - \frac{C_0^2}{T^3} (1 + \gamma \rho^2) \exp(-\gamma \rho^2) - \frac{\alpha d \rho^5}{T^2} \right]^2}{\text{denominator}}$$

where the denominator is

$$\begin{aligned} & \{RT + 2\left(B_0 RT - A_0 - \frac{C_0}{T^2} + \frac{D_0}{T^3} - \frac{E_0}{T^4}\right)\rho + 3\rho^2\left(bRT - a - \frac{d}{T}\right) \\ & + 6\alpha\rho^2\left(a + \frac{d}{T}\right) + \frac{C_p^2}{T^2}(3 + 3\gamma_p^2 - 2\gamma_p^2)^4 \exp(-\gamma_p^2)\} \end{aligned}$$

It can be shown that the work content of a gaseous mixture is given by the relation:

$$A = \sum X_i [RT \ln \rho RT X_i + E_i^0 - TS_i^0] + \int_0^\rho \frac{P - RT\rho}{\rho^2} d\rho \quad (3-64)$$

By substituting the B-W-R equation into the above equation, it follows that

$$\begin{aligned} A = & \sum X_i [RT \ln \rho RT X_i + E_i^0 - TS_i^0] + \left(B_0 RT - A_0 - \frac{C_0}{T^2}\right)\rho + (bRT - a)\frac{\rho^2}{2} \\ & + a\alpha\rho^5/5 + \frac{C_p^2}{T^2} \left[ \frac{1 - \exp(-\gamma_p^2)}{\gamma_p^2} - \frac{\exp(-\gamma_p^2)}{2} \right] \end{aligned} \quad (3-65)$$

where  $E_i^0$  and  $S_i^0$  are, respectively, the energy and entropy of one mole of the  $i$ th pure component in the ideal gas state.

The fugacity,  $f_i$ , is obtained from the work content by the thermodynamic relation

$$RT \ln f_i = \left[ \frac{\partial NA}{\partial n_i} \right]_{V,T,n} - [E_i^0 - TS_i^0 + RT] \quad (3-66)$$

where  $n_i$  = number of moles of  $i$ th component and

$$N = \text{total number of moles} = \sum n_i$$

Substituting the expression for  $A$  into the above equation yields

$$\begin{aligned} RT \ln f_i = & RT \ln \rho RT X_i + [(B_0 + B_{0i})RT - 2(A_0 A_{0i})^{1/2} - 2(C_0 C_{0i})^{1/2}/T^2]\rho \\ & + \frac{3}{2}[RT(b^2 b_i)^{1/3} - (a^2 a_i)^{1/3}]_p^2 + \frac{3}{5}[a(\alpha^2 \alpha_i)^{1/3} + \alpha(a^2 a_i)^{1/3}]_p^5 \\ & + \frac{3\rho^2(C^2 C_i)^{1/3}}{T^2} \left[ \frac{1 - \exp(-\gamma_p^2)}{\gamma_p^2} - \frac{\exp(-\gamma_p^2)}{2} \right] \\ & - \frac{2\rho^2 C(\gamma_i)^{1/2}}{T^2} \left[ \frac{1 - \exp(-\gamma_p^2)}{\gamma_p^2} - \exp(-\gamma_p^2) \right] \\ & - [\gamma_p^2 \exp(-\gamma_p^2)]/2 \end{aligned} \quad (3-67)$$

Similarly, by applying the equation of state of propane proposed by K. E. Starling, the fugacity of the  $i$ th component in a mixture is

$$\begin{aligned}
 RT \ln f_i = & RT \ln (\rho RT_i) + \rho(B_0 + B_{0i})RT + 2\rho \sum_{j=1}^n x_j \left[ -(A_{0j} A_{0i})^{1/2} \right. \\
 & \left. - \frac{(C_{0j} C_{0i})^{1/2}}{T^2} + \frac{(D_{0j} D_{0i})^{1/2}}{T^3} - \frac{(E_{0j} E_{0i})^{1/2}}{T^4} \right] \\
 & + \frac{\rho^2}{2} \left[ 3(b^2 b_i)^{1/3} RT - 3(a^2 a_i)^{1/3} - \frac{3(d^2 d_i)^{1/3}}{T} \right] \\
 & + \frac{\alpha \rho^5}{5} \left[ 3(a^2 a_i)^{1/3} + \frac{3(d^2 d_i)^{1/3}}{T} \right] + \frac{3\rho^5}{5} \left( a + \frac{d}{T} \right) (a^2 a_i)^{1/3} \\
 & + \frac{3(C^2 C_i)^{1/3} \rho^2}{T^2} \left[ \frac{1 - \exp(-\gamma \rho^2)}{\gamma \rho^2} - \frac{\exp(-\gamma \rho^2)}{2} \right] \\
 & - \frac{2C}{\gamma T^2} \left[ \frac{\gamma_i}{\gamma} \right]^{1/2} \left\{ 1 - \exp(-\gamma \rho^2) [1 + \gamma \rho^2 + \frac{1}{2} \gamma^2 \rho^4] \right\} \quad (3-68)
 \end{aligned}$$

In order to evaluate the thermodynamic properties of a mixture, the properties of the constituents have to be known. The method employed in obtaining the thermodynamic data for propylene and n-butane was the same as that described above for pure propane. Tables 3-2, 3-3, and 3-4 give the coefficients for the ninth order equations for the enthalpy departure, the entropy reference and the specific heat reference of propylene and n-butane in addition to propane. This will enable the reader of this report to evaluate properties of any mixture of the three constituents without undue difficulties.

Above it was mentioned that Starling's equation appears to be more accurate in predicting saturation properties. In addition, the subcooled liquid data predicted by Starling's equation approximates experimental results better than those predicted by the B-W-R equation. For these reasons, the thermodynamic properties of mixtures were only calculated using Starling's equation.

Table 3-8 is a saturation temperature table for a "Pseudo-Fluid" consisting of 65% (by mole) propane, 25% propylene and 10% n-butane. Figure 3-8 shows the temperature-entropy diagram for this mixture. Also enclosed

are the saturation temperature tables for propylene and n-butane (see Tables 3-9 and 3-10). Figure 3-9 and 3-10 give the temperature-entropy diagrams of propylene and n-butane, respectively.

### 3.3 Discussion on the Thermodynamic Properties

In section 3.0 it was seen that Starling's equation incorporated more virial coefficients than that by Benedict-Webb-Rubin. Therefore, it is plausible to expect a higher accuracy from Starling's equation. This expectation is in part born out when one compares the predicted saturation pressures with those given by Stearns and George. (Compare Tables 3-6a with 3-7, and 3-5a with 3-7.) In addition, the predicted subcooled liquid properties of Starling's equation more closely approximate existing measured values than those resulting from the B-W-R equation. Also, it was found that, using Starling's equation, the calculated saturated liquid density at the critical point was the same as the calculated saturated vapor density, as it should be. This was found not to be the case when those properties were calculated with the B-W-R equation.

It is seen from the appropriate thermodynamic tables that there are negative values of enthalpy at the saturated liquid region for both the B-W-R and Starling's predictions but not for the Stearns and George's data. This is due to the difference in selection of the reference points. As mentioned before, the enthalpy was calculated by adding the standard enthalpy of formation  $H_0^0$  from the elements at 0°R and 0 psia to the difference in the enthalpy of propane in the ideal gas state at the temperature of interest and the reference state ( $H_0 - H_0^0$ ) and to the enthalpy departure ( $H - H_0$ ). When the enthalpy departure gives a negative value of magnitude greater than the sum of the other two terms, a negative value of enthalpy results.

TABLE 3-1a  
CONSTANTS FOR THE BENEDICT-WEBB-RUBIN EQUATION

Substances	Units	Propylene	Propane	n-Butane
molecular weight		42.047	44.062	58.078
$B_0$	$\frac{\text{ft}^3}{\text{lb-mole}}$	1.36263	1.55884	1.99211
$A_0$	$\frac{\text{ft}^6 \cdot \text{lb}_f}{\text{in}^2 \cdot \text{lb-mole}^2}$	23049.2	25915.4	38029.6
$C_0 \times 10^{-6}$	$\frac{\text{ft}^6 R^2 \text{lb}_f}{\text{lb-mole}^2 \cdot \text{in}^2}$	5365.97	6209.93	12130.5
$b$	$\frac{\text{ft}^6}{\text{lb-mole}^2}$	4.79997	5.77355	10.2636
$a$	$\frac{\text{lb}_f \cdot \text{ft}^9}{\text{lb-mole}^3 \cdot \text{in}^2}$	46758.6	57248.0	113705.0
$C \times 10^{-6}$	$\frac{\text{lb}_f \cdot \text{ft}^9 \cdot R^2}{\text{in}^2 \cdot \text{lb-mole}^3}$	20083.0	25247.8	61925.6
$\alpha$	$\frac{\text{ft}^9}{\text{lb-mole}^3}$	1873.12	2495.77	4526.93
$\gamma$	$\frac{\text{ft}^6}{\text{lb-mole}^2}$	469.325	564.524	872.447

TABLE 3 - 1b  
CONSTANTS FOR STARLING'S EQUATION

Substances	Units	Propylene	Propane	n-Butane
Molecular Weight		42.047	44.062	58.078
$B_0$	$\frac{ft^3}{lb\text{-mole}}$	0.114457	0.964762	1.56588
$A_0$	$\frac{ft^6 \cdot lb_f}{in^2 \cdot lb\text{-mole}^2}$	6051.36	18634.7	32544.7
$C_0$	$\frac{ft^6 R^2 lb_f}{lb\text{-mole}^2 \cdot in^2}$	$974762 \times 10^4$	$796178 \times 10^4$	$137436 \times 10^5$
$D_0$	$\frac{ft^6 R^3 lb_f}{lb\text{-mole}^2 \cdot in^2}$	$705921 \times 10^6$	$453708 \times 10^6$	$333159 \times 10^6$
$E_0$	$\frac{ft^6 R^4 lb_f}{lb\text{-mole}^2 \cdot in^2}$	$341250 \times 10^8$	$256053 \times 10^8$	$230902 \times 10^7$
$b$	$\frac{ft^6}{lb\text{-mole}^2}$	7.64114	5.46248	9.14066
$a$	$\frac{lb_f \cdot ft^9}{lb\text{-mole}^3 \cdot in^2}$	81880.4	40066.4	71181.8
$d$	$\frac{ft^9 R \cdot lb_f}{in^2 \cdot lb\text{-mole}^3}$	$54193.5 \times 10^2$	$150520 \times 10^2$	$364238 \times 10^2$
$\alpha$	$\frac{ft^9}{lb\text{-mole}^3}$	1.36532	2.01402	4.00985
$c$	$\frac{lb_f \cdot ft^9 \cdot R^2}{in^2 \cdot lb\text{-mole}^3}$	$294141 \times 10^5$	$274461 \times 10^5$	$700044 \times 10^5$
$\gamma$	$\frac{ft^6}{lb\text{-mole}^2}$	4.07919	4.56182	7.54122

Table 3-2

	Propane	Propylene	N-Butane
$\alpha_{e1}$	.742481481481 $\times 10^3$	.111045237968 $\times 10^4$	.802791666667 $\times 10^3$
$\alpha_{e2}$	.995278195229 $\times 10^3$	.107023834244 $\times 10^4$	.100514466012 $\times 10^4$
$\alpha_{e3}$	.727096407095 $\times 10^3$	.836734429396 $\times 10^3$	.649244242375 $\times 10^3$
$\alpha_{e4}$	.818422637234 $\times 10^3$	.963958858537 $\times 10^3$	.839380451085 $\times 10^3$
$\alpha_{e5}$	.830353420162 $\times 10^3$	.119605120652 $\times 10^4$	.971719198416 $\times 10^3$
$\alpha_{e6}$	.865844174954 $\times 10^3$	.123523622846 $\times 10^4$	.981070432727 $\times 10^3$
$\alpha_{e7}$	.932582802450 $\times 10^3$	.122910114799 $\times 10^4$	.955651779468 $\times 10^3$
$\alpha_{e8}$	.917816919015 $\times 10^3$	.123840922182 $\times 10^4$	.101726967301 $\times 10^4$
$\alpha_{e9}$	.858860971639 $\times 10^3$	.126348199349 $\times 10^4$	.980490358349 $\times 10^3$
$\beta_{e1}$	.182214471879 $\times 10^6$	.289148135505 $\times 10^6$	.172047081597 $\times 10^6$
$\beta_{e2}$	.202821566954 $\times 10^6$	.303593655594 $\times 10^6$	.210130748405 $\times 10^6$
$\beta_{e3}$	.223279163286 $\times 10^6$	.359719906439 $\times 10^6$	.254086490775 $\times 10^6$
$\beta_{e4}$	.189349834247 $\times 10^6$	.198487765514 $\times 10^6$	.147054880648 $\times 10^6$
$\beta_{e5}$	.172040258843 $\times 10^6$	.138702585635 $\times 10^6$	.117199772498 $\times 10^6$
$\beta_{e6}$	.148017284610 $\times 10^6$	.127279693740 $\times 10^6$	.123341054830 $\times 10^6$
$\beta_{e7}$	.118381676422 $\times 10^6$	.129278290233 $\times 10^6$	.103664754054 $\times 10^6$
$\beta_{e8}$	.139840562107 $\times 10^6$	.147957814196 $\times 10^6$	.883803087541 $\times 10^5$
$\beta_{e9}$	.118493330732 $\times 10^6$	.174325424377 $\times 10^6$	.946889837873 $\times 10^5$
$C_{e1}$	.126140038915 $\times 10^5$	.201157556705 $\times 10^5$	.182684354167 $\times 10^5$
$C_{e2}$	.254420893407 $\times 10^2$	.249178060153 $\times 10^2$	.343889910054 $\times 10^2$
$C_{e3}$	.111693664398 $\times 10^{-1}$	.793873123412 $\times 10^{-2}$	.142798901081 $\times 10^{-1}$
$C_{e4}$	.981725124759 $\times 10^{-6}$	.112252896961 $\times 10^{-5}$	.151117378284 $\times 10^{-5}$
$C_{e5}$	.194411920914 $\times 10^{-8}$	.572184000520 $\times 10^{-9}$	.192631943869 $\times 10^{-8}$
$C_{e6}$	.153143261260 $\times 10^{-11}$	.705903272455 $\times 10^{-12}$	.194002529244 $\times 10^{-11}$
$C_{e7}$	.138220156370 $\times 10^{-15}$	.472345691675 $\times 10^{-15}$	.621958539961 $\times 10^{-15}$
$C_{e8}$	.305475135778 $\times 10^{-17}$	.390746140224 $\times 10^{-18}$	.111591462586 $\times 10^{-17}$
$C_{e9}$	.628558859816 $\times 10^{-20}$	.150828380816 $\times 10^{-20}$	.202228932320 $\times 10^{-20}$
$C_{e10}$	.604295630108 $\times 10^{-23}$	.848699864953 $\times 10^{-23}$	.127422880370 $\times 10^{-22}$
$H_0^0$	-35042.06798	14534.46128	11768.34008

Table 3-3

	Propane	Propylene	N-Butane
$\alpha_{e1}$	.121486500000 $\times 10^4$	.553847718462 $\times 10^9$	.145800000000 $\times 10^4$
$\alpha_{e2}$	.157575186470 $\times 10^4$	.664615397654 $\times 10^{10}$	.152575335121 $\times 10^4$
$\alpha_{e3}$	.146640593519 $\times 10^4$	.161423147522 $\times 10^4$	.156891382752 $\times 10^4$
$\alpha_{e4}$	.139993086664 $\times 10^4$	.162766912336 $\times 10^4$	.156539439070 $\times 10^4$
$\alpha_{e5}$	.146520971796 $\times 10^4$	.719999522832 $\times 10^{10}$	.153356457801 $\times 10^4$
$\alpha_{e6}$	.143264451942 $\times 10^4$	.631478364392 $\times 10^4$	.149922265352 $\times 10^4$
$\alpha_{e7}$	.142047526795 $\times 10^4$	.170709680249 $\times 10^4$	.148560135399 $\times 10^4$
$\alpha_{e8}$	.139214986725 $\times 10^4$	.124270164341 $\times 10^9$	.148865270315 $\times 10^4$
$\alpha_{e9}$	.134990212476 $\times 10^4$	.707573157625 $\times 10^{10}$	.148324423940 $\times 10^4$
$\beta_{e1}$	.613757596275 $\times 10^6$	.368094501245 $\times 10^{19}$	.563976000000 $\times 10^6$
$\beta_{e2}$	.405377805164 $\times 10^6$	.543757512200 $\times 10^7$	.400713794392 $\times 10^6$
$\beta_{e3}$	.477683840709 $\times 10^6$	.386499419225 $\times 10^6$	.364028426115 $\times 10^6$
$\beta_{e4}$	.431356410957 $\times 10^6$	.553679411841 $\times 10^{12}$	.357374314602 $\times 10^6$
$\beta_{e5}$	.399730302774 $\times 10^6$	.338024126545 $\times 10^{14}$	.358830780250 $\times 10^6$
$\beta_{e6}$	.399682917428 $\times 10^6$	.286971601807 $\times 10^6$	.350381228412 $\times 10^6$
$\beta_{e7}$	.374740444251 $\times 10^6$	.241240598015 $\times 10^6$	.324510014436 $\times 10^6$
$\beta_{e8}$	.377041634817 $\times 10^6$	.879289793523 $\times 10^{18}$	.292118892082 $\times 10^6$
$\beta_{e9}$	.338738853360 $\times 10^6$	.120207105186 $\times 10^8$	.266308028731 $\times 10^6$
$c_{e1}$	.825700000000 $\times 10^2$	.883538461538 $\times 10^2$	.106566666667 $\times 10^3$
$c_{e2}$	.266135841725 $\times 10^{-1}$	.292708189478 $\times 10^{-8}$	.334716370909 $\times 10^{-1}$
$c_{e3}$	.395796189449 $\times 10^{-5}$	.281725147400 $\times 10^{-11}$	.480866637359 $\times 10^{-5}$
$c_{e4}$	.788110527067 $\times 10^{-9}$	.420386090977 $\times 10^{-15}$	.572031476567 $\times 10^{-9}$
$c_{e5}$	.688562267346 $\times 10^{-12}$	.923330124310 $\times 10^{-20}$	.160064264642 $\times 10^{-12}$
$c_{e6}$	.907615953571 $\times 10^{-15}$	.918526012476 $\times 10^{-29}$	.221775210984 $\times 10^{-15}$
$c_{e7}$	.956080011946 $\times 10^{-18}$	.483637271218 $\times 10^{-33}$	.439488097002 $\times 10^{-18}$
$c_{e8}$	.968897518982 $\times 10^{-21}$	.797306956991 $\times 10^{-33}$	.503179453448 $\times 10^{-21}$
$c_{e9}$	.137432907223 $\times 10^{-23}$	.638050169456 $\times 10^{-41}$	.402404744657 $\times 10^{-24}$
$c_{e10}$	.686591484810 $\times 10^{-27}$	.395373525494 $\times 10^{-48}$	.233709969648 $\times 10^{-27}$

Table 3-4

	Propane	Propylene	N-Butane
$\alpha_{e1}$	.121171500000 $\times 10^4$	.111890476190 $\times 10^4$	.732764705882 $\times 10^3$
$\alpha_{e2}$	.156393932388 $\times 10^4$	.127428305279 $\times 10^4$	.928122739667 $\times 10^3$
$\alpha_{e3}$	.144300986829 $\times 10^4$	.132273649816 $\times 10^4$	.883526559810 $\times 10^3$
$\alpha_{e4}$	.139317577302 $\times 10^4$	.130752856489 $\times 10^4$	.877112912243 $\times 10^3$
$\alpha_{e5}$	.148108914194 $\times 10^4$	.126887266352 $\times 10^4$	.821626216559 $\times 10^3$
$\alpha_{e6}$	.146525609386 $\times 10^4$	.123145100632 $\times 10^4$	.838146564495 $\times 10^3$
$\alpha_{e7}$	.146426799121 $\times 10^4$	.122428880142 $\times 10^4$	.825270570532 $\times 10^3$
$\alpha_{e8}$	.143686445275 $\times 10^4$	.124021816239 $\times 10^4$	.807006176432 $\times 10^3$
$\alpha_{e9}$	.136105738084 $\times 10^4$	.124873578342 $\times 10^4$	.763580499084 $\times 10^3$
$\beta_{e1}$	.619898773275 $\times 10^6$	.278948181406 $\times 10^6$	.588451211073 $\times 10^5$
$\beta_{e2}$	.417344093380 $\times 10^6$	.169462158799 $\times 10^6$	.457379553837 $\times 10^5$
$\beta_{e3}$	.491622431021 $\times 10^6$	.155950524167 $\times 10^6$	.393482833606 $\times 10^5$
$\beta_{e4}$	.427343890147 $\times 10^6$	.161217407838 $\times 10^6$	.467988179474 $\times 10^5$
$\beta_{e5}$	.384885019474 $\times 10^6$	.171708625504 $\times 10^6$	.407590942774 $\times 10^5$
$\beta_{e6}$	.374955579138 $\times 10^6$	.174439209490 $\times 10^6$	.361214749425 $\times 10^5$
$\beta_{e7}$	.346493535855 $\times 10^6$	.162501007150 $\times 10^6$	.267115109296 $\times 10^5$
$\beta_{e8}$	.355265885086 $\times 10^6$	.146873882126 $\times 10^6$	.265722245049 $\times 10^5$
$\beta_{e9}$	.345189959100 $\times 10^6$	.136435643095 $\times 10^6$	.176479405673 $\times 10^5$
$C_{e1}$	.294185000000 $\times 10^2$	.247374285714 $\times 10^2$	.295083529412 $\times 10^2$
$C_{e2}$	.168993352207 $\times 10^{-1}$	.149128702681 $\times 10^{-1}$	.306182347186 $\times 10^{-1}$
$C_{e3}$	-.583778927465 $\times 10^{-5}$	-.515569210551 $\times 10^{-5}$	-.895371840923 $\times 10^{-5}$
$C_{e4}$	.958637032132 $\times 10^{-9}$	.621288442486 $\times 10^{-9}$	-.799920168655 $\times 10^{-8}$
$C_{e5}$	.792131317606 $\times 10^{-12}$	.111130562037 $\times 10^{-11}$	.213486869887 $\times 10^{-10}$
$C_{e6}$	.745544270460 $\times 10^{-16}$	-.171640456258 $\times 10^{-14}$	-.298797054874 $\times 10^{-13}$
$C_{e7}$	.367952233356 $\times 10^{-18}$	.857104317985 $\times 10^{-18}$	.878606120216 $\times 10^{-16}$
$C_{e8}$	.200994242615 $\times 10^{-23}$	.137562067206 $\times 10^{-20}$	-.214733834833 $\times 10^{-18}$
$C_{e9}$	-.555179524348 $\times 10^{-23}$	-.258502116823 $\times 10^{-23}$	-.656409752151 $\times 10^{-21}$
$C_{e10}$	.234126033182 $\times 10^{-26}$	.181970505311 $\times 10^{-26}$	.129920025308 $\times 10^{-22}$

THERMODYNAMIC PROPERTIES OF PROPANE AS PREDICTED BY BENIDICT-WEBB-RUJIN EQUATION OF STATE

Table 3-5a

Saturation Temperature Table for Propane Calculated from the Benedict-Webb-Rubin Equation of State.

Table 3-5a (continued)

130.00	68.	3333242975	3041C27987	-820.715395416	-670.592574463	• 95166427271	1.21701914309
133.75	70.	0334378955	7812240767	-809.367670898	-670.149781753	• 5641762425	1.21682268617
137.52	72.	0235333208	78CB249574	-808.019533299	-669.676336214	• 55667001840	1.21675744876
141.51	74.	0335663651	7768573729	-806.670581351	-669.292074459	• 95591532292	1.2163757366
145.48	76.	0235910767	776245	-802.369968779	-668.423676515	• 96410274760	1.2162236352
149.57	78.	033503808	77177	-802.617817329	-668.003402606	• 3665613611	1.216158655
153.57	80.	0334265735	77961	-801.264155728	-667.593628244	• 96714637947	1.2160576678
157.57	82.	0334426216	7791	-798.176426216	-667.173754380	• 96714637947	1.2160576678
161.57	84.	03344242457	7792	-797.191743446	-666.7642616	• 96714637947	1.2160576678
165.57	86.	03345337947	783	-795.830095565	-665.961078931	• 97877001285	1.21486380027
169.57	88.	0346641616	785	-795.830095565	-665.961078931	• 97877001285	1.21486380027
173.68	90.	0349642661	794	-795.466977308	-665.180710316	• 983357668677	1.21476845098
177.68	92.	0349272179	795	-795.101031944	-664.821608418	• 98598037648	1.21419843982
181.68	94.	0349645571	796	-795.128277	-664.022126407	• 98436822770	1.21365148755
185.68	96.	0349245555	797	-795.4246102	-664.322126407	• 990084212271	1.21365148755
189.68	98.	0349582668	798	-795.7072739	-664.322126407	• 9932056980	1.21365148755
193.68	100.	0349624935	799	-797.603817270	-663.95034342	• 9956246664813	1.21344648132
197.68	102.	0349152154	800	-798.4152343	-663.95034342	• 9956246664813	1.21344648132
201.68	104.	0349631787	801	-798.4152343	-662.952322	• 9956246664813	1.21344648132
205.68	106.	0349631787	802	-798.4152343	-662.952322	• 9956246664813	1.21344648132
209.68	108.	0349631787	803	-798.4152343	-662.952322	• 9956246664813	1.21344648132
213.68	110.	0349641616	804	-798.4152343	-662.952322	• 9956246664813	1.21344648132
217.68	112.	0349642661	805	-798.4152343	-662.952322	• 9956246664813	1.21344648132
221.68	114.	0349642661	806	-798.4152343	-662.952322	• 9956246664813	1.21344648132
225.68	116.	0349642661	807	-798.4152343	-662.952322	• 9956246664813	1.21344648132
229.68	118.	0349642661	808	-798.4152343	-662.952322	• 9956246664813	1.21344648132
233.68	120.	0349642661	809	-798.4152343	-662.952322	• 9956246664813	1.21344648132
237.68	122.	0349642661	810	-798.4152343	-662.952322	• 9956246664813	1.21344648132
241.68	124.	0349642661	811	-798.4152343	-662.952322	• 9956246664813	1.21344648132
245.68	126.	0349642661	812	-798.4152343	-662.952322	• 9956246664813	1.21344648132
249.68	128.	0349642661	813	-798.4152343	-662.952322	• 9956246664813	1.21344648132
253.68	130.	0349642661	814	-798.4152343	-662.952322	• 9956246664813	1.21344648132
257.68	132.	0349642661	815	-798.4152343	-662.952322	• 9956246664813	1.21344648132
261.68	134.	0349642661	816	-798.4152343	-662.952322	• 9956246664813	1.21344648132
265.68	136.	0349642661	817	-798.4152343	-662.952322	• 9956246664813	1.21344648132
269.68	138.	0349642661	818	-798.4152343	-662.952322	• 9956246664813	1.21344648132
273.68	140.	0349642661	819	-798.4152343	-662.952322	• 9956246664813	1.21344648132
277.68	142.	0349642661	820	-798.4152343	-662.952322	• 9956246664813	1.21344648132
281.68	144.	0349642661	821	-798.4152343	-662.952322	• 9956246664813	1.21344648132
285.68	146.	0349642661	822	-798.4152343	-662.952322	• 9956246664813	1.21344648132
289.68	148.	0349642661	823	-798.4152343	-662.952322	• 9956246664813	1.21344648132
293.68	150.	0349642661	824	-798.4152343	-662.952322	• 9956246664813	1.21344648132
297.68	152.	0349642661	825	-798.4152343	-662.952322	• 9956246664813	1.21344648132
301.68	154.	0349642661	826	-798.4152343	-662.952322	• 9956246664813	1.21344648132
305.68	156.	0349642661	827	-798.4152343	-662.952322	• 9956246664813	1.21344648132
309.68	158.	0349642661	828	-798.4152343	-662.952322	• 9956246664813	1.21344648132
313.68	160.	0349642661	829	-798.4152343	-662.952322	• 9956246664813	1.21344648132
317.68	162.	0349642661	830	-798.4152343	-662.952322	• 9956246664813	1.21344648132
321.68	164.	0349642661	831	-798.4152343	-662.952322	• 9956246664813	1.21344648132
325.68	166.	0349642661	832	-798.4152343	-662.952322	• 9956246664813	1.21344648132
329.68	168.	0349642661	833	-798.4152343	-662.952322	• 9956246664813	1.21344648132
333.68	170.	0349642661	834	-798.4152343	-662.952322	• 9956246664813	1.21344648132
337.68	172.	0349642661	835	-798.4152343	-662.952322	• 9956246664813	1.21344648132
341.68	174.	0349642661	836	-798.4152343	-662.952322	• 9956246664813	1.21344648132
345.68	176.	0349642661	837	-798.4152343	-662.952322	• 9956246664813	1.21344648132
349.68	178.	0349642661	838	-798.4152343	-662.952322	• 9956246664813	1.21344648132
353.68	180.	0349642661	839	-798.4152343	-662.952322	• 9956246664813	1.21344648132
357.68	182.	0349642661	840	-798.4152343	-662.952322	• 9956246664813	1.21344648132
361.68	184.	0349642661	841	-798.4152343	-662.952322	• 9956246664813	1.21344648132
365.68	186.	0349642661	842	-798.4152343	-662.952322	• 9956246664813	1.21344648132
369.68	188.	0349642661	843	-798.4152343	-662.952322	• 9956246664813	1.21344648132
373.68	190.	0349642661	844	-798.4152343	-662.952322	• 9956246664813	1.21344648132
377.68	192.	0349642661	845	-798.4152343	-662.952322	• 9956246664813	1.21344648132
381.68	194.	0349642661	846	-798.4152343	-662.952322	• 9956246664813	1.21344648132
385.68	196.	0349642661	847	-798.4152343	-662.952322	• 9956246664813	1.21344648132
389.68	198.	0349642661	848	-798.4152343	-662.952322	• 9956246664813	1.21344648132
393.68	200.	0349642661	849	-798.4152343	-662.952322	• 9956246664813	1.21344648132
397.68	202.	0349642661	850	-798.4152343	-662.952322	• 9956246664813	1.21344648132
401.68	204.	0349642661	851	-798.4152343	-662.952322	• 9956246664813	1.21344648132
405.68	206.	0349642661	852	-798.4152343	-662.952322	• 9956246664813	1.21344648132
409.68	208.	0349642661	853	-798.4152343	-662.952322	• 9956246664813	1.21344648132
413.68	210.	0349642661	854	-798.4152343	-662.952322	• 9956246664813	1.21344648132
417.68	212.	0349642661	855	-798.4152343	-662.952322	• 9956246664813	1.21344648132
421.68	214.	0349642661	856	-798.4152343	-662.952322	• 9956246664813	1.21344648132
425.68	216.	0349642661	857	-798.4152343	-662.952322	• 9956246664813	1.21344648132
429.68	218.	0349642661	858	-798.4152343	-662.952322	• 9956246664813	1.21344648132
433.68	220.	0349642661	859	-798.4152343	-662.952322	• 9956246664813	1.21344648132
437.68	222.	0349642661	860	-798.4152343	-662.952322	• 9956246664813	1.21344648132
441.68	224.	0349642661	861	-798.4152343	-662.952322	• 9956246664813	1.21344648132
445.68	226.	0349642661	862	-798.4152343	-662.952322	• 9956246664813	1.21344648132
449.68	228.	0349642661	863	-798.4152343	-662.952322	• 9956246664813	1.21344648132
453.68	230.	0349642661	864	-798.4152343	-662.952322	• 9956246664813	1.21344648132
457.68	232.	0349642661	865	-798.4152343	-662.952322	• 9956246664813	1.21344648132
461.68	234.	0349642661	866	-798.4152343	-662.952322	• 9956246664813	1.21344648132
465.68	236.	0349642661	867	-798.4152343	-662.952322	• 9956246664813	1.21344648132
469.68	238.	0349642661	868	-798.4152343	-662.952322	• 9956246664813	1.21344648132
473.68	240.	0349642661	869	-798.4152343	-662.952322	• 9956246664813	1.21344648132
477.68	242.	0349642661	870	-798.4152343	-662.952322	• 9956246664813	1.21344648132
481.68	244.	0349642661	871	-798.4152343	-662.952322	• 9956246664813	1.21344648132
485.68	246.	0349642661	872	-798.4152343	-662.952322	• 9956246664813	1.21344648132
489.68	248.	0349642661	873	-798.4152343	-662.952322	• 9956246664813	1.21344648132
493.68	250.	0349642661	874	-798.4152343	-662.952322	• 9956246664813	1.21344648132
497.68	252.	0349642661	875	-798.4152343	-662.952322	• 9956246664813	1.21344648132
501.68	254.	0349642661	876	-798.4152343	-662.952322	• 9956246664813	1.21344648132
505.68	256.	0349642661	877	-798.4152343	-662.952322	• 9956246664813	1.21344648132
509.68	258.	0349642661					

### THERMODYNAMIC PROPERTIES OF PROPANE AS PREDICTED BY DEMIDECT-WEBB-RUBIN EQUATION OF STATE

Table 3-5a (continued)

Table 3-5a (continued)

130.00	68.	4491123432	4652941447	3758950735	2209.289995
133.75	70.	4485550947	4676260881	222762111	2187.952929
137.50	72.	4475550472	4687642558	3775614271	683.123553
141.45	74.	4474762558	4722956769	2145.632887	681.1478057
145.50	76.	4468456471	4745056559	2103.062422	676.812557
149.50	78.	4468156471	4767456619	2083.062422	674.561988
153.75	80.	4462762558	4798275278	2209.123545	672.1268345
157.75	82.	4462166852	48275278	2209.166852	669.766477
161.75	84.	4462626692	4847166852	2209.202000	667.373043
165.75	86.	4462326692	4867166852	2209.242000	665.5864263
169.75	88.	4461361370	4887166852	2209.282000	663.73043
173.75	90.	4461466479	4907166852	2209.322000	662.373043
177.75	92.	4461766479	4927166852	2209.362000	660.5864263
181.75	94.	4461266479	4947166852	2209.402000	658.73043
185.75	96.	4461566479	4967166852	2209.442000	656.943043
189.75	98.	4461866479	4987166852	2209.482000	655.153043
193.75	100.	4462166479	5007166852	2209.522000	653.363043
197.75	102.	4462466479	5027166852	2209.562000	651.573043
201.75	104.	4462766479	5047166852	2209.602000	649.783043
205.75	106.	4463066479	5067166852	2209.642000	647.993043
209.75	108.	4463366479	5087166852	2209.682000	646.203043
213.75	110.	4463666479	5107166852	2209.722000	644.413043
217.75	112.	4463966479	5127166852	2209.762000	642.623043
221.75	114.	4464266479	5147166852	2209.802000	640.833043
225.75	116.	4464566479	5167166852	2209.842000	639.043043
229.75	118.	4464866479	5187166852	2209.882000	637.253043
233.75	120.	4465166479	5207166852	2209.922000	635.463043
237.75	122.	4465466479	5227166852	2209.962000	633.673043
241.75	124.	4465766479	5247166852	2209.102000	631.883043
245.75	126.	4466066479	5267166852	2209.142000	629.093043
249.75	128.	4466366479	5287166852	2209.182000	627.303043
253.75	130.	4466666479	5307166852	2209.222000	625.513043
257.75	132.	4466966479	5327166852	2209.262000	623.723043
261.75	134.	4467266479	5347166852	2209.302000	621.933043
265.75	136.	4467566479	5367166852	2209.342000	620.143043
269.75	138.	4467866479	5387166852	2209.382000	618.353043
273.75	140.	4468166479	5407166852	2209.422000	616.563043
277.75	142.	4468466479	5427166852	2209.462000	614.773043
281.75	144.	4468766479	5447166852	2209.502000	612.983043
285.75	146.	4469066479	5467166852	2209.542000	611.193043
289.75	148.	4469366479	5487166852	2209.582000	609.403043
293.75	150.	4469666479	5507166852	2209.622000	607.613043
297.75	152.	4469966479	5527166852	2209.662000	605.823043
301.75	154.	4470266479	5547166852	2209.702000	604.033043
305.75	156.	4470566479	5567166852	2209.742000	602.243043
309.75	158.	4470866479	5587166852	2209.782000	600.453043
313.75	160.	4471166479	5607166852	2209.822000	598.663043
317.75	162.	4471466479	5627166852	2209.862000	596.873043
321.75	164.	4471766479	5647166852	2209.902000	595.083043
325.75	166.	4472066479	5667166852	2209.942000	593.293043
329.75	168.	4472366479	5687166852	2209.982000	591.503043
333.75	170.	4472666479	5707166852	2210.022000	589.713043
337.75	172.	4472966479	5727166852	2210.062000	587.923043
341.75	174.	4473266479	5747166852	2210.102000	586.133043
345.75	176.	4473566479	5767166852	2210.142000	584.343043
349.75	178.	4473866479	5787166852	2210.182000	582.553043
353.75	180.	4474166479	5807166852	2210.222000	580.763043
357.75	182.	4474466479	5827166852	2210.262000	578.973043
361.75	184.	4474766479	5847166852	2210.302000	577.183043
365.75	186.	4475066479	5867166852	2210.342000	575.393043
369.75	188.	4475366479	5887166852	2210.382000	573.603043
373.75	190.	4475666479	5907166852	2210.422000	571.813043
377.75	192.	4475966479	5927166852	2210.462000	569.023043
381.75	194.	4476266479	5947166852	2210.502000	567.233043
385.75	196.	4476566479	5967166852	2210.542000	565.443043
389.75	198.	4476866479	5987166852	2210.582000	563.653043
393.75	200.	4477166479	6007166852	2210.622000	561.863043
397.75	202.	4477466479	6027166852	2210.662000	559.073043
401.75	204.	4477766479	6047166852	2210.702000	557.283043
405.75	206.	4478066479	6067166852	2210.742000	555.493043
409.75	208.	4478366479	6087166852	2210.782000	553.703043
413.75	210.	4478666479	6107166852	2210.822000	551.913043
417.75	212.	4478966479	6127166852	2210.862000	549.123043
421.75	214.	4479266479	6147166852	2210.902000	547.333043
425.75	216.	4479566479	6167166852	2210.942000	545.543043
429.75	218.	4479866479	6187166852	2210.982000	543.753043
433.75	220.	4480166479	6207166852	2211.022000	541.963043
437.75	222.	4480466479	6227166852	2211.062000	539.173043
441.75	224.	4480766479	6247166852	2211.102000	537.383043
445.75	226.	4481066479	6267166852	2211.142000	535.593043
449.75	228.	4481366479	6287166852	2211.182000	533.803043
453.75	230.	4481666479	6307166852	2211.222000	531.913043
457.75	232.	4481966479	6327166852	2211.262000	529.123043
461.75	234.	4482266479	6347166852	2211.302000	527.333043
465.75	236.	4482566479	6367166852	2211.342000	525.543043
469.75	238.	4482866479	6387166852	2211.382000	523.753043
473.75	240.	4483166479	6407166852	2211.422000	521.963043
477.75	242.	4483466479	6427166852	2211.462000	519.173043
481.75	244.	4483766479	6447166852	2211.502000	517.383043
485.75	246.	4484066479	6467166852	2211.542000	515.593043
489.75	248.	4484366479	6487166852	2211.582000	513.803043
493.75	250.	4484666479	6507166852	2211.622000	511.913043
497.75	252.	4484966479	6527166852	2211.662000	509.123043
501.75	254.	4485266479	6547166852	2211.702000	507.333043
505.75	256.	4485566479	6567166852	2211.742000	505.543043
509.75	258.	4485866479	6587166852	2211.782000	503.753043
513.75	260.	4486166479	6607166852	2211.822000	501.963043
517.75	262.	4486466479	6627166852	2211.862000	500.173043
521.75	264.	4486766479	6647166852	2211.902000	498.383043
525.75	266.	4487066479	6667166852	2211.942000	496.593043
529.75	268.	4487366479	6687166852	2211.982000	494.803043
533.75	270.	4487666479	6707166852	2212.022000	493.013043
537.75	272.	4487966479	6727166852	2212.062000	491.223043
541.75	274.	4488266479	6747166852	2212.102000	489.433043
545.75	276.	4488566479	6767166852	2212.142000	487.643043
549.75	278.	4488866479	6787166852	2212.182000	485.853043
553.75	280.	4489166479	6807166852	2212.222000	484.063043
557.75	282.	4489466479	6827166852	2212.262000	482.273043
561.75	284.	4489766479	6847166852	2212.302000	480.483043
565.75	286.	4490066479	6867166852	2212.342000	478.693043
569.75	288.	4490366479	6887166852	2212.382000	476.903043
573.75	290.	4490666479	6907166852	2212.422000	475.113043
577.75	292.	4490966479	6927166852	2212.462000	473.323043
581.75	294.	4491266479	6947166852	2212.502000	471.533043
585.75	296.	4491566479	6967166852	2212.542000	469.743043
589.75	298.	4491866479	6987166852	2212.582000	468.053043
593.75	300.	4492166479	7007166852	2212.622000	466.263043
597.75	302.	4492466479	7027166852	2212.662000	464.473043
601.75	304.	4492766479	7047166852	2212.702000	462.683043
605.75	306.	4493066479	7067166852	2212.742000	460.893043
609.75	308.	4493366479	7087166852	2212.782000	459.103043
613.75	310.	4493666479	7107166852	2212.822000	457.313043
617.75	312.	4493966479	7127166852	2212.862000	455.523043
621.75	314.	4494266479	7147166852	2212.902000	453.733043
625.75	316.	4494566479	7167166852	2212.942000	451.943043
629.75	318.	4494866479	7187166852	2212.982000	449.153043
633.75	320.	4495166479	7207166852	2213.022000	447.363043
637.75	322.	4495466479	7227166852	2213.062000	445.573043
641.75	324.	4495766479	7247166852	2213.102000	443.783043
645.75	326.	4496066479	7267166852	2213.142000	441.993043
649.75	328.	4496366479	7287166852	2213.182000	439.203043
653.75	330.	4496666479	7307166852	2213.222000	4

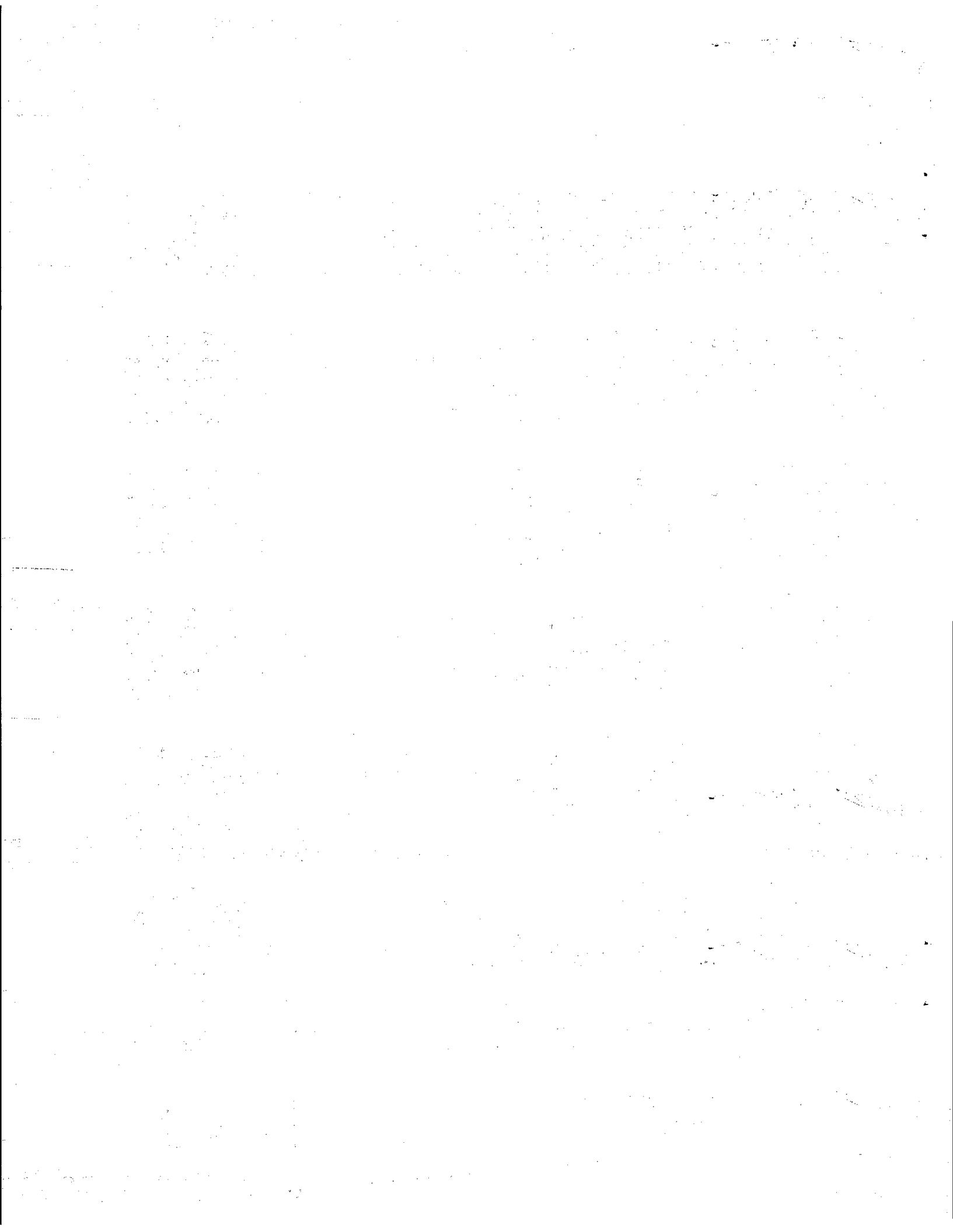


Table 3-5b (continued)

Table 3-5b (continued)

Table 3-5b (continued)

240	•
220	•
210	•
200	•
190	•
180	•
170	•
160	•
150	•
140	•
130	•
120	•
110	•
100	•
90	•
80	•
70	•

PRESSURE PSIA	VOLUME FT <sup>3</sup> /LBM	ENTHALPY BTU/LBM	ENTROPY BTU/LBM/SEG F	TEMPERATURE = 30 DEG F	CP BTU/LBM/DEG F	CV BTU/LBM/DEG F	SONIC VELOCITY FT/SEC
100	1.0000	100.00	0.2900				

PRESSURE PSIA	VOLUME FT <sup>3</sup> /LBM	ENTHALPY BTU/LBM	ENTROPY BTU/LB <sup>M</sup> /DEG F	CP BTU/LB <sup>M</sup> /DEG F	CV BTU/LB <sup>M</sup> /DEG F	SONIC VELOCITY FT/SEC
5600	0.03146695	-828.927872	9111753	47003177	46979312	2673.8545
5640	0.03148242	-828.961866	9113403	46931263	46907935	2667.7454
5680	0.03150812	-828.96571	9115062	46931356	46950656	2661.6113
5720	0.03152385	-828.9681	9116725	46931263	46949267	2655.4521
5760	0.03154569	-828.9703	9118376	46931263	46949267	2651.6
5800	0.03156166	-828.9707	91201761	46931263	46949267	2649.0
5840	0.03157616	-828.9707	91216364	46931263	46949267	2647.6
5880	0.03159405	-828.9707	91232036	46931263	46949267	2646.2
5920	0.03161092	-828.9707	91237775	46931263	46949267	2645.0
5960	0.03161676	-828.9707	91255523	46931263	46949267	2644.0
6000	0.03162269	-828.9707	91272380	46931263	46949267	2643.0
6040	0.03162862	-828.9707	91289136	46931263	46949267	2642.0
6080	0.03163456	-828.9707	91305892	46931263	46949267	2641.0
6120	0.03164046	-828.9707	91322648	46931263	46949267	2640.0
6160	0.03164639	-828.9707	91339388	46931263	46949267	2639.0
6200	0.03165233	-828.9707	91356134	46931263	46949267	2638.0
6240	0.03165827	-828.9707	91372830	46931263	46949267	2637.0
6280	0.03166421	-828.9707	91389576	46931263	46949267	2636.0
6320	0.03167015	-828.9707	91406322	46931263	46949267	2635.0
6360	0.03167609	-828.9707	91423068	46931263	46949267	2634.0
6400	0.03168193	-828.9707	91439814	46931263	46949267	2633.0
6440	0.03168787	-828.9707	91456550	46931263	46949267	2632.0
6480	0.03169381	-828.9707	91473296	46931263	46949267	2631.0
6520	0.03169975	-828.9707	91489032	46931263	46949267	2630.0
6560	0.03170569	-828.9707	91505778	46931263	46949267	2629.0
6600	0.03171163	-828.9707	91522524	46931263	46949267	2628.0
6640	0.03171757	-828.9707	91539270	46931263	46949267	2627.0
6680	0.03172351	-828.9707	91555916	46931263	46949267	2626.0
6720	0.03172945	-828.9707	91572652	46931263	46949267	2625.0
6760	0.03173539	-828.9707	91589388	46931263	46949267	2624.0
6800	0.03174133	-828.9707	91606124	46931263	46949267	2623.0
6840	0.03174727	-828.9707	91622860	46931263	46949267	2622.0
6880	0.03175321	-828.9707	91639596	46931263	46949267	2621.0
6920	0.03175915	-828.9707	91656332	46931263	46949267	2620.0
6960	0.03176509	-828.9707	91673068	46931263	46949267	2619.0
7000	0.03177103	-828.9707	91689804	46931263	46949267	2618.0
7040	0.03177697	-828.9707	91706540	46931263	46949267	2617.0
7080	0.03178291	-828.9707	91723276	46931263	46949267	2616.0
7120	0.03178885	-828.9707	91739912	46931263	46949267	2615.0
7160	0.03179479	-828.9707	91756648	46931263	46949267	2614.0
7200	0.03179973	-828.9707	91773384	46931263	46949267	2613.0
7240	0.03180567	-828.9707	91789120	46931263	46949267	2612.0
7280	0.03181161	-828.9707	91805856	46931263	46949267	2611.0
7320	0.03181755	-828.9707	91822592	46931263	46949267	2610.0
7360	0.03182349	-828.9707	91839328	46931263	46949267	2609.0
7400	0.03182943	-828.9707	91856064	46931263	46949267	2608.0
7440	0.03183537	-828.9707	91872800	46931263	46949267	2607.0
7480	0.03184131	-828.9707	91889536	46931263	46949267	2606.0
7520	0.03184725	-828.9707	91906272	46931263	46949267	2605.0
7560	0.03185319	-828.9707	91922998	46931263	46949267	2604.0
7600	0.03185913	-828.9707	91939734	46931263	46949267	2603.0
7640	0.03186507	-828.9707	91956470	46931263	46949267	2602.0
7680	0.03187001	-828.9707	91973206	46931263	46949267	2601.0
7720	0.03187595	-828.9707	91989942	46931263	46949267	2600.0
7760	0.03188189	-828.9707	92006678	46931263	46949267	2599.0
7800	0.03188783	-828.9707	92023414	46931263	46949267	2598.0
7840	0.03189377	-828.9707	92039940	46931263	46949267	2597.0
7880	0.03189971	-828.9707	92056676	46931263	46949267	2596.0
7920	0.03190565	-828.9707	92073412	46931263	46949267	2595.0
7960	0.03191159	-828.9707	92089948	46931263	46949267	2594.0
8000	0.03191753	-828.9707	92106684	46931263	46949267	2593.0
8040	0.03192347	-828.9707	92123420	46931263	46949267	2592.0
8080	0.03192941	-828.9707	92139956	46931263	46949267	2591.0
8120	0.03193535	-828.9707	92156692	46931263	46949267	2590.0
8160	0.03194129	-828.9707	92173428	46931263	46949267	2589.0
8200	0.03194723	-828.9707	92189964	46931263	46949267	2588.0
8240	0.03195317	-828.9707	92206690	46931263	46949267	2587.0
8280	0.03195911	-828.9707	92223426	46931263	46949267	2586.0
8320	0.03196505	-828.9707	92239962	46931263	46949267	2585.0
8360	0.03197099	-828.9707	92256698	46931263	46949267	2584.0
8400	0.03197693	-828.9707	92273434	46931263	46949267	2583.0
8440	0.03198287	-828.9707	92289970	46931263	46949267	2582.0
8480	0.03198881	-828.9707	92306706	46931263	46949267	2581.0
8520	0.03199475	-828.9707	92323442	46931263	46949267	2580.0
8560	0.03200069	-828.9707	92339978	46931263	46949267	2579.0
8600	0.03200663	-828.9707	92356714	46931263	46949267	2578.0
8640	0.03201257	-828.9707	92373450	46931263	46949267	2577.0
8680	0.03201851	-828.9707	92389986	46931263	46949267	2576.0
8720	0.03202445	-828.9707	92406722	46931263	46949267	2575.0
8760	0.03203039	-828.9707	92423458	46931263	46949267	2574.0
8800	0.03203633	-828.9707	92439994	46931263	46949267	2573.0
8840	0.03204227	-828.9707	92456730	46931263	46949267	2572.0
8880	0.03204821	-828.9707	92473466	46931263	46949267	2571.0
8920	0.03205415	-828.9707	92489992	46931263	46949267	2570.0
8960	0.03206009	-828.9707	92506728	46931263	46949267	2569.0
9000	0.03206603	-828.9707	92523464	46931263	46949267	2568.0
9040	0.03207197	-828.9707	92539990	46931263	46949267	2567.0
9080	0.03207791	-828.9707	92556726	46931263	46949267	2566.0
9120	0.03208385	-828.9707	92573462	46931263	46949267	2565.0
9160	0.03208979	-828.9707	92590198	46931263	46949267	2564.0
9200	0.03209573	-828.9707	92606934	46931263	46949267	2563.0
9240	0.03210167	-828.9707	92623670	46931263	46949267	2562.0
9280	0.03210761	-828.9707	92640406	46931263	46949267	2561.0
9320	0.03211355	-828.9707	92657142	46931263	46949267	2560.0
9360	0.03211949	-828.9707	92673878	46931263	46949267	2559.0

Table 3-5b (continued)

Table 3-5b (continued)

PRESSURE PSIA	VOLUME FT <sup>3</sup> /LBM	ENTHALPY BTU/LBM	ENTROPY BTU/LBM/DEG F	CP BTU/LBM/DEG F	CV BTU/LBM/DEG F	SONIC VELOCITY FT/SEC
560.	0.03290205	-302.0733016	94.979112	45355007	42549220	2347.9174
540.	0.03292464	-809.092975	94.979834	4531371	42535693	2340.8426
520.	0.03294783	-309.112453	95.013714	4521371	42533296	2333.7295
500.	0.03297103	-809.131261	95.026986	45165656	42531978	2326.5966
490.	0.03299444	-903.146227	95.026988	45165554	42531244	2321.0554
460.	0.03118066	-809.167400	95.026982	45162267	42531204	2314.8835
440.	0.03114911	-809.180126	95.016187	45162297	42529702	2290.2150
420.	0.03120698	-809.20126	95.016197	45162282	42528202	2282.8175
400.	0.03126027	-809.217251	95.016197	45162267	42526000	2267.0363
380.	0.03130362	-805.232671	95.016197	45162245	42524500	2245.1608
360.	0.03134807	-805.247473	95.016197	45162229	42522244	2222.2244
340.	0.03139535	-809.261645	95.016197	45162214	42521500	2214.0188
320.	0.03143535	-809.275173	95.016197	45162175	42520900	2198.3997
300.	0.03147112	-805.280246	95.016197	45162139	42520400	2190.4267
280.	0.03150665	-809.286065	95.016197	45162094	42519800	2198.3997
260.	0.03153633	-809.293016	95.016197	45162055	42519200	2192.0628
240.	0.03156448	-809.302468	95.016197	45162016	42518600	2186.9933
220.	0.03159333	-809.311764	95.016197	45161976	42518000	2180.9933
200.	0.03162204	-809.322562	95.016197	45161937	42517400	2174.8862
180.	0.03164506	-809.334264	95.016197	45161898	42516800	2168.8862
160.	0.03166740	-809.345966	95.016197	45161859	42516200	2162.8862
140.	0.03168906	-809.358823	95.016197	45161820	42515600	2156.8862
120.	0.03171515	-809.371224	95.016197	45161781	42515000	2150.8862
100.	0.03174080	-809.384633	95.016197	45161742	42514400	2144.8862
80.	0.03176458	-809.398044	95.016197	45161703	42513800	2138.8862
60.	0.03178983	-809.411455	95.016197	45161664	42513200	2132.8862
50.	0.03181569	-809.424863	95.016197	45161625	42512600	2126.8862
40.	0.03184263	-802.438160	95.016197	45161586	42512000	2120.8862
30.	0.03186955	-802.451560	95.016197	45161547	42511400	2114.8862
20.	0.03189547	-802.464955	95.016197	45161508	42507900	2079.8862
10.	0.03192147	-802.478350	95.016197	45161469	42504400	2044.8862
5.	0.03193547	-802.489796	95.016197	45161430	42501900	2019.8862
2.	0.03194950	-802.501390	95.016197	45161391	42500400	2004.8862
1.	0.03195950	-802.512983	95.016197	45161352	42500000	2000.8862
0.	0.03196950	-802.524576	95.016197	45161313	42500000	2000.8862

Table 3-5b (continued)

TEMPERATURE = 100 DEG F						TEMPERATURE = 110 DEG F						TEMPERATURE = 120 DEG F					
PRESSURE	VOLUME	ENTHALPY	ENTROPY	BTU/LBM	BTU/LBM/DEG F	PRESSURE	VOLUME	ENTHALPY	ENTROPY	BTU/LBM	BTU/LBM/DEG F	PRESSURE	VOLUME	ENTHALPY	ENTROPY	BTU/LBM	BTU/LBM/DEG F
PSIA	FT <sup>3</sup> /LBM	BTU/LBM	BTU/LBM/DEG F	BTU/LBM/DEG F	BTU/LBM/DEG F	PSIA	FT <sup>3</sup> /LBM	BTU/LBM	BTU/LBM/DEG F	BTU/LBM/DEG F	BTU/LBM/DEG F	PSIA	FT <sup>3</sup> /LBM	BTU/LBM	BTU/LBM/DEG F	BTU/LBM/DEG F	BTU/LBM/DEG F
440.	341.9575	-795.924459	-975.939000	• 975.939000	• 975.939000	540.	342.2795	-795.923984	-975.923984	• 975.923984	• 975.923984	540.	342.6106	-795.922459	-975.922459	• 975.922459	• 975.922459
420.	342.6106	-795.922459	-975.922459	• 975.922459	• 975.922459	520.	342.9459	-795.921652	-975.921652	• 975.921652	• 975.921652	520.	343.2855	-795.920537	-975.920537	• 975.920537	• 975.920537
400.	343.2855	-795.920537	-975.920537	• 975.920537	• 975.920537	500.	343.6785	-795.919748	-975.919748	• 975.919748	• 975.919748	500.	344.07318	-795.919034	-975.919034	• 975.919034	• 975.919034
380.	344.07318	-795.919034	-975.919034	• 975.919034	• 975.919034	480.	344.46901	-795.918459	-975.918459	• 975.918459	• 975.918459	480.	344.86500	-795.917984	-975.917984	• 975.917984	• 975.917984
360.	344.86500	-795.917984	-975.917984	• 975.917984	• 975.917984	460.	345.2534	-795.917537	-975.917537	• 975.917537	• 975.917537	460.	345.6520	-795.917091	-975.917091	• 975.917091	• 975.917091
340.	345.6520	-795.917091	-975.917091	• 975.917091	• 975.917091	440.	346.0500	-795.916659	-975.916659	• 975.916659	• 975.916659	440.	346.44801	-795.916234	-975.916234	• 975.916234	• 975.916234
320.	346.44801	-795.916234	-975.916234	• 975.916234	• 975.916234	420.	346.84601	-795.915818	-975.915818	• 975.915818	• 975.915818	420.	347.24401	-795.915412	-975.915412	• 975.915412	• 975.915412
300.	347.24401	-795.915412	-975.915412	• 975.915412	• 975.915412	400.	347.64200	-795.915016	-975.915016	• 975.915016	• 975.915016	400.	348.04000	-795.914620	-975.914620	• 975.914620	• 975.914620
280.	348.04000	-795.914620	-975.914620	• 975.914620	• 975.914620	380.	348.43800	-795.914224	-975.914224	• 975.914224	• 975.914224	380.	348.83600	-795.913830	-975.913830	• 975.913830	• 975.913830
260.	348.83600	-795.913830	-975.913830	• 975.913830	• 975.913830	360.	349.23400	-795.913434	-975.913434	• 975.913434	• 975.913434	360.	349.63200	-795.913040	-975.913040	• 975.913040	• 975.913040
240.	349.63200	-795.913040	-975.913040	• 975.913040	• 975.913040	340.	350.03000	-795.912645	-975.912645	• 975.912645	• 975.912645	340.	350.42800	-795.912251	-975.912251	• 975.912251	• 975.912251
220.	350.42800	-795.912251	-975.912251	• 975.912251	• 975.912251	320.	350.82600	-795.911856	-975.911856	• 975.911856	• 975.911856	320.	351.22400	-795.911462	-975.911462	• 975.911462	• 975.911462
200.	351.22400	-795.911462	-975.911462	• 975.911462	• 975.911462	300.	351.62200	-795.911067	-975.911067	• 975.911067	• 975.911067	300.	352.02000	-795.910673	-975.910673	• 975.910673	• 975.910673
180.	352.02000	-795.910673	-975.910673	• 975.910673	• 975.910673	280.	352.41800	-795.909278	-975.909278	• 975.909278	• 975.909278	280.	352.81600	-795.908884	-975.908884	• 975.908884	• 975.908884
160.	352.81600	-795.908884	-975.908884	• 975.908884	• 975.908884	260.	353.21400	-795.908489	-975.908489	• 975.908489	• 975.908489	260.	353.61200	-795.908095	-975.908095	• 975.908095	• 975.908095
140.	353.61200	-795.908095	-975.908095	• 975.908095	• 975.908095	240.	354.01000	-795.907699	-975.907699	• 975.907699	• 975.907699	240.	354.40800	-795.907305	-975.907305	• 975.907305	• 975.907305
120.	354.40800	-795.907305	-975.907305	• 975.907305	• 975.907305	220.	354.79600	-795.906911	-975.906911	• 975.906911	• 975.906911	220.	355.19400	-795.906517	-975.906517	• 975.906517	• 975.906517
100.	355.19400	-795.906517	-975.906517	• 975.906517	• 975.906517	200.	355.59200	-795.906123	-975.906123	• 975.906123	• 975.906123	200.	355.99000	-795.905729	-975.905729	• 975.905729	• 975.905729
80.	355.99000	-795.905729	-975.905729	• 975.905729	• 975.905729	180.	356.38800	-795.905335	-975.905335	• 975.905335	• 975.905335	180.	356.78600	-795.904941	-975.904941	• 975.904941	• 975.904941
60.	356.78600	-795.904941	-975.904941	• 975.904941	• 975.904941	160.	357.18400	-795.904547	-975.904547	• 975.904547	• 975.904547	160.	357.58200	-795.904153	-975.904153	• 975.904153	• 975.904153
40.	357.58200	-795.904153	-975.904153	• 975.904153	• 975.904153	140.	357.98000	-795.903759	-975.903759	• 975.903759	• 975.903759	140.	358.37800	-795.903365	-975.903365	• 975.903365	• 975.903365
20.	358.37800	-795.903365	-975.903365	• 975.903365	• 975.903365	100.	358.77600	-795.902971	-975.902971	• 975.902971	• 975.902971	100.	359.17400	-795.902577	-975.902577	• 975.902577	• 975.902577
0.	359.17400	-795.902577	-975.902577	• 975.902577	• 975.902577	0.	359.57200	-795.902183	-975.902183	• 975.902183	• 975.902183	0.	359.97000	-795.901789	-975.901789	• 975.901789	• 975.901789

Table 3-5b (continued)

PRESSURE PSIA	VOLUME FT <sup>3</sup> /LB <sup>3</sup> M	BTU/LB <sup>3</sup> M	BTU/LB <sup>3</sup> M/DEG F	STU/LB <sup>3</sup> M/DEG F	3TU/LB <sup>3</sup> M/DEG F	FT/SEC	SONIC VELOCITY FT/SEC		
							CV	BTU/LB <sup>3</sup> M/DEG F	BTU/LB <sup>3</sup> M/DEG F
TEMPERATURE = 130 DEG F									
PRESSURE PSIA	VOLUME FT <sup>3</sup> /LB <sup>3</sup> M	ENTHALAPY BTU/LBM	ENTROPY BTU/LBM/DEG F	CP BTU/LBM/DEG F	CV BTU/LBM	BTU/LBM/DEG F	BTU/LBM/DEG F	BTU/LBM/DEG F	
560.	.036083338	1.00098764	1.0211671	1.0220980	1.0217691	1.0371720	1.04368516	1.04912729	
560.	.036083468	-775.753655	1.00104616	1.0224323	1.0227759	1.0376253	1.044880281	1.04906523	
560.	.03613695	-775.681400	1.00104616	1.0227748	1.0230427	1.0376559	1.044884028	1.04904520	
560.	.0361821	-775.642127	1.00104628	1.0230325	1.0233034	1.0376852	1.044884028	1.04903517	
560.	.03624452	-775.605649	1.00113698	1.0233476	1.0236246	1.0377152	1.044884028	1.04902516	
560.	.03628992	-775.566877	1.00116812	1.0236587	1.0239567	1.0377452	1.044884028	1.04901515	
560.	.03635645	-775.521071	1.00119974	1.0240297	1.0243657	1.0377752	1.044884028	1.04900514	
560.	.03641418	-775.482065	1.00123183	1.0243643	1.0247627	1.0378052	1.044884028	1.04899513	
560.	.03647324	-775.441031	1.00126443	1.0247956	1.0251936	1.0378352	1.044884028	1.04898512	
560.	.03653340	-775.403567	1.00129756	1.0252097	1.0255346	1.0378652	1.044884028	1.04897511	
560.	.03659503	-775.365561	1.00132124	1.0255839	1.0258756	1.0378952	1.044884028	1.04896510	
560.	.03665809	-775.324565	1.00135155	1.0260339	1.0262656	1.0379252	1.044884028	1.04895529	
560.	.03672264	-775.284721	1.00140036	1.0263036	1.0265587	1.0379552	1.044884028	1.04894528	
560.	.03678879	-775.241709	1.00143586	1.0265739	1.0268498	1.0379852	1.044884028	1.04893527	
560.	.03685660	-775.200696	1.00147202	1.0268038	1.0270998	1.0408783	1.045073541	1.046668313	
560.	.03692617	-775.160519	1.00147202	1.0270998	1.0273028	1.0409265	1.04508264	1.046668313	
TEMPERATURE = 130 DEG F									
PRESSURE PSIA	VOLUME FT <sup>3</sup> /LB <sup>3</sup> M	ENTHALAPY BTU/LBM	ENTROPY BTU/LBM/DEG F	CP BTU/LBM/DEG F	CV BTU/LBM	BTU/LBM/DEG F	BTU/LBM/DEG F	BTU/LBM/DEG F	
560.	.03686178	-768.797294	1.02117691	1.0220980	1.0227722	1.0376284	1.045030892	1.04912729	
560.	.03692514	-768.759316	1.02117691	1.0227722	1.0231179	1.0376594	1.045045065	1.04911919	
560.	.03705637	-768.721037	1.021234699	1.0232823	1.0236282	1.0376862	1.045053082	1.04911919	
560.	.03712423	-768.685917	1.021234699	1.0232823	1.0238101	1.0377166	1.045062976	1.04910824	
560.	.03719396	-768.649210	1.021234699	1.0232823	1.0241935	1.0377452	1.045072056	1.04909717	
560.	.03726525	-768.604986	1.021241935	1.02341935	1.0244782	1.0377752	1.045082706	1.04908694	
560.	.03733578	-768.561096	1.021241935	1.02341935	1.0246568	1.0378052	1.04509292	1.04907686	
560.	.03749114	-768.516378	1.021249457	1.02349457	1.0249457	1.0378352	1.045102806	1.04906695	
560.	.03756762	-768.471435	1.021253355	1.02353355	1.02527297	1.0378652	1.045112705	1.04905685	
560.	.03763716	-768.426649	1.021261349	1.02361349	1.0256261349	1.0378952	1.045122604	1.04904685	
560.	.03770743	-768.381595	1.021261349	1.02361349	1.026261349	1.0379252	1.045132503	1.04903675	
560.	.03777743	-768.337165	1.021261349	1.02361349	1.026261349	1.0379552	1.045142402	1.04902665	
TEMPERATURE = 140 DEG F									
PRESSURE PSIA	VOLUME FT <sup>3</sup> /LB <sup>3</sup> M	ENTHALAPY BTU/LBM	ENTROPY BTU/LBM/DEG F	CP BTU/LBM/DEG F	CV BTU/LBM	BTU/LBM/DEG F	BTU/LBM/DEG F	BTU/LBM/DEG F	
560.	.03780818	-761.643043	1.0337936	1.0341746	1.0345635	1.04337389	1.04748653	1.05337389	
560.	.03789716	-761.605417	1.0341746	1.0345635	1.0349603	1.043414266	1.047514372	1.0437514372	
560.	.03805702	-761.563979	1.0349603	1.0349603	1.0352931	1.043512387	1.047521387	1.0437521387	
560.	.03814500	-761.521326	1.0352931	1.0352931	1.0356216	1.043521326	1.047531326	1.0437531326	
560.	.03823578	-761.481368	1.0356216	1.0356216	1.0357625	1.0435280797	1.047541368	1.0437541368	
560.	.03832955	-761.440493	1.03562081	1.03562081	1.035864265	1.04352700536	1.0475504265	1.04375504265	
560.	.03842695	-760.972054	1.03562081	1.03562081	1.035864265	1.04352700536	1.0475504265	1.04375504265	
560.	.03853109	-760.938366	1.0357920	1.0357920	1.035864265	1.04352700536	1.0475504265	1.04375504265	
560.	.03863127	-760.89251	1.0357920	1.0357920	1.035864265	1.04352700536	1.0475504265	1.04375504265	
560.	.03888183	-760.85123	1.0358625	1.0358625	1.035882089	1.04352700536	1.0475504265	1.04375504265	
TEMPERATURE = 150 DEG F									
PRESSURE PSIA	VOLUME FT <sup>3</sup> /LB <sup>3</sup> M	ENTHALAPY BTU/LBM	ENTROPY BTU/LBM/DEG F	CP BTU/LBM/DEG F	CV BTU/LBM	BTU/LBM/DEG F	BTU/LBM/DEG F	BTU/LBM/DEG F	
560.	.03780818	-761.643043	1.0337936	1.0341746	1.0345635	1.04337389	1.04748653	1.05337389	
560.	.03789716	-761.605417	1.0341746	1.0345635	1.0349603	1.043414266	1.047514372	1.0437514372	
560.	.03805702	-761.563979	1.0349603	1.0349603	1.0352931	1.043512387	1.047521387	1.0437521387	
560.	.03814500	-761.521326	1.0352931	1.0352931	1.0356216	1.043521326	1.047531326	1.0437531326	
560.	.03823578	-761.481368	1.0356216	1.0356216	1.0357625	1.0435280797	1.047541368	1.0437541368	
560.	.03832955	-761.440493	1.03562081	1.03562081	1.035864265	1.04352700536	1.0475504265	1.04375504265	
560.	.03842695	-760.972054	1.0357920	1.0357920	1.035864265	1.04352700536	1.0475504265	1.04375504265	
560.	.03853109	-760.938366	1.0357920	1.0357920	1.035864265	1.04352700536	1.0475504265	1.04375504265	
560.	.03863127	-760.89251	1.0358625	1.0358625	1.035882089	1.04352700536	1.0475504265	1.04375504265	
560.	.03888183	-760.85123	1.0358625	1.0358625	1.035882089	1.04352700536	1.0475504265	1.04375504265	

Table 3-5b (continued)

560.	.038919C5	-754.214246	1.0460726	*44192630
540.	.039018C3	-754.08033C	1.0460727	*44192645
520.	.039136C3	-753.939126	1.04607273	*44201245
500.	.039251C8	-753.790066	1.04607276	*44201247
480.	.039371C5	-753.632512	1.04607277	*44201247
460.	.039496E7	-753.463277	1.04607278	*44201247
440.	.03962734	-753.288916	1.04607279	*44201247
420.	.039764C2	-753.101090	1.04607280	*44201247
400.	.03990793	-752.901153	1.04607281	*44201247
380.	.0400C694	-752.667809	1.04607282	*44201247
360.	.04021942	-752.459525	1.04607283	*44201247

TEMPERATURE=160 DEG F

PRESSURE PSIA	VOLUME FT <sup>3</sup> /LBM	ENTHALAPY BTU/LBM	ENTROPY BTU/LBM/DEG F	CP BTU/LBM/DEG F	CV BTU/LBM/DEG F	SONIC VELOCITY FT/SEC
560.	.04027499	-746.192277	1.0597973	*46C67781	*44712C17	1453.9733
540.	.04042554	-746.192277	1.0593708	*46066811	*4476831	1427.9996
520.	.040564C0	-745.262330	1.059670C	*46C666665	*44743C25	1414.6101
500.	.0407130	-745.72732	1.0605082	*46D67566	*44760765	1405.9228
480.	.04092854	-745.206443	1.0612373	*46D68655	*448C1270	1396.9110
460.	.04111706	-745.206443	1.0619178	*46D73144	*44802547C	1372.5431
440.	.0413851	-744.8159216	1.0623338	*46D78228	*448051863	1357.5780
420.	.04153491	-744.8159216	1.0633906	*46D851410	*448081362	13342.5768
400.	.04176887	-744.254855	1.0641947			

TEMPERATURE=170 DEG F

PRESSURE PSIA	VOLUME FT <sup>3</sup> /LBM	ENTHALAPY BTU/LBM	ENTROPY BTU/LBM/DEG F	CP BTU/LBM/DEG F	CV BTU/LBM/DEG F	SONIC VELOCITY FT/SEC
560.	.04203613	-737.938566	1.0723157	*46573849	*45328011	1355.4C27
540.	.04227177	-737.630228	1.07310C4	*46586505	*45368499	1341.0C24
520.	.04256682	-736.823165	1.0739347	*4661756	*45391756	1326.3622
500.	.04280496	-736.823165	1.0748273	*466171217	*45442318	1312.1917
480.	.04311110	-736.379909	1.0757897	*46638308	*45471729	1295.5050
460.	.04345196	-735.880115	1.0768373	*466664277	*45520134	1279.2150

TEMPERATURE=180 DEG F

PRESSURE PSIA	VOLUME FT <sup>3</sup> /LBM	ENTHALAPY BTU/LBM	ENTROPY BTU/LBM/DEG F	CP BTU/LBM/DEG F	CV BTU/LBM/DEG F	SONIC VELOCITY FT/SEC
560.	.04460919	-728.336946	1.0874339	*47233229	*46097407	1258.9839
540.	.04506207	-727.682953	1.0887151	*4727484	*46164594	1238.6836
520.	.04559665	-726.92144	1.0901660	*47332528	*46244212	1220.6825
500.	.04624116	-726.01113	1.0918550	*474C3C43	*46341402	121C1.8736

TEMPERATURE=190 DEG F

PRESSURE PSIA	VOLUME FT <sup>3</sup> /LBM	ENTHALAPY BTU/LBM	ENTROPY BTU/LBM/DEG F	CP BTU/LBM/DEG F	CV BTU/LBM/DEG F	SONIC VELOCITY FT/SEC
560.	.04972073	-715.596783	1.1073151	*48276165	*4725C342	1144.3225
540.	.0517C479	-713.015848	1.1114356	*48523237	*47524971	1116.6933

Table 3-5b (continued)

PRESSURE PSIA	VOLUME FT <sup>3</sup> /LBM	ENTHALPY BTU/LBM	ENTROPY BTU/LBM/DEG F	CP BTU/LBM/DEG F	CV BTU/LBM/DEG F	SONIC VELOCITY FT/SEC
560.	.214046336	-6653.710960	1.2017890	.52458429	.48855772	567.3130
540.	.215812786	-6448.597800	1.2103744	.52672264	.48478054	557.2793

### THERMODYNAMIC PROPERTIES OF PROPANE AS PREDICTED BY STARLING'S EQUATION OF STATE

Table 3-6a

**Saturation Temperature Table for Propane Calculated from Starling's Equation of State.**

Table 3-6a (continued)

Table 3-6a (continued)

## THERMODYNAMIC PROPERTIES OF PROPANE AS PREDICTED BY STARLING'S EQUATION OF STATE

Table 3-6a (continued)

121.31	4286126963	4167299306	375133012	2243.433897	696.661904
124.90	4296097404	4177799210	3768287781	2224.17288	695.117555
128.54	430946494	418316095	3784870912	2204.78733	693.722329
132.84	4315774212	419886594	3784870912	2204.78733	693.722329
136.91	4326874120	420169496	3784870912	2204.78733	693.722329
140.41	435125435	4205040	3784870912	2204.78733	693.722329
144.82	4355468615	4205040	3784870912	2204.78733	693.722329
148.23	437596194	4205040	3784870912	2204.78733	693.722329
152.65	43943289	4205040	3784870912	2204.78733	693.722329
156.06	440430204	4205040	3784870912	2204.78733	693.722329
160.47	442302695	4205040	3784870912	2204.78733	693.722329
164.88	444218560	4205040	3784870912	2204.78733	693.722329
169.29	446285629	4205040	3784870912	2204.78733	693.722329
173.70	448342184	4205040	3784870912	2204.78733	693.722329
177.11	450383425	4205040	3784870912	2204.78733	693.722329
180.52	452449356	4205040	3784870912	2204.78733	693.722329
184.93	454507767	4205040	3784870912	2204.78733	693.722329
188.34	456562295	4205040	3784870912	2204.78733	693.722329
192.75	458627495	4205040	3784870912	2204.78733	693.722329
197.16	460675921	4205040	3784870912	2204.78733	693.722329
201.57	462716405	4205040	3784870912	2204.78733	693.722329
205.98	464776214	4205040	3784870912	2204.78733	693.722329
210.40	466834817	4205040	3784870912	2204.78733	693.722329
214.81	468896480	4205040	3784870912	2204.78733	693.722329
219.22	470952857	4205040	3784870912	2204.78733	693.722329
223.63	473051407	4205040	3784870912	2204.78733	693.722329
228.04	475117047	4205040	3784870912	2204.78733	693.722329
232.45	477180267	4205040	3784870912	2204.78733	693.722329
236.86	479246713	4205040	3784870912	2204.78733	693.722329
241.27	481313867	4205040	3784870912	2204.78733	693.722329
245.68	483385713	4205040	3784870912	2204.78733	693.722329
250.09	485451662	4205040	3784870912	2204.78733	693.722329
254.50	487513620	4205040	3784870912	2204.78733	693.722329
258.91	489575028	4205040	3784870912	2204.78733	693.722329
263.32	491644466	4205040	3784870912	2204.78733	693.722329
267.73	493712024	4205040	3784870912	2204.78733	693.722329
272.14	495776750	4205040	3784870912	2204.78733	693.722329
276.55	497834024	4205040	3784870912	2204.78733	693.722329
280.96	499896396	4205040	3784870912	2204.78733	693.722329
285.37	501934944	4205040	3784870912	2204.78733	693.722329
289.78	503984718	4205040	3784870912	2204.78733	693.722329
294.19	505947656	4205040	3784870912	2204.78733	693.722329
298.60	507905205	4205040	3784870912	2204.78733	693.722329
303.01	509861784	4205040	3784870912	2204.78733	693.722329
307.42	511825364	4205040	3784870912	2204.78733	693.722329
311.83	513781944	4205040	3784870912	2204.78733	693.722329
316.24	515736536	4205040	3784870912	2204.78733	693.722329
320.65	517703093	4205040	3784870912	2204.78733	693.722329
325.06	519659369	4205040	3784870912	2204.78733	693.722329
329.47	521615937	4205040	3784870912	2204.78733	693.722329
333.88	523574597	4205040	3784870912	2204.78733	693.722329
338.29	525532156	4205040	3784870912	2204.78733	693.722329
342.70	527500715	4205040	3784870912	2204.78733	693.722329
347.11	529468294	4205040	3784870912	2204.78733	693.722329
351.52	531435852	4205040	3784870912	2204.78733	693.722329
355.93	533403411	4205040	3784870912	2204.78733	693.722329
360.34	535371070	4205040	3784870912	2204.78733	693.722329
364.75	537338630	4205040	3784870912	2204.78733	693.722329
369.16	539306139	4205040	3784870912	2204.78733	693.722329
373.57	541273798	4205040	3784870912	2204.78733	693.722329
378.98	543241357	4205040	3784870912	2204.78733	693.722329
383.39	545208916	4205040	3784870912	2204.78733	693.722329
387.80	547176475	4205040	3784870912	2204.78733	693.722329
392.21	549143934	4205040	3784870912	2204.78733	693.722329
396.62	551111493	4205040	3784870912	2204.78733	693.722329
401.03	553078952	4205040	3784870912	2204.78733	693.722329
405.44	555046511	4205040	3784870912	2204.78733	693.722329
409.85	557013970	4205040	3784870912	2204.78733	693.722329
414.26	559081529	4205040	3784870912	2204.78733	693.722329
418.67	561049088	4205040	3784870912	2204.78733	693.722329
423.08	563016647	4205040	3784870912	2204.78733	693.722329
427.49	565084206	4205040	3784870912	2204.78733	693.722329
431.90	567051765	4205040	3784870912	2204.78733	693.722329
436.31	569019324	4205040	3784870912	2204.78733	693.722329
440.72	571086883	4205040	3784870912	2204.78733	693.722329
445.13	573054442	4205040	3784870912	2204.78733	693.722329
449.54	575021992	4205040	3784870912	2204.78733	693.722329
453.95	577088551	4205040	3784870912	2204.78733	693.722329
458.36	579056110	4205040	3784870912	2204.78733	693.722329
462.77	581023669	4205040	3784870912	2204.78733	693.722329
467.18	583001228	4205040	3784870912	2204.78733	693.722329
471.59	585068787	4205040	3784870912	2204.78733	693.722329
475.99	587036346	4205040	3784870912	2204.78733	693.722329
480.40	589003895	4205040	3784870912	2204.78733	693.722329
484.81	591071454	4205040	3784870912	2204.78733	693.722329
489.22	593039094	4205040	3784870912	2204.78733	693.722329
493.63	595006653	4205040	3784870912	2204.78733	693.722329
498.04	597074212	4205040	3784870912	2204.78733	693.722329
502.45	599041871	4205040	3784870912	2204.78733	693.722329
506.86	601006430	4205040	3784870912	2204.78733	693.722329
511.27	603073989	4205040	3784870912	2204.78733	693.722329
515.68	605041548	4205040	3784870912	2204.78733	693.722329
519.09	607009107	4205040	3784870912	2204.78733	693.722329
523.50	609076666	4205040	3784870912	2204.78733	693.722329
527.91	611044225	4205040	3784870912	2204.78733	693.722329
532.32	613011884	4205040	3784870912	2204.78733	693.722329
536.73	615080443	4205040	3784870912	2204.78733	693.722329
541.14	617047002	4205040	3784870912	2204.78733	693.722329
545.55	618014561	4205040	3784870912	2204.78733	693.722329
549.96	620082121	4205040	3784870912	2204.78733	693.722329
554.37	622059680	4205040	3784870912	2204.78733	693.722329
558.78	624037239	4205040	3784870912	2204.78733	693.722329
563.19	626014898	4205040	3784870912	2204.78733	693.722329
567.60	628012557	4205040	3784870912	2204.78733	693.722329
572.01	630083216	4205040	3784870912	2204.78733	693.722329
576.42	632050875	4205040	3784870912	2204.78733	693.722329
580.83	634028444	4205040	3784870912	2204.78733	693.722329
585.24	636006013	4205040	3784870912	2204.78733	693.722329
589.65	638003672	4205040	3784870912	2204.78733	693.722329
594.06	640001231	4205040	3784870912	2204.78733	693.722329
598.47	642008791	4205040	3784870912	2204.78733	693.722329
602.88	644006350	4205040	3784870912	2204.78733	693.722329
607.29	646003909	4205040	3784870912	2204.78733	693.722329
611.70	648001568	4205040	3784870912	2204.78733	693.722329
616.11	650009238	4205040	3784870912	2204.78733	693.722329
620.52	653006807	4205040	3784870912	2204.78733	693.722329
624.93	656004407	4205040	3784870912	2204.78733	693.722329
629.34	659002036	4205040	3784870912	2204.78733	693.722329
633.75	662000605	4205040	3784870912	2204.78733	693.722329
638.16	665000274	4205040	3784870912	2204.78733	693.722329
642.57	668000943	4205040	3784870912	2204.78733	693.722329
647.00	671000612	4205040	3784870912	2204.78733	693.722329
651.41	674000381	4205040	3784870912	2204.78733	693.722329
655.82	677000050	4205040	3784870912	2204.78733	693.722329
660.23	680000719	4205040	3784870912	2204.78733	693.722329
664.64	683000388	4205040	3784870912	2204.78733	693.722329
669.05	686000057	4205040	3784870912	2204.78733	693.722329
673.46	689000746	4205040	3784870912	2204.78733	693.722329
677.87	692000416</				

THERMODYNAMIC PROPERTIES OF PROPANE AS PREDICTED BY STARLING'S EQUATION OF STATE

TEMPERATURE = -30 DEG F

PRESSURE PSIA	VOLUME FT <sup>3</sup> /LB M	ENTHALAPY BTU/LB M	ENTROPY BTU/LBM/DEG F	CP BTU/LBM/DEG F	CV BTU/LBM/DEG F	SONIC VELOCITY FT/SEC
560.	.02831413	-871.882226	82232591	82242595	82242595	3249.4854
540.	.02832139	-871.882224	82232593	82242597	82242597	3249.4854
520.	.02832868	-871.942545	82232594	82242598	82242598	3249.4854
500.	.02833592	-872.0123034	82232596	82242600	82242600	3249.4854
480.	.02834326	-872.0822245	82232597	82242601	82242601	3249.4854
460.	.02835056	-872.1423034	82232598	82242602	82242602	3249.4854
440.	.02835787	-872.2123034	82232599	82242603	82242603	3249.4854
420.	.02836514	-872.28228416	82232600	82242604	82242604	3249.4854
400.	.02837241	-872.35228416	82232601	82242605	82242605	3249.4854
380.	.02837969	-872.42228416	82232602	82242606	82242606	3249.4854
360.	.02838705	-872.49228416	82232603	82242607	82242607	3249.4854
340.	.02839438	-872.56228416	82232604	82242608	82242608	3249.4854
320.	.02840172	-872.63228416	82232605	82242609	82242609	3249.4854
300.	.02840907	-872.70228416	82232606	82242610	82242610	3249.4854
280.	.02841642	-872.77228416	82232607	82242611	82242611	3249.4854
260.	.02842377	-872.84228416	82232608	82242612	82242612	3249.4854
240.	.02843112	-872.91228416	82232609	82242613	82242613	3249.4854
220.	.02843847	-872.98228416	82232610	82242614	82242614	3249.4854
200.	.02844582	-873.05228416	82232611	82242615	82242615	3249.4854
180.	.02845317	-873.12228416	82232612	82242616	82242616	3249.4854
160.	.02846052	-873.19228416	82232613	82242617	82242617	3249.4854
140.	.02846787	-873.26228416	82232614	82242618	82242618	3249.4854
120.	.02847522	-873.33228416	82232615	82242619	82242619	3249.4854
100.	.02848257	-873.40228416	82232616	82242620	82242620	3249.4854
80.	.02848992	-873.47228416	82232617	82242621	82242621	3249.4854
60.	.02850732	-873.54228416	82232618	82242622	82242622	3249.4854
40.	.02851531	-873.61228416	82232619	82242623	82242623	3249.4854
30.	.02851531	-873.68228416	82232620	82242624	82242624	3249.4854

TEMPERATURE = -20 DEG F

PRESSURE PSIA	VOLUME FT <sup>3</sup> /LB M	ENTHALAPY BTU/LB M	ENTROPY BTU/LBM/DEG F	CP BTU/LBM/DEG F	CV BTU/LBM/DEG F	SONIC VELOCITY FT/SEC
560.	.02659705	-866.428985	8347749	8349814	8349814	315.5326
540.	.02660505	-866.498015	8349881	8350951	8350951	315.5326
520.	.02661299	-866.564564	8350951	8352024	8352024	315.5326
500.	.02662100	-866.632324	8352024	8353154	8353154	315.5326
480.	.02662904	-866.701624	8353154	8354124	8354124	315.5326
460.	.02663711	-866.771024	8354124	8355138	8355138	315.5326
440.	.02664521	-866.840324	8355138	8356158	8356158	315.5326
420.	.02665334	-866.909624	8356158	8357161	8357161	315.5326
400.	.02666145	-866.988924	8357161	8358184	8358184	315.5326
380.	.02666959	-867.068224	8358184	8359207	8359207	315.5326
360.	.02667471	-867.137524	8359207	8360231	8360231	315.5326
340.	.02668285	-867.206824	8360231	8361254	8361254	315.5326
320.	.02668962	-867.276124	8361254	8362287	8362287	315.5326
300.	.02669619	-867.345424	8362287	8363320	8363320	315.5326
280.	.02670274	-867.414724	8363320	8364353	8364353	315.5326
260.	.02670927	-867.484024	8364353	8365386	8365386	315.5326
240.	.02671578	-867.553324	8365386	8366419	8366419	315.5326
220.	.02672230	-867.622624	8366419	8367453	8367453	315.5326
200.	.02672881	-867.691924	8367453	8368582	8368582	315.5326
180.	.02673534	-867.761224	8368582	8369619	8369619	315.5326
160.	.02674187	-867.830524	8369619	8370656	8370656	315.5326
140.	.02674840	-867.900824	8370656	8371619	8371619	315.5326
120.	.02675493	-867.970124	8371619	8372608	8372608	315.5326
100.	.02676147	-868.040424	8372608	8373645	8373645	315.5326
80.	.02676700	-868.110724	8373645	8374682	8374682	315.5326
60.	.02677353	-868.181024	8374682	8375719	8375719	315.5326
40.	.02677906	-868.251324	8375719	8376755	8376755	315.5326
30.	.02678459	-868.321624	8376755	8377802	8377802	315.5326

Table 3-6b (continued)

Table 3-6b (continued)

PRESSURE PSIA	VOLUME FT <sup>3</sup> /LBM	ENTHALPY BTU/LBM	CP BTU/LBM/DEG F	ENTROPY BTU/LBM/DEG F	CV BTU/LBM/DEG F	SONIC VELOCITY FT/SEC
220.	560.	-844.344739	-844.344739	-844.344739	-844.344739	3800.6923
240.	540.	-844.346313	-844.346313	-844.346313	-844.346313	3885.7802
260.	520.	-844.347818	-844.347818	-844.347818	-844.347818	3884.0191
280.	500.	-844.349372	-844.349372	-844.349372	-844.349372	3888.31372
300.	480.	-844.350914	-844.350914	-844.350914	-844.350914	3888.31544
320.	460.	-844.352454	-844.352454	-844.352454	-844.352454	3888.13708
340.	440.	-844.353987	-844.353987	-844.353987	-844.353987	3888.13779
360.	420.	-844.355519	-844.355519	-844.355519	-844.355519	3888.13779
380.	400.	-844.357051	-844.357051	-844.357051	-844.357051	3888.13779
400.	380.	-844.358583	-844.358583	-844.358583	-844.358583	3888.13779
420.	360.	-844.360115	-844.360115	-844.360115	-844.360115	3888.13779
440.	340.	-844.361647	-844.361647	-844.361647	-844.361647	3888.13779
460.	320.	-844.363179	-844.363179	-844.363179	-844.363179	3888.13779
480.	300.	-844.364711	-844.364711	-844.364711	-844.364711	3888.13779
500.	280.	-844.366243	-844.366243	-844.366243	-844.366243	3888.13779
520.	260.	-844.367775	-844.367775	-844.367775	-844.367775	3888.13779
540.	240.	-844.369307	-844.369307	-844.369307	-844.369307	3888.13779
560.	220.	-844.370839	-844.370839	-844.370839	-844.370839	3888.13779
580.	200.	-844.372371	-844.372371	-844.372371	-844.372371	3888.13779
600.	180.	-844.373903	-844.373903	-844.373903	-844.373903	3888.13779
620.	160.	-844.375435	-844.375435	-844.375435	-844.375435	3888.13779
640.	140.	-844.376967	-844.376967	-844.376967	-844.376967	3888.13779
660.	120.	-844.378500	-844.378500	-844.378500	-844.378500	3888.13779
680.	100.	-844.380032	-844.380032	-844.380032	-844.380032	3888.13779
700.	80.	-844.381564	-844.381564	-844.381564	-844.381564	3888.13779
720.	60.	-844.383096	-844.383096	-844.383096	-844.383096	3888.13779
740.	40.	-844.384628	-844.384628	-844.384628	-844.384628	3888.13779
760.	20.	-844.386160	-844.386160	-844.386160	-844.386160	3888.13779
780.	0.	-844.387692	-844.387692	-844.387692	-844.387692	3888.13779
220.	220.	-844.395049	-844.395049	-844.395049	-844.395049	3888.13779
240.	200.	-844.396581	-844.396581	-844.396581	-844.396581	3888.13779
260.	180.	-844.398113	-844.398113	-844.398113	-844.398113	3888.13779
280.	160.	-844.400645	-844.400645	-844.400645	-844.400645	3888.13779
300.	140.	-844.403177	-844.403177	-844.403177	-844.403177	3888.13779
320.	120.	-844.405709	-844.405709	-844.405709	-844.405709	3888.13779
340.	100.	-844.408241	-844.408241	-844.408241	-844.408241	3888.13779
360.	80.	-844.410773	-844.410773	-844.410773	-844.410773	3888.13779
380.	60.	-844.413305	-844.413305	-844.413305	-844.413305	3888.13779
400.	40.	-844.415837	-844.415837	-844.415837	-844.415837	3888.13779
420.	20.	-844.418369	-844.418369	-844.418369	-844.418369	3888.13779
440.	0.	-844.420901	-844.420901	-844.420901	-844.420901	3888.13779
220.	220.	-844.429333	-844.429333	-844.429333	-844.429333	3888.13779
240.	200.	-844.431865	-844.431865	-844.431865	-844.431865	3888.13779
260.	180.	-844.434397	-844.434397	-844.434397	-844.434397	3888.13779
280.	160.	-844.436929	-844.436929	-844.436929	-844.436929	3888.13779
300.	140.	-844.439461	-844.439461	-844.439461	-844.439461	3888.13779
320.	120.	-844.441993	-844.441993	-844.441993	-844.441993	3888.13779
340.	100.	-844.444525	-844.444525	-844.444525	-844.444525	3888.13779
360.	80.	-844.447057	-844.447057	-844.447057	-844.447057	3888.13779
380.	60.	-844.449589	-844.449589	-844.449589	-844.449589	3888.13779
400.	40.	-844.452121	-844.452121	-844.452121	-844.452121	3888.13779
420.	20.	-844.454653	-844.454653	-844.454653	-844.454653	3888.13779
440.	0.	-844.457185	-844.457185	-844.457185	-844.457185	3888.13779
220.	220.	-844.465617	-844.465617	-844.465617	-844.465617	3888.13779
240.	200.	-844.468149	-844.468149	-844.468149	-844.468149	3888.13779
260.	180.	-844.470681	-844.470681	-844.470681	-844.470681	3888.13779
280.	160.	-844.473213	-844.473213	-844.473213	-844.473213	3888.13779
300.	140.	-844.475745	-844.475745	-844.475745	-844.475745	3888.13779
320.	120.	-844.478277	-844.478277	-844.478277	-844.478277	3888.13779
340.	100.	-844.480809	-844.480809	-844.480809	-844.480809	3888.13779
360.	80.	-844.483341	-844.483341	-844.483341	-844.483341	3888.13779
380.	60.	-844.485873	-844.485873	-844.485873	-844.485873	3888.13779
400.	40.	-844.488405	-844.488405	-844.488405	-844.488405	3888.13779
420.	20.	-844.490937	-844.490937	-844.490937	-844.490937	3888.13779
440.	0.	-844.493469	-844.493469	-844.493469	-844.493469	3888.13779
220.	220.	-844.499901	-844.499901	-844.499901	-844.499901	3888.13779
240.	200.	-844.502433	-844.502433	-844.502433	-844.502433	3888.13779
260.	180.	-844.504965	-844.504965	-844.504965	-844.504965	3888.13779
280.	160.	-844.507497	-844.507497	-844.507497	-844.507497	3888.13779
300.	140.	-844.510029	-844.510029	-844.510029	-844.510029	3888.13779
320.	120.	-844.512561	-844.512561	-844.512561	-844.512561	3888.13779
340.	100.	-844.515093	-844.515093	-844.515093	-844.515093	3888.13779
360.	80.	-844.517625	-844.517625	-844.517625	-844.517625	3888.13779
380.	60.	-844.520157	-844.520157	-844.520157	-844.520157	3888.13779
400.	40.	-844.522689	-844.522689	-844.522689	-844.522689	3888.13779
420.	20.	-844.525221	-844.525221	-844.525221	-844.525221	3888.13779
440.	0.	-844.527753	-844.527753	-844.527753	-844.527753	3888.13779
220.	220.	-844.535185	-844.535185	-844.535185	-844.535185	3888.13779
240.	200.	-844.537717	-844.537717	-844.537717	-844.537717	3888.13779
260.	180.	-844.540249	-844.540249	-844.540249	-844.540249	3888.13779
280.	160.	-844.542781	-844.542781	-844.542781	-844.542781	3888.13779
300.	140.	-844.545313	-844.545313	-844.545313	-844.545313	3888.13779
320.	120.	-844.547845	-844.547845	-844.547845	-844.547845	3888.13779
340.	100.	-844.550377	-844.550377	-844.550377	-844.550377	3888.13779
360.	80.	-844.552909	-844.552909	-844.552909	-844.552909	3888.13779
380.	60.	-844.555441	-844.555441	-844.555441	-844.555441	3888.13779
400.	40.	-844.557973	-844.557973	-844.557973	-844.557973	3888.13779
420.	20.	-844.560505	-844.560505	-844.560505	-844.560505	3888.13779
440.	0.	-844.562527	-844.562527	-844.562527	-844.562527	3888.13779
220.	220.	-844.565059	-844.565059	-844.565059	-844.565059	3888.13779
240.	200.	-844.567591	-844.567591	-844.567591	-844.567591	3888.13779
260.	180.	-844.570123	-844.570123	-844.570123	-844.570123	3888.13779
280.	160.	-844.572655	-844.572655	-844.572655	-844.572655	3888.13779
300.	140.	-844.575187	-844.575187	-844.575187	-844.575187	3888.13779
320.	120.	-844.577719	-844.577719	-844.577719	-844.577719	3888.13779
340.	100.	-844.580251	-844.580251	-844.580251	-844.580251	3888.13779
360.	80.	-844.582783	-844.582783	-844.582783	-844.582783	3888.13779
380.	60.	-844.585315	-844.585315	-844.585315	-844.585315	3888.13779
400.	40.	-844.587847	-844.587847	-844.587847	-844.587847	3888.13779
420.	20.	-844.590379	-844.590379	-844.590379	-844.590379	3888.13779
440.	0.	-844.592911	-844.592911	-844.592911	-844.592911	3888.13779
220.	220.	-844.595443	-844.595443	-844.595443	-844.595443	3888.13779
240.	200.	-844.597975	-844.597975	-844.597975	-844.597975	3888.13779
260.	180.	-844.600507	-844.600507	-844.600507	-844.600507	3888.13779
280.	160.	-844.603039	-844.603039	-844.603039	-844.603039	3888.13779
300.	140.	-844.605571	-844.605571	-844.605571	-844.605571	3888.13779
320.	120.	-844.608103	-844.608103	-844.608103	-844.608103	3888.13779
340.	100.	-844.610635	-844.610635	-844.610635	-844.610635	3888.13779
360.	80.	-844.613167	-844.613167	-844.613167	-844.613167	3888.13779
380.	60.	-844.615699	-844.615699	-844.615699	-844.615699	3888.13779
400.	40.	-844.618231	-844.618231	-844.618231	-844.618231	3888.13779
420.	20.	-844.620763	-844.620763	-844.620763	-844.620763	3888.13779
440.	0.	-844.623305	-844.623305	-844.623305	-844.623305	3888.13779
220.	220.	-844.625837	-844.625837	-844.625837	-844.625837	3888.13779
240.	200.	-844.628369	-844.628369	-844.628369	-844.628369	3888.13779
260.	180.	-844.630901	-844.63090			

Table 3-6b (continued)

PRESSURE PSIA	VOLUME FT <sup>3</sup> /LBMM	ENTHALAPY BTU/LBMM	ENTROPY BTU/LBMM/DEG F	TEMPERATURE= 30 DEG F	CP BTU/LEM/DEG F	CV BTU/LBM/DEG F	SONIC VELOCITY FT/SEC
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PRESSURE PSIA	VOLUME FT <sup>3</sup> /LBM	TEMPERATURE = 40 DEG F		SONIC VELOCITY FT/SEC	
		ENTHALAPY BTU/LBM	ENTROPY BTU/LSM/DEG F	CP BTU/LSM/DEG F	CV BTU/LBM/DEG F
560.	0.3053298	-832.926257	9063191	42058276	0391707
540.	0.3054174	-832.970667	9064558	42028562	0384790
520.	0.3055619	-833.015667	9065931	41988769	0387767
500.	0.3056766	-833.060667	9067305	41988899	0390752
480.	0.3058913	-833.105667	9068694	41933945	039362432
460.	0.3060713	-833.150667	9070135	41878879	03961786
440.	0.3062104	-833.195667	9071482	41804602	03984662
420.	0.3063604	-833.240667	9072886	41813622	03992618
400.	0.3065513	-833.285667	9074296	41813622	03994184
380.	0.3066613	-833.330667	9075513	41781362	039941159
360.	0.3068163	-833.375667	9075513	41751871	039941159
340.	0.3069713	-833.420667	9075513	41726976	039941242
320.	0.3071252	-833.465667	9075513	4172777	039941242
300.	0.3072812	-833.500667	9075513	41696536	039941242
280.	0.3074482	-833.535667	9075513	41665348	039941242
260.	0.3076142	-833.570667	9075513	41634653	039941242

Table 3-6b (continued)

PRESSURE PSIA	VOLUME FT <sup>3</sup> /LB M	ENTHALAPY BTU/LBM	ENTROPY BTU/LBM/DEG F	TEMPERATURE = 50 DEG F	CP	CV	BTU/LBM/DEG F	SONIC VELOCITY FT/SEC
					BTU/LBM/DEG F	BTU/LBM/DEG F	BTU/LBM/DEG F	BTU/LBM/DEG F
260.	03077963	-833.56538	-833.610652	4160.3968	4261.9718	4088.91786	4257.0.5779	2567.0.5152
	030779158	-833.651068	-833.69184	4154.7294	4261.9718	4088.85015	4256.532	2565.532
240.	030802397	-833.707724	-833.730967	4154.7294	4261.9718	4088.78246	4256.532	2565.49687
	0308024034	-833.730967	-833.760864	4154.7294	4261.9718	4088.71481	4256.49687	2565.49687
190.	030802342	-833.760864	-833.790724	4154.7294	4261.9718	4088.65798	4256.49687	2565.49687
	030802342	-833.790724	-833.820586	4154.7294	4261.9718	4088.60202	4256.49687	2565.49687
140.	030802342	-833.820586	-833.850444	4154.7294	4261.9718	4088.54707	4256.49687	2565.49687
	030802342	-833.850444	-833.880302	4154.7294	4261.9718	4088.49112	4256.49687	2565.49687
100.	030802342	-833.880302	-833.910164	4154.7294	4261.9718	4088.44522	4256.49687	2565.49687
	030802342	-833.910164	-833.940024	4154.7294	4261.9718	4088.39937	4256.49687	2565.49687
80.	030802342	-833.940024	-833.970706	4154.7294	4261.9718	4088.35352	4256.49687	2565.49687
	030802342	-833.970706	-833.999999	4154.7294	4261.9718	4088.30767	4256.49687	2565.49687
60.	03094416	-8227.102156	-8227.142907	4154.7294	4261.9718	4088.26181	4256.49687	2565.49687
	03094416	-8227.142907	-8227.183524	4154.7294	4261.9718	4088.21599	4256.49687	2565.49687
50.	03094416	-8227.183524	-8227.224252	4154.7294	4261.9718	4088.17039	4256.49687	2565.49687
	03094416	-8227.224252	-8227.264955	4154.7294	4261.9718	4088.13479	4256.49687	2565.49687
40.	03094416	-8227.264955	-8227.305658	4154.7294	4261.9718	4088.09919	4256.49687	2565.49687
	03094416	-8227.305658	-8227.346361	4154.7294	4261.9718	4088.06359	4256.49687	2565.49687
30.	03094416	-8227.346361	-8227.387064	4154.7294	4261.9718	4088.02799	4256.49687	2565.49687
	03094416	-8227.387064	-8227.427767	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
20.	03094416	-8227.427767	-8227.468470	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
	03094416	-8227.468470	-8227.509173	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
10.	03094416	-8227.509173	-8227.549876	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
	03094416	-8227.549876	-8227.580579	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
0.	03094416	-8227.580579	-8227.621282	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
	03094416	-8227.621282	-8227.661985	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
-10.	03094416	-8227.661985	-8227.702688	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
	03094416	-8227.702688	-8227.743391	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
-20.	03094416	-8227.743391	-8227.784084	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
	03094416	-8227.784084	-8227.824787	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
-30.	03094416	-8227.824787	-8227.865490	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
	03094416	-8227.865490	-8227.906193	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
-40.	03094416	-8227.906193	-8227.946896	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
	03094416	-8227.946896	-8227.987599	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
-50.	03094416	-8227.987599	-8228.028302	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
	03094416	-8228.028302	-8228.069005	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
-60.	03094416	-8228.069005	-8228.109708	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
	03094416	-8228.109708	-8228.149411	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
-70.	03094416	-8228.149411	-8228.189114	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
	03094416	-8228.189114	-8228.229817	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
-80.	03094416	-8228.229817	-8228.269520	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
	03094416	-8228.269520	-8228.309223	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
-90.	03094416	-8228.309223	-8228.348926	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
	03094416	-8228.348926	-8228.388629	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
-100.	03094416	-8228.388629	-8228.428332	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
	03094416	-8228.428332	-8228.468035	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
-120.	03094416	-8228.468035	-8228.507738	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
	03094416	-8228.507738	-8228.547441	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
-140.	03094416	-8228.547441	-8228.587144	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
	03094416	-8228.587144	-8228.626847	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
-160.	03094416	-8228.626847	-8228.666550	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
	03094416	-8228.666550	-8228.706253	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
-180.	03094416	-8228.706253	-8228.745956	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
	03094416	-8228.745956	-8228.785659	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
-200.	03094416	-8228.785659	-8228.825362	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
	03094416	-8228.825362	-8228.865065	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
-220.	03094416	-8228.865065	-8228.904768	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
	03094416	-8228.904768	-8228.944471	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
-240.	03094416	-8228.944471	-8228.984174	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
	03094416	-8228.984174	-8229.023877	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
-260.	03094416	-8229.023877	-8229.063580	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
	03094416	-8229.063580	-8229.103283	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
-280.	03094416	-8229.103283	-8229.142986	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
	03094416	-8229.142986	-8229.182689	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
-300.	03094416	-8229.182689	-8229.222392	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
	03094416	-8229.222392	-8229.262095	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
-320.	03094416	-8229.262095	-8229.301798	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
	03094416	-8229.301798	-8229.341501	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
-340.	03094416	-8229.341501	-8229.381204	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
	03094416	-8229.381204	-8229.420907	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
-360.	03094416	-8229.420907	-8229.460610	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
	03094416	-8229.460610	-8229.500313	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
-380.	03094416	-8229.500313	-8229.539996	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
	03094416	-8229.539996	-8229.579699	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
-400.	03094416	-8229.579699	-8229.619392	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
	03094416	-8229.619392	-8229.659095	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
-420.	03094416	-8229.659095	-8229.698798	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
	03094416	-8229.698798	-8229.738491	4154.7294	4261.9718	4088.00239	4256.49687	2565.49687
-440.	03094416	-8229.738491	-8229.778194	4154.7294	4261.9718	4088.0		

Table 3-6b (continued)

160. • 03173603 -821.837168  
140. • 03174748 -821.864790  
120. • 03174913 -821.8919C

• 41270190 2340.0682  
• 41269253 2332.6582  
• 41258335 2325.2112

TEMPERATURE = 70 DEG F

PRESSURE PSIA	VOLUME FT <sup>3</sup> /LBM	ENTHALPY BTU/LBM	ENTROPY BTU/LEM/DEG F	CP BTU/LEM/DEC F	CV BTU/LBM/DEC F	SONIC VELOCITY FT/SEC
560.	03176134	-815.214765	• 9408204	• 4189370.5	• 4186817.9	2385.4536
540.	03176200	-815.244485	• 9411487	• 418676.6	• 418671.7	2379.4053
520.	03176480	-815.273616	• 9414871	• 4186266.8	• 418671.7	2371.3748
500.	03176421	-815.332304	• 9416513	• 4186576.6	• 418671.7	2360.0610
480.	03176454	-815.392235	• 941921624	• 4185537.5	• 4185537.5	2349.8607
460.	03176440	-815.441546	• 94219926	• 4185637.5	• 4185637.5	2339.4254
440.	03176420	-815.491546	• 94236056	• 4184584.7	• 4184584.7	2329.2715
420.	03176400	-815.541546	• 94265056	• 4184584.7	• 4184584.7	2319.1435
400.	03176380	-815.591546	• 94322969	• 41823256.9	• 41823256.9	2309.0944
380.	03176360	-815.641546	• 94329433	• 41812713.5	• 41812713.5	2299.0444
360.	03176340	-815.691546	• 9433945	• 41802713.5	• 41802713.5	2289.0557
340.	03176320	-815.741546	• 94349060	• 41802713.5	• 41802713.5	2279.0557
320.	03176300	-815.791546	• 94359060	• 41802713.5	• 41802713.5	2269.0557
300.	03176280	-815.841546	• 94369060	• 41802713.5	• 41802713.5	2259.0557
280.	03176260	-815.891546	• 94379060	• 41802713.5	• 41802713.5	2249.0557
260.	03176240	-815.941546	• 94389060	• 41802713.5	• 41802713.5	2239.0557
240.	03176220	-815.991546	• 94399060	• 41802713.5	• 41802713.5	2229.0557
220.	03176200	-816.041546	• 94409060	• 41802713.5	• 41802713.5	2219.0557
200.	03176180	-816.091546	• 94419060	• 41802713.5	• 41802713.5	2209.0557
180.	03176160	-816.141546	• 94429060	• 41802713.5	• 41802713.5	2199.0557
160.	03176140	-816.191546	• 94439060	• 41802713.5	• 41802713.5	2189.0557
140.	03176120	-816.241546	• 94449060	• 41802713.5	• 41802713.5	2179.0557

TEMPERATURE = 80 DEG F

PRESSURE PSIA	VOLUME FT <sup>3</sup> /LBM	ENTHALPY BTU/LBM	ENTROPY BTU/LEM/DEG F	CP BTU/LBM/DEC F	CV BTU/LBM/DEC F	SONIC VELOCITY FT/SEC
560.	03176111	-809.570722	• 9522574	• 41866111	• 41899356	2289.2952
540.	03176122	-809.579136	• 95235808	• 41866111	• 41899356	2274.5529
520.	03176132	-809.588075	• 95245702	• 41866111	• 41899356	2260.0587
500.	03176142	-809.596215	• 95255104	• 41866111	• 41899356	2245.4613
480.	03176152	-809.604255	• 95265104	• 41866111	• 41899356	2231.3703
460.	03176162	-809.612295	• 95275104	• 41866111	• 41899356	2217.2803
440.	03176172	-809.620335	• 95285104	• 41866111	• 41899356	2203.1903
420.	03176182	-809.628375	• 95295104	• 41866111	• 41899356	2189.0903
400.	03176192	-809.636415	• 95305104	• 41866111	• 41899356	2175.0003
380.	03176202	-809.644455	• 95315104	• 41866111	• 41899356	2161.9103
360.	03176212	-809.652495	• 95325104	• 41866111	• 41899356	2148.8203
340.	03176222	-809.660535	• 95335104	• 41866111	• 41899356	2135.7303
320.	03176232	-809.668575	• 95345104	• 41866111	• 41899356	2122.6403
300.	03176242	-809.676615	• 95355104	• 41866111	• 41899356	2109.5503
280.	03176252	-809.684655	• 95365104	• 41866111	• 41899356	2096.4603
260.	03176262	-809.692695	• 95375104	• 41866111	• 41899356	2083.3703
240.	03176272	-809.700735	• 95385104	• 41866111	• 41899356	2070.2803
220.	03176282	-809.708775	• 95395104	• 41866111	• 41899356	2057.1903
200.	03176292	-809.716815	• 95405104	• 41866111	• 41899356	2044.1003
180.	03176302	-809.724855	• 95415104	• 41866111	• 41899356	2031.0103
160.	03176312	-809.732895	• 95425104	• 41866111	• 41899356	2017.9203
140.	03176322	-809.740935	• 95435104	• 41866111	• 41899356	2004.8303

TEMPERATURE = 90 DEG F

PRESSURE PSIA	VOLUME FT <sup>3</sup> /LBM	ENTHALPY BTU/LBM	ENTROPY BTU/LEM/DEG F	CP BTU/LBM/DEC F	CV BTU/LBM/DEC F	SONIC VELOCITY FT/SEC
560.	03176033	-809.748975	• 95445104	• 41866047	• 41899408	2289.2942
540.	03176043	-809.756915	• 95455104	• 41866047	• 41899408	2274.5529
520.	03176053	-809.764955	• 95465104	• 41866047	• 41899408	2260.0587
500.	03176063	-809.772995	• 95475104	• 41866047	• 41899408	2245.4613
480.	03176073	-809.780935	• 95485104	• 41866047	• 41899408	2231.3703
460.	03176083	-809.788975	• 95495104	• 41866047	• 41899408	2217.2803
440.	03176093	-809.796915	• 95505104	• 41866047	• 41899408	2203.1903
420.	03176103	-809.804955	• 95515104	• 41866047	• 41899408	2189.0903
400.	03176113	-809.812995	• 95525104	• 41866047	• 41899408	2175.0003
380.	03176123	-809.820935	• 95535104	• 41866047	• 41899408	2161.9103
360.	03176133	-809.828975	• 95545104	• 41866047	• 41899408	2148.8203
340.	03176143	-809.836915	• 95555104	• 41866047	• 41899408	2135.7303
320.	03176153	-809.844955	• 95565104	• 41866047	• 41899408	2122.6403
300.	03176163	-809.852995	• 95575104	• 41866047	• 41899408	2109.5503
280.	03176173	-809.860935	• 95585104	• 41866047	• 41899408	2096.4603
260.	03176183	-809.868975	• 95595104	• 41866047	• 41899408	2083.3703
240.	03176193	-809.876915	• 95605104	• 41866047	• 41899408	2070.2803
220.	03176203	-809.884955	• 95615104	• 41866047	• 41899408	2057.1903
200.	03176213	-809.892995	• 95625104	• 41866047	• 41899408	2044.1003
180.	03176223	-809.900935	• 95635104	• 41866047	• 41899408	2031.0103
160.	03176233	-809.908975	• 95645104	• 41866047	• 41899408	2017.9203

Table 3-6b (continued)

220.

.03454575 -789.622316 .9910546 .48436556

.03454575 -789.622316 .9910546 .48436556

.03454575 -789.622316 .9910546 .48436556

PRESSURE PSIA	VOLUME FT <sup>3</sup> /LBM	ENTHALAPY BTU/LBM	ENTROPY BTU/LBM/DEG F	CP BTU/LBM/DEG F	CV BTU/LBM/DEG F	SONIC VELOCITY FT/SEC
560.	.034548349	-783.245791	.998387C	45745556	4496407	1902.5030
540.	.03452825	-783.222860	.9986467	4569702	4496315	1893.5499
520.	.03462010	-783.193212	.9983908	45663064	4496362	1884.4177
500.	.03466725	-783.171487	.9981761	4566554	4496897	1866.2395
480.	.03467152	-783.143521	.9984460	4567459	4497389	1856.4845
460.	.03471526	-783.108196	.99999966	45679490	4498966	1847.6499
440.	.03476476	-783.046581	1.0000276	45561407	4499927	1838.7355
420.	.03486476	-783.010562	1.00005626	4552321	4495138	1828.7330
400.	.03491656	-783.010516	1.00008516	45496469	4495249	1819.7459
380.	.03496939	-783.01452	1.0014432	4543256	44954169	1809.4695
360.	.03502333	-783.014745	1.0017458	45404669	44958049	1799.8375
340.	.03507840	-783.002053	1.0020533	453804669	449510397	1779.8758
320.	.03513468	-782.979381	1.0023658	453804669	449512970	1769.84426
300.	.03519220	-782.942701	1.00266837	45322530	4495322530	1759.6443

## TEMPERATURE = 130 DEG F

PRESSURE PSIA	VOLUME FT <sup>3</sup> /LBM	ENTHALAPY BTU/LBM	ENTROPY BTU/LBM/DEG F	CP BTU/LBM/DEG F	CV BTU/LBM/DEG F	SONIC VELOCITY FT/SEC
560.	.03522705	-776.329508	1.0102111	46161397	45857	1805.2696
540.	.03528163	-776.285277	1.0105073	4610780	45029	1795.7705
520.	.0353805	-776.238587	1.011133	46080832	45049	1786.1843
500.	.03539530	-776.189337	1.0114236	46057652	450106	1776.5377
480.	.0354380	-776.137414	1.011736	46026569	450312	1756.8754
460.	.03546371	-776.082704	1.0120567	45999434	4506182	1746.8468
440.	.03551361	-776.025074	1.0123569	45947216	45097371	1736.8756
420.	.03556714	-775.964393	1.0123180	45944707	4507422	1726.9745
400.	.03563737	-775.905217	1.0130561	45917208	45081802	1715.9946
380.	.03567034	-775.833251	1.0134007	4588900	45086530	1695.4865
360.	.03576715	-775.762514	1.0137520	45861941	4516530	1684.4860
340.	.03583450	-775.688604	1.0141103	45834177	45103036	1674.0863
320.	.035897458	-775.609650	1.0144761	45806329	45112122	1663.1883
300.	.03604752	-775.527139	1.0148498	45778396	45117783	1653.1883
280.	.03612255	-775.440256				

## TEMPERATURE = 140 DEG F

PRESSURE PSIA	VOLUME FT <sup>3</sup> /LBM	ENTHALAPY BTU/LBM	ENTROPY BTU/LBM/DEG F	CP BTU/LBM/DEG F	CV BTU/LBM/DEG F	SONIC VELOCITY FT/SEC
560.	.03608276	-769.150676	1.022277C	46565654	465650871	1707.7567
540.	.03615214	-769.07132	1.0226223	46535071	46509259	1697.6332
520.	.03622330	-768.999284	1.0229743	46533131	46483399	1687.4014
500.	.03629635	-768.9183908	1.02336933	4651561	46452416	1676.6010
480.	.03644854	-768.833689	1.0240528	4650451	4645306	1664.5010
460.	.03649793	-768.7444151	1.0245452	4649714	464234771	1652.3518
440.	.036644854	-768.6501046	1.0248454	46462454	464123478	1642.3518
420.	.03679714	-768.5650656	1.0252454	46457652	46401589	1631.6378
400.	.036864403	-768.479105	1.02567452	46431562	4637552	1621.3518
380.	.036964042	-768.3906402	1.0260752	4641562	46325142	1611.026694
360.	.037064042	-768.3026579	1.0264752	46401562	46315792	1601.026694
340.	.037164042	-768.2147912	1.02687452	46387452	46275579	1591.9788
320.	.037264042	-768.1269172	1.027276	46372452	46252752	1581.90350

Table 3-6b (continued)

PRESSURE PSIA	VOLUME FT <sup>3</sup> /LBM	TEMPERATURE = 150 DEG F			TEMPERATURE = 160 DEG F			TEMPERATURE = 170 DEG F			TEMPERATURE = 180 DEG F		
		ENTHALAPY BTU/LBM	ENTROPY BTU/LBM/DEG F	CP BTU/LBM/DEG F									
560.	0.3709333	-761.636739	1.0346968	47028389	-761.520862	1.0351121	47029488	-761.417616	1.0356178	46224258	-761.317243	1.0356178	46224258
540.	0.3718450	-761.393391	1.0356178	46986331	-761.270570	1.0356178	46986331	-761.159312	1.0356178	46224258	-761.047596	1.0356178	46224258
520.	0.3727800	-761.270570	1.0356178	46956862	-761.147596	1.0356178	46956862	-761.036473	1.0356178	46224258	-760.924217	1.0356178	46224258
500.	0.3737162	-761.147596	1.0356178	46933124	-760.993107	1.0356178	46933124	-760.884207	1.0356178	46224258	-760.763645	1.0356178	46224258
480.	0.3741842	-760.993107	1.0356178	46909507	-760.842217	1.0356178	46909507	-760.707849	1.0356178	46224258	-760.574777	1.0356178	46224258
460.	0.3758185	-760.842217	1.0356178	468862658	-760.683716	1.0356178	468862658	-760.637849	1.0356178	46224258	-760.515477	1.0356178	46224258
440.	0.3765905	-760.683716	1.0356178	468616581	-760.547767	1.0356178	468616581	-760.498137	1.0356178	46224258	-760.416516	1.0356178	46224258
420.	0.3778390	-760.547767	1.0356178	468315481	-760.405348	1.0356178	468315481	-760.354817	1.0356178	46224258	-760.27103	1.0356178	46224258
400.	0.3792197	-760.405348	1.0356178	468016516	-760.261666	1.0356178	468016516	-760.213796	1.0356178	46224258	-760.146059	1.0356178	46224258
380.	0.3804523	-760.261666	1.0356178	46771380	-760.19398621	1.0356178	46771380	-760.146059	1.0356178	46224258	-759.946059	1.0356178	46224258
360.	0.3817450	-760.19398621	1.0356178	46747774	-759.946059	1.0356178	46747774	-759.77259	1.0356178	46224258	-759.520862	1.0356178	46224258
340.	0.3831010	-759.946059	1.0356178	46713124	-759.707849	1.0356178	46713124	-759.56248	1.0356178	46224258	-759.371060	1.0356178	46224258
320.	0.3845657	-759.707849	1.0356178	466893146	-759.4692760	1.0356178	466893146	-759.32488	1.0356178	46224258	-759.1663201	1.0356178	46224258
300.	0.3859138	-759.4692760	1.0356178	46665899	-759.222149	1.0356178	46665899	-759.08726	1.0356178	46224258	-758.98955	1.0356178	46224258
280.	0.3873057	-759.222149	1.0356178	46642760	-758.98955	1.0356178	46642760	-758.84726	1.0356178	46224258	-758.73521	1.0356178	46224258
260.	0.3887681	-758.98955	1.0356178	466205658	-758.640132	1.0356178	466205658	-758.5010993	1.0356178	46224258	-758.363169	1.0356178	46224258
240.	0.3903090	-758.640132	1.0356178	466082627	-758.261684	1.0356178	466082627	-758.1261684	1.0356178	46224258	-758.080087	1.0356178	46224258
220.	0.3919376	-758.261684	1.0356178	465864593	-757.8940087	1.0356178	465864593	-757.530983	1.0356178	46224258	-757.330766	1.0356178	46224258
200.	0.3936665	-757.8940087	1.0356178	465645931	-757.530983	1.0356178	465645931	-757.174593	1.0356178	46224258	-756.839583	1.0356178	46224258
180.	0.3955055	-757.530983	1.0356178	465424593	-757.174593	1.0356178	465424593	-756.714593	1.0356178	46224258	-756.359583	1.0356178	46224258
160.	0.3974751	-757.174593	1.0356178	465214593	-756.714593	1.0356178	465214593	-756.293254	1.0356178	46224258	-755.839583	1.0356178	46224258
140.	0.4000000	-756.714593	1.0356178	465004593	-756.293254	1.0356178	465004593	-755.773254	1.0356178	46224258	-755.359583	1.0356178	46224258
120.	0.4025000	-756.293254	1.0356178	464804593	-755.773254	1.0356178	464804593	-755.253254	1.0356178	46224258	-754.839583	1.0356178	46224258
100.	0.4050000	-755.773254	1.0356178	464604593	-755.253254	1.0356178	464604593	-754.733254	1.0356178	46224258	-754.359583	1.0356178	46224258
80.	0.4075000	-755.253254	1.0356178	464404593	-754.733254	1.0356178	464404593	-754.213254	1.0356178	46224258	-753.839583	1.0356178	46224258
60.	0.4100000	-754.733254	1.0356178	464204593	-754.213254	1.0356178	464204593	-753.693254	1.0356178	46224258	-753.359583	1.0356178	46224258
40.	0.4125000	-754.213254	1.0356178	464004593	-753.693254	1.0356178	464004593	-753.173254	1.0356178	46224258	-752.839583	1.0356178	46224258
20.	0.4150000	-753.693254	1.0356178	463804593	-753.173254	1.0356178	463804593	-752.673254	1.0356178	46224258	-752.359583	1.0356178	46224258
0.	0.4175000	-753.173254	1.0356178	463604593	-752.673254	1.0356178	463604593	-752.173254	1.0356178	46224258	-751.839583	1.0356178	46224258

## TEMPERATURE = 110 DEG F

PRESSURE PSIA	VOLUME FT <sup>3</sup> /LBM	ENTHALPY BTU/LBM	ENTROPY BTU/LBM <sup>0</sup> /DEG F	CP BTU/LBM/DEG F	CV BTU/LBM/DEG F	SONIC VELOCITY FT/SEC
560.	*04639675	-722.822616	1.0961326	*49464274	*49387322	1208.5299
540.	*24747335	-721.278544	1.0987752	*49556986	*49535266	1187.9847
520.	*04904743	-719.094464	1.1024099	*497C7768	*49742678	1162.7700

## TEMPERATURE = 200 DEG F

PRESSURE PSIA	VOLUME FT <sup>3</sup> /LBM	ENTHALPY BTU/LBM	ENTROPY BTU/LBM <sup>0</sup> /DEG F	CP BTU/LBM/DEG F	CV BTU/LBM/DEG F	SONIC VELOCITY FT/SEC
560.	*14480587	-653.384450	1.2020357	*53462232	*49752069	548.1292
540.	*15987708	-648.130360	1.2108435	*53665348	*49251524	544.1123

Table 3-7

## Saturation Temperature Table for Propane as Given by Stearns &amp; George.

## THERMODYNAMIC PROPERTIES OF PROPANE AS GIVEN BY STEARNS &amp; GEORGE

P	T	VF	VG	FT3/LBM	BTU/LBM	HG	SF	SG	BTU/LBM/DEG F
PSIA	DEG F								
14.70	-43.71	.02752	6.6660	1.8136	364.76	.9266	1.3682		
15.28	-42.00	.02757	6.4200	1.8190	365.20	.9289	1.3676		
16.79	-38.00	.02763	6.1600	1.8300	366.30	.9315	1.3670		
17.56	-36.00	.02769	5.9200	1.8410	366.90	.9340	1.3664		
18.49	-34.00	.02775	5.6600	1.8510	367.50	.9365	1.3652		
19.30	-32.00	.02781	5.4200	1.8620	368.00	.9391	1.3646		
20.18	-30.00	.02784	5.1800	1.8730	368.60	.9416	1.3640		
21.05	-28.00	.02800	4.9200	1.8840	369.20	.9441	1.3634		
22.01	-26.00	.02807	4.6300	1.8950	369.80	.9467	1.3628		
23.08	-24.00	.02813	4.4400	1.9160	370.40	.9492	1.3622		
24.00	-22.00	.02820	4.2500	1.9270	370.90	.9517	1.3616		
25.13	-20.00	.02826	4.0600	1.9380	371.50	.9543	1.3610		
26.15	-18.00	.02833	3.9000	1.9490	372.10	.9568	1.3604		
27.30	-16.00	.02839	3.7600	1.9600	372.70	.9617	1.3599		
28.50	-14.00	.02846	3.6190	1.9710	373.30	.9641	1.3593		
29.70	-12.00	.02852	3.4770	1.9820	373.80	.9666	1.3588		
31.05	-10.00	.02859	3.3300	1.9940	374.40	.9690	1.3582		
32.23	-8.00	.02866	3.2000	2.0050	375.00	.9714	1.3577		
33.55	-6.00	.02873	3.0800	2.0160	375.50	.9739	1.3571		
34.80	-4.00	.02879	2.9600	2.0270	376.00	.9763	1.3566		
36.00	-2.00	.02886	2.8460	2.0380	376.50	.9788	1.3560		
37.81	0.00	.02893	2.7400	2.0500	377.00	.9812	1.3555		
39.30	2.00	.02900	2.6600	2.0610	377.50	.9836	1.3550		
40.65	4.00	.02908	2.5600	2.0720	378.00	.9860	1.3545		
42.50	6.00	.02915	2.4700	2.0840	378.50	.9884	1.3541		
44.13	8.00	.02923	2.3800	2.0960	379.00	.9908	1.3536		
45.85	10.00	.02930	2.3000	2.1070	380.00	.9932	1.3531		
47.55	12.00	.02938	2.2200	2.1190	380.60	.9956	1.3527		
49.25	14.00	.02946	2.1400	2.1310	381.10	.9979	1.3523		
51.20	16.00	.02954	2.0600	2.1420	381.60	1.0003	1.3518		
53.10	18.00	.02962	1.9900	2.1540	382.10	1.0026	1.3514		
55.00	20.00	.02970	1.9300	2.1660	382.60	1.0050	1.3510		
57.05	22.00	.02978	1.8600	2.1770	383.10	1.0073	1.3506		
59.10	24.00	.02986	1.7900	2.1880	383.60	1.0097	1.3502		
61.25	26.00	.02995	1.7200	2.2000	384.10	1.0120	1.3499		
63.45	28.00	.03003	1.6500	2.2210	384.60	1.0144	1.3495		
65.70	30.00	.03011	1.6000	2.2420	385.10	1.0167	1.3491		
67.95	32.00	.03020	1.5400	2.2640	385.60	1.0190	1.3487		
70.20	34.00	.03029	1.4800	2.2850	386.10	1.0213	1.3484		
72.45	36.00	.03037	1.4300	2.3060	386.60	1.0237	1.3480		
75.25	38.00	.03046	1.3900	2.2260	387.10	1.0260	1.3477		
77.80	40.00	.03055	1.3300	2.2790	387.50	1.0283	1.3473		
80.40	42.00	.03064	1.2800	2.2910	388.00	1.0306	1.3470		
83.05	44.00	.03073	1.2500	2.3120	388.50	1.0329	1.3466		
85.65	46.00	.03083	1.2100	2.3260	389.00	1.0352	1.3463		
89.50	48.00	.03092	1.1700	2.3380	389.50	1.0375	1.3459		
94.50	50.00	.03101	1.1300	2.3490	390.00	1.0400	1.3456		
97.50	52.00	.03111	1.1000	2.3610	390.50	1.0421	1.3453		
101.60	54.00	.03121	1.0700	2.3730	391.00	1.0443	1.3450		
105.70	56.00	.03130	1.0400	2.3850	391.50	1.0466	1.3447		
109.70	58.00	.03140	1.0100	2.3984	392.00	1.0488	1.3441		
113.70	60.00	.03150	9.8000	2.4100	392.50	1.0511	1.3438		
117.60	62.00	.03162	9.5000	2.4220	393.00	1.0534	1.3435		
121.50	64.00	.03174	9.3200	2.4340	393.50	1.0579	1.3433		
125.40	66.00	.03185	9.0600	2.4460	394.00	1.0604	1.3427		
129.30	68.00	.03197	8.8000	2.4570	394.50	1.0647	1.3424		
133.20	70.00	.03209	8.5200	2.4690	395.00	1.0680	1.3421		
137.10	72.00	.03221	8.2500	2.4800	395.50	1.0717	1.3418		

131•70	74•00	•0323•3	•810	248•10	•3421
135•60	76•00	•0324•5	788	249•40	•0669
139•60	78•00	•0325•7	766	250•20	•0692
143•60	80•00	•0326•9	745	251•90	•0714
147•70	82•00	•0328•1	725	253•10	•0737
151•40	84•00	•0329•3	704	254•40	•0780
156•60	86•00	•0330•5	684	255•60	•0827
145•60	88•00	•0331•7	663	256•20	•0850
149•60	90•00	•0332•9	643	257•50	•0873
152•60	92•00	•0334•1	626	258•80	•0895
154•60	94•00	•0335•3	609	260•10	•0918
158•60	96•00	•0336•6	592	262•30	•0940
162•60	98•00	•0337•8	575	264•60	•0963
166•60	100•00	•0339•0	558	265•90	•0986
170•60	102•00	•0340•2	544	266•90	•3386
174•60	104•00	•0341•5	530	267•20	•400•90
178•60	106•00	•0342•7	516	268•50	•401•20
182•60	108•00	•0343•9	502	269•80	•401•60
186•60	110•00	•0345•2	487	271•10	•401•90
190•60	112•00	•0346•4	475	272•50	•402•30
194•60	114•00	•0348•4	463	273•90	•402•70
198•60	116•00	•0350•0	451	275•20	•403•00
202•60	118•00	•0351•2	439	276•50	•403•40
206•60	120•00	•0353•2	426	278•00	•404•80
210•60	122•00	•0354•4	415	279•40	•404•10
214•60	124•00	•0356•4	404	280•90	•404•50
218•60	126•00	•0358•0	393	282•30	•404•80
222•60	128•00	•0359•6	382	283•80	•405•20
226•60	130•00	•0361•2	370	285•20	•405•60
230•60	132•00	•0363•0	360	286•70	•405•70
234•60	134•00	•0364•8	350	288•20	•406•10
238•60	136•00	•0366•6	340	289•70	•406•40
242•60	138•00	•0368•4	330	291•20	•406•70
246•60	140•00	•0370•2	320	292•70	•407•00
250•60	142•00	•0372•5	312	294•20	•407•30
254•60	144•00	•0374•8	303	295•70	•407•60
258•60	146•00	•0377•4	295	297•20	•407•80
262•60	148•00	•0379•1	286	298•70	•408•00
266•60	150•00	•0381•7	276	300•20	•408•20
270•60	152•00	•0384•6	267	301•70	•408•40
274•60	154•00	•0387•5	256	303•20	•408•60
278•60	156•00	•0390•4	255	305•10	•408•80
282•60	158•00	•0393•3	248	306•60	•409•00
286•60	160•00	•0396•2	240	308•40	•409•20
290•60	162•00	•0399•6	234	310•20	•409•40
294•60	164•00	•0403•0	227	312•00	•409•90
298•60	166•00	•0406•4	221	313•70	•408•90
302•60	168•00	•0413•2	208	317•50	•408•60
306•60	170•00	•0417•9	202	319•50	•408•40
310•60	172•00	•0422•6	197	321•50	•408•20
314•60	174•00	•0427•3	191	323•50	•408•00
318•60	176•00	•0432•0	186	325•50	•407•80
322•60	178•00	•0436•7	180	327•50	•407•60
326•60	180•00	•0440•4	174	329•60	•407•40
330•60	182•00	•0443•6	168	332•60	•407•10
334•60	184•00	•0447•4	161	334•90	•406•60
338•60	186•00	•0451•2	155	336•20	•405•90
342•60	188•00	•0464•3	149	338•50	•404•60
346•60	190•00	•0471•2	143	339•50	•39•30
350•60	192•00	•0521•0	138	343•50	•3040

Table 3-8  
 Saturation Temperature Table for the Pseudo-Fluid; 65% by Mole Propane,  
 25% Propylene, and 10% N-Butane

Table 3-8 (continued)

## THERMODYNAMIC PROPERTIES OF PROPANE-PROPYLENE-N-BUTANE MIXTURE, (65-25-10), AS PREDICTED BY STARLING'S EQUATION OF STATE

Table 3-8 (continued)

Table 3-8 (continued)

125.31	62	70	4005063102	479085642	398556207	378628064	405412968	6574300	6709672
129.11	64	74	4016500711	4773266672	3997985557	3823975287	401025313	6547311	6677310
133.97	66	76	4027891383	4779266550	3970391396	3823975287	401025313	655537898	665537898
136.97	68	78	4039262640	4820410555	39843562084	3842426024	401025313	655837897	665837897
141.03	70	80	40461857276	4867315778	39884405266	38864405266	401025313	656237896	666237896
145.18	72	82	41065648376	49085673524	4095648376	38864405266	401025313	65674300	66674300
149.73	74	84	41065648376	4929164464	4095648376	38864405266	401025313	65714300	66714300
153.87	76	86	41162073044	4929164464	4095648376	38864405266	401025313	65754300	66754300
158.09	78	88	41162073044	4929164464	4095648376	38864405266	401025313	65794300	66794300
162.31	80	90	41162073044	4929164464	4095648376	38864405266	401025313	65834300	66834300
167.2	82	92	41162073044	4929164464	4095648376	38864405266	401025313	65874300	66874300
171.7	84	94	41162073044	4929164464	4095648376	38864405266	401025313	65914300	66914300
176.2	86	96	41162073044	4929164464	4095648376	38864405266	401025313	65954300	66954300
180.7	88	98	41162073044	4929164464	4095648376	38864405266	401025313	66094300	66094300
185.2	90	100	41162073044	4929164464	4095648376	38864405266	401025313	66134300	66134300
189.7	92	102	41162073044	4929164464	4095648376	38864405266	401025313	66174300	66174300
194.2	94	104	41162073044	4929164464	4095648376	38864405266	401025313	66214300	66214300
198.7	96	106	41162073044	4929164464	4095648376	38864405266	401025313	66254300	66254300
203.2	98	108	41162073044	4929164464	4095648376	38864405266	401025313	66294300	66294300
207.7	100	110	41162073044	4929164464	4095648376	38864405266	401025313	66334300	66334300
212.2	102	112	41162073044	4929164464	4095648376	38864405266	401025313	66374300	66374300
216.7	104	114	41162073044	4929164464	4095648376	38864405266	401025313	66414300	66414300
221.2	106	116	41162073044	4929164464	4095648376	38864405266	401025313	66454300	66454300
225.7	108	118	41162073044	4929164464	4095648376	38864405266	401025313	66494300	66494300
230.2	110	120	41162073044	4929164464	4095648376	38864405266	401025313	66534300	66534300
234.7	112	122	41162073044	4929164464	4095648376	38864405266	401025313	66574300	66574300
239.2	114	124	41162073044	4929164464	4095648376	38864405266	401025313	66614300	66614300
243.7	116	126	41162073044	4929164464	4095648376	38864405266	401025313	66654300	66654300
248.2	118	128	41162073044	4929164464	4095648376	38864405266	401025313	66694300	66694300
252.7	120	130	41162073044	4929164464	4095648376	38864405266	401025313	66734300	66734300
257.2	122	132	41162073044	4929164464	4095648376	38864405266	401025313	66774300	66774300
261.7	124	134	41162073044	4929164464	4095648376	38864405266	401025313	66814300	66814300
266.2	126	136	41162073044	4929164464	4095648376	38864405266	401025313	66854300	66854300
270.7	128	138	41162073044	4929164464	4095648376	38864405266	401025313	66894300	66894300
275.2	130	140	41162073044	4929164464	4095648376	38864405266	401025313	66934300	66934300
279.7	132	142	41162073044	4929164464	4095648376	38864405266	401025313	66974300	66974300
284.2	134	144	41162073044	4929164464	4095648376	38864405266	401025313	67014300	67014300
288.7	136	146	41162073044	4929164464	4095648376	38864405266	401025313	67054300	67054300
293.2	138	148	41162073044	4929164464	4095648376	38864405266	401025313	67094300	67094300
297.7	140	150	41162073044	4929164464	4095648376	38864405266	401025313	67134300	67134300
302.2	142	152	41162073044	4929164464	4095648376	38864405266	401025313	67174300	67174300
306.7	144	154	41162073044	4929164464	4095648376	38864405266	401025313	67214300	67214300
311.2	146	156	41162073044	4929164464	4095648376	38864405266	401025313	67254300	67254300
315.7	148	158	41162073044	4929164464	4095648376	38864405266	401025313	67294300	67294300
320.2	150	160	41162073044	4929164464	4095648376	38864405266	401025313	67334300	67334300
324.7	152	162	41162073044	4929164464	4095648376	38864405266	401025313	67374300	67374300
329.2	154	164	41162073044	4929164464	4095648376	38864405266	401025313	67414300	67414300
333.7	156	166	41162073044	4929164464	4095648376	38864405266	401025313	67454300	67454300
338.2	158	168	41162073044	4929164464	4095648376	38864405266	401025313	67494300	67494300
342.7	160	170	41162073044	4929164464	4095648376	38864405266	401025313	67534300	67534300
347.2	162	172	41162073044	4929164464	4095648376	38864405266	401025313	67574300	67574300
351.7	164	174	41162073044	4929164464	4095648376	38864405266	401025313	67614300	67614300
356.2	166	176	41162073044	4929164464	4095648376	38864405266	401025313	67654300	67654300
360.7	168	178	41162073044	4929164464	4095648376	38864405266	401025313	67694300	67694300
365.2	170	180	41162073044	4929164464	4095648376	38864405266	401025313	67734300	67734300
369.7	172	182	41162073044	4929164464	4095648376	38864405266	401025313	67774300	67774300
374.2	174	184	41162073044	4929164464	4095648376	38864405266	401025313	67814300	67814300
378.7	176	186	41162073044	4929164464	4095648376	38864405266	401025313	67854300	67854300
383.2	178	188	41162073044	4929164464	4095648376	38864405266	401025313	67894300	67894300
387.7	180	190	41162073044	4929164464	4095648376	38864405266	401025313	67934300	67934300
392.2	182	192	41162073044	4929164464	4095648376	38864405266	401025313	67974300	67974300
396.7	184	194	41162073044	4929164464	4095648376	38864405266	401025313	68014300	68014300
401.2	186	196	41162073044	4929164464	4095648376	38864405266	401025313	68054300	68054300
405.7	188	198	41162073044	4929164464	4095648376	38864405266	401025313	68094300	68094300
410.2	190	200	41162073044	4929164464	4095648376	38864405266	401025313	68134300	68134300
414.7	192	202	41162073044	4929164464	4095648376	38864405266	401025313	68174300	68174300
419.2	194	204	41162073044	4929164464	4095648376	38864405266	401025313	68214300	68214300
423.7	196	206	41162073044	4929164464	4095648376	38864405266	401025313	68254300	68254300
428.2	198	208	41162073044	4929164464	4095648376	38864405266	401025313	68294300	68294300
432.7	200	210	41162073044	4929164464	4095648376	38864405266	401025313	68334300	68334300
437.2	202	212	41162073044	4929164464	4095648376	38864405266	401025313	68374300	68374300
441.7	204	214	41162073044	4929164464	4095648376	38864405266	401025313	68414300	68414300
446.2	206	216	41162073044	4929164464	4095648376	38864405266	401025313	68454300	68454300
450.7	208	218	41162073044	4929164464	4095648376	38864405266	401025313	68494300	68494300
455.2	210	220	41162073044	4929164464	4095648376	38864405266	401025313	68534300	68534300
459.7	212	222	41162073044	4929164464	4095648376	38864405266	401025313	68574300	68574300
464.2	214	224	41162073044	4929164464	4095648376	38864405266	401025313	68614300	68614300
468.7	216	226	41162073044	4929164464	4095648376	38864405266	401025313	68654300	68654300
473.2	218	228	41162073044	4929164464	4095648376	38864405266	401025313	68694300	68694300
477.7	220	230	41162073044	4929164464	4095648376	38864405266	401025313	68734300	68734300
482.2	222	232	41162073044	4929164464	4095648376	38864405266	401025313	68774300	68774300
486.7	224	234	41162073044	4929164464	4095648376	38864405266	401025313	68814300	68814300
491.2	226	236	41162073044	4929164464	4095648376	38864405266	401025313	68854300	68854300
495.7	228	238	41162073044	4929164464	4095648376	388			

## THERMODYNAMIC PROPERTIES OF PROPYLENE AS PREDICTED BY STARLING'S EQUATION OF STATE

Table 3-9  
 Saturation Temperature Table for Propylene  
 Calculated from Starling's Equation of State

Table 3-9 (continued)

Table 3-9 (continued)

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四庫全書

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5 0 0 0  
5 7 1 0  
5 6 7 8  
4 4 4 4  
0 0 0 0

182.

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Table 3-9 (continued)

THERMODYNAMIC PROPERTIES OF PROPYLENE AS PREDICTED BY STARLING'S EQUATION OF STATE

Table 3-9 (continued)

Table 3-9 (Continued)

642.4411

13308.9474

471235741

451935295

4926364720

4354646490

188.

513.53

\*The lack of values for entropy and enthalpy departures and for specific heat references does not permit an accurate calculation of the shown thermodynamic properties in this temperature range.

Table 3-10  
 Saturation Temperature Table for N-Butane  
 Calculated from Starling's Equation of State

Table 3-10 (continued)

Table 3-10 (continued)

### THERMODYNAMIC PROPERTIES OF N-BUTANE AS PREDICTED BY STARLING'S EQUATION OF STATE

Table 3-10 (continued)

Table 3-10 (continued)

Table 3-10 (continued)

\*The lack of values for entropy and enthalpy departures and for specific heat references does not permit an accurate calculation of the shown thermodynamic properties in this temperature range.

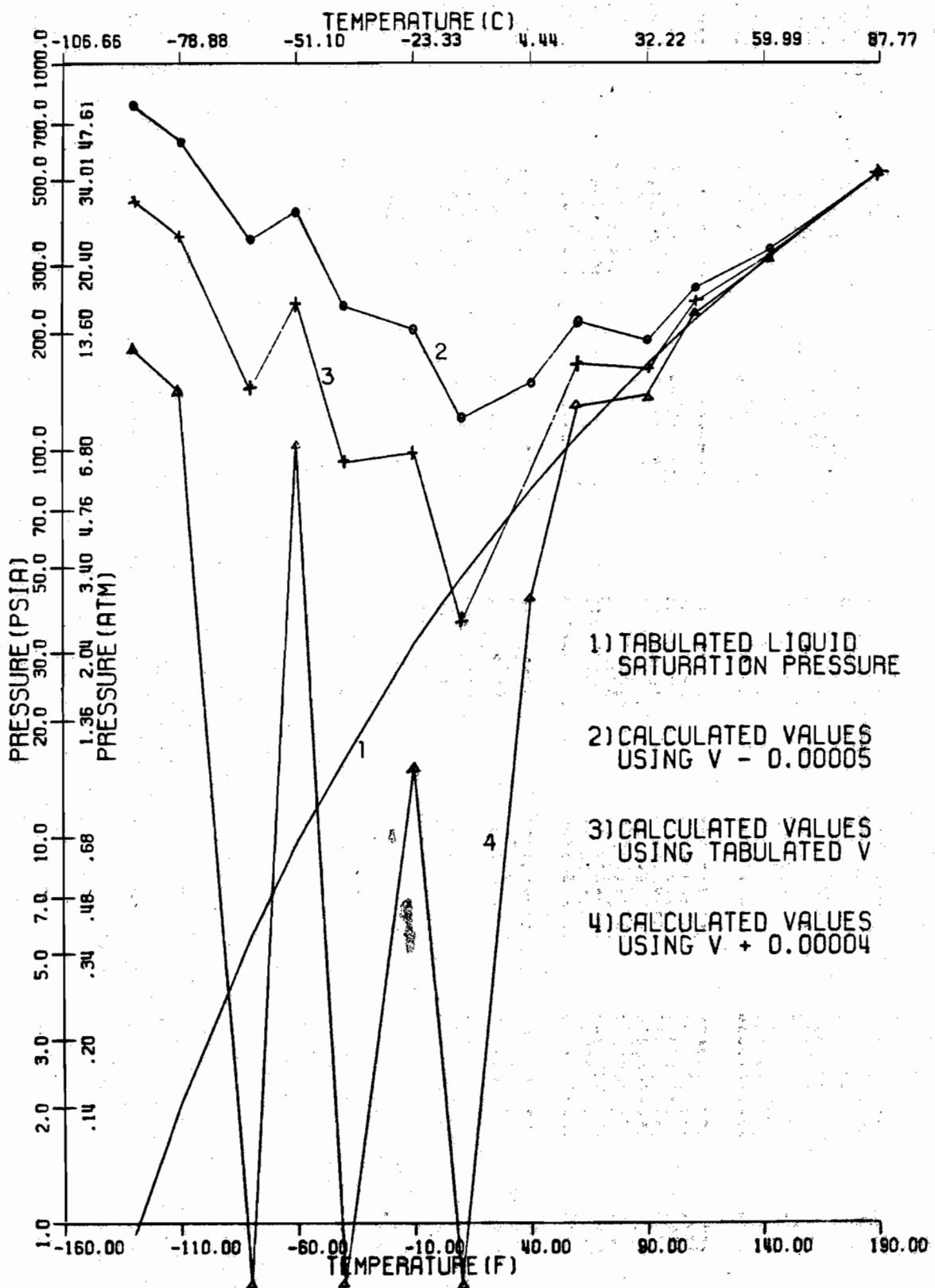


Figure 3-1. Saturation Pressures vs. Saturation Temperatures

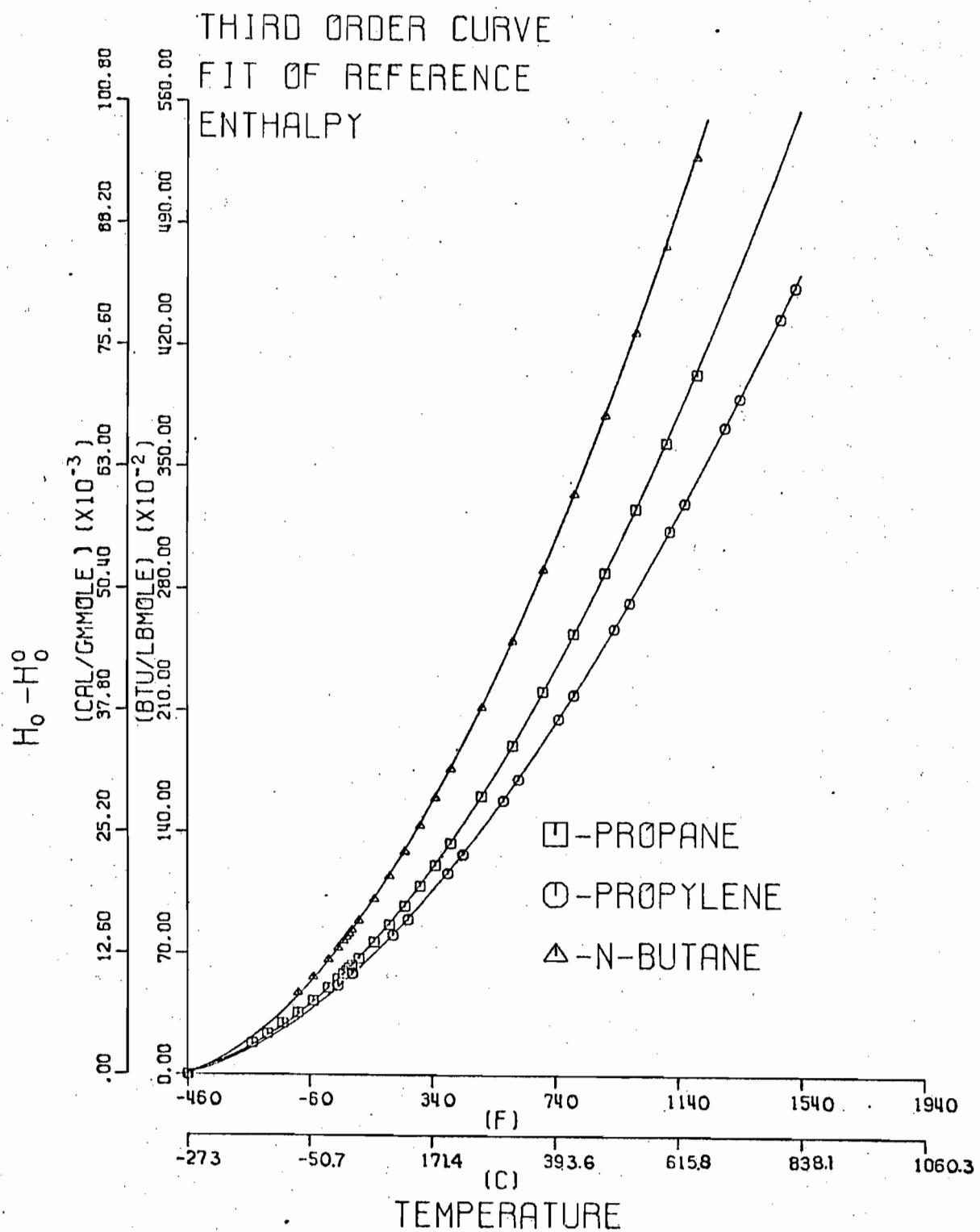


Figure 3-2a. Enthalpy Departures as a Function of Temperature for Propane, Propylene, and N-Butane.

NINTH ORDER CURVE  
FIT OF REFERENCE  
ENTHALPY

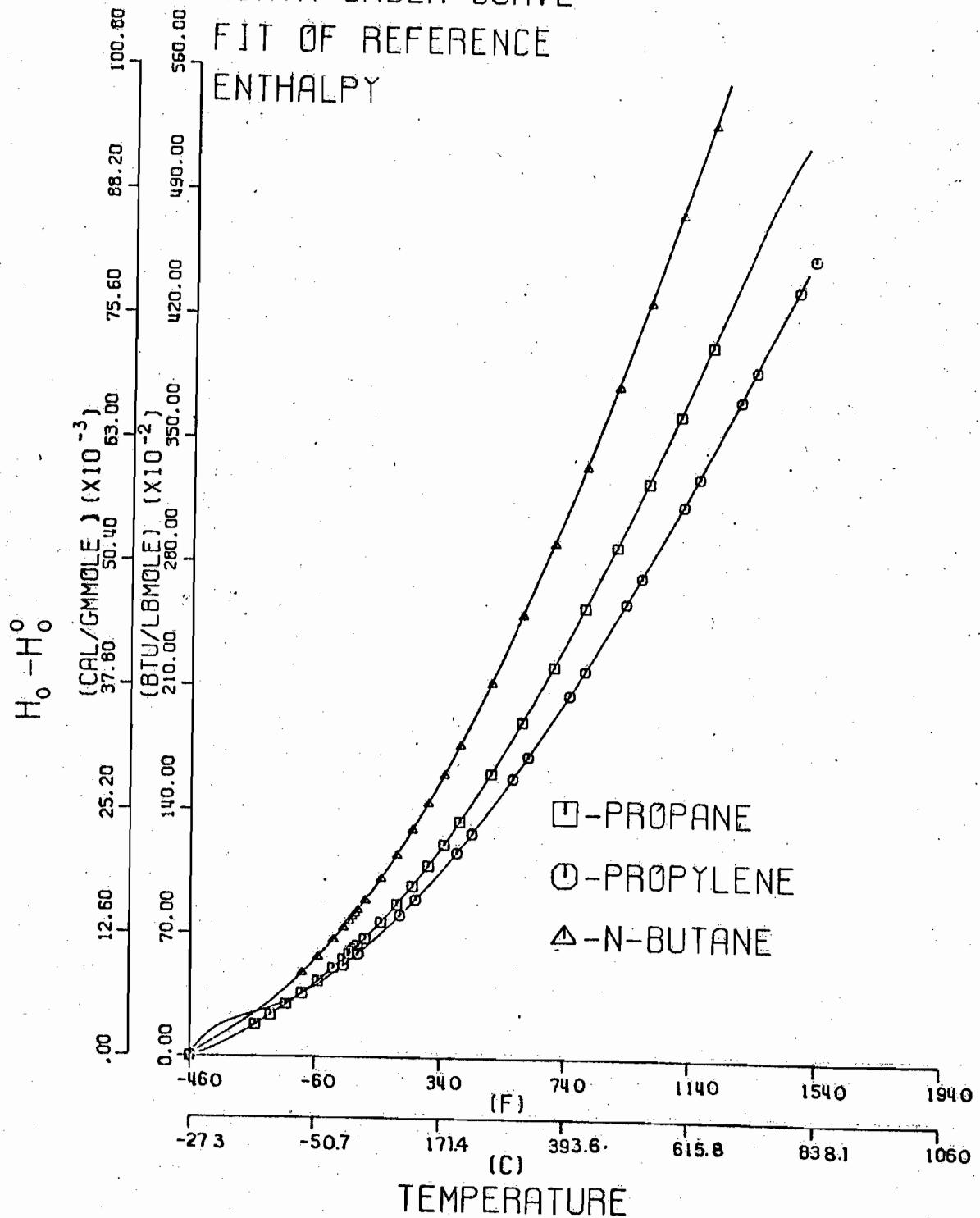


Figure 3-2b. Enthalpy Departures as a Function of Temperature for Propane, Propylene, and N-Butane.

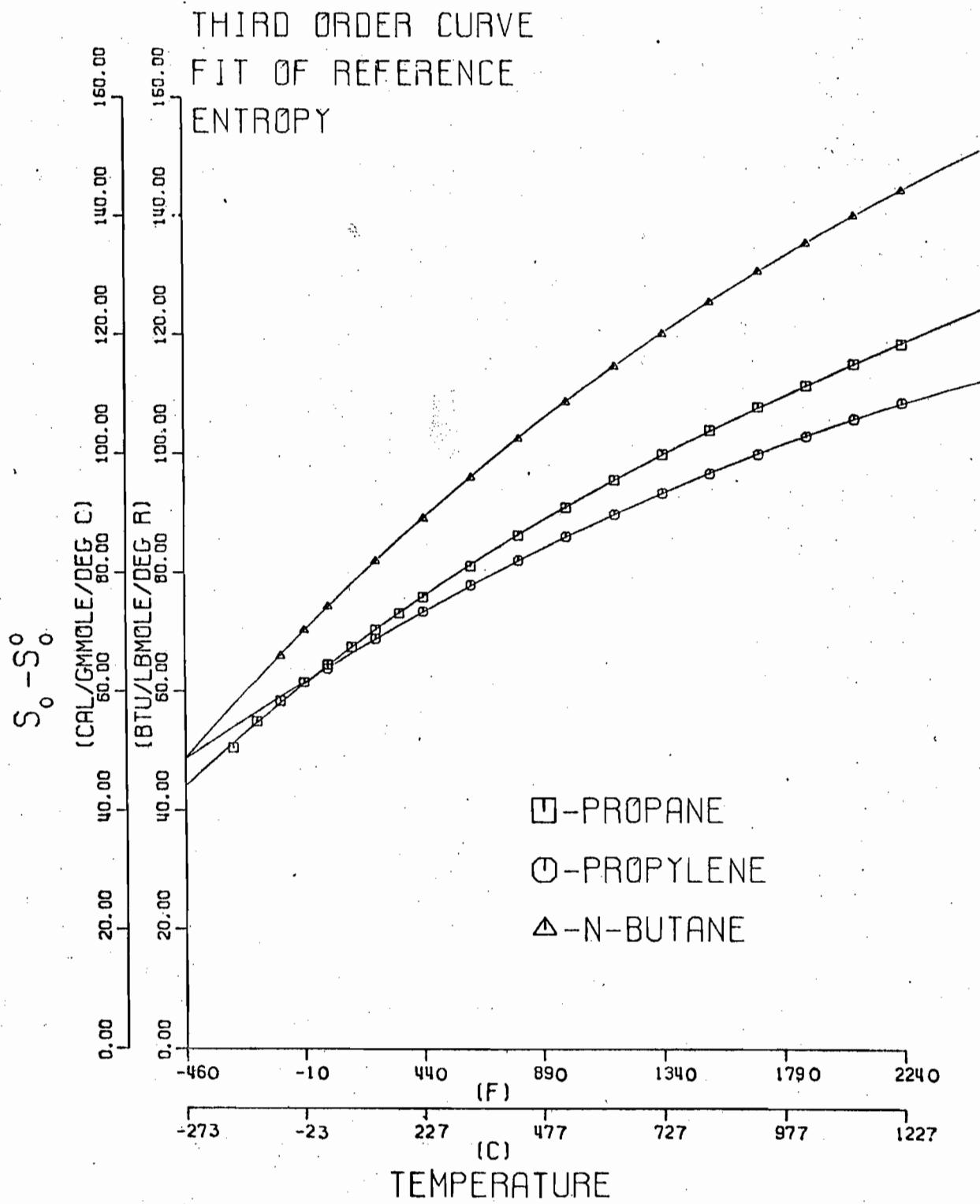


Figure 3-3a. Entropy Departures as a Function of Temperature for Propane, Propylene, and N-Butane.

NINTH ORDER CURVE  
FIT OF REFERENCE  
ENTROPY

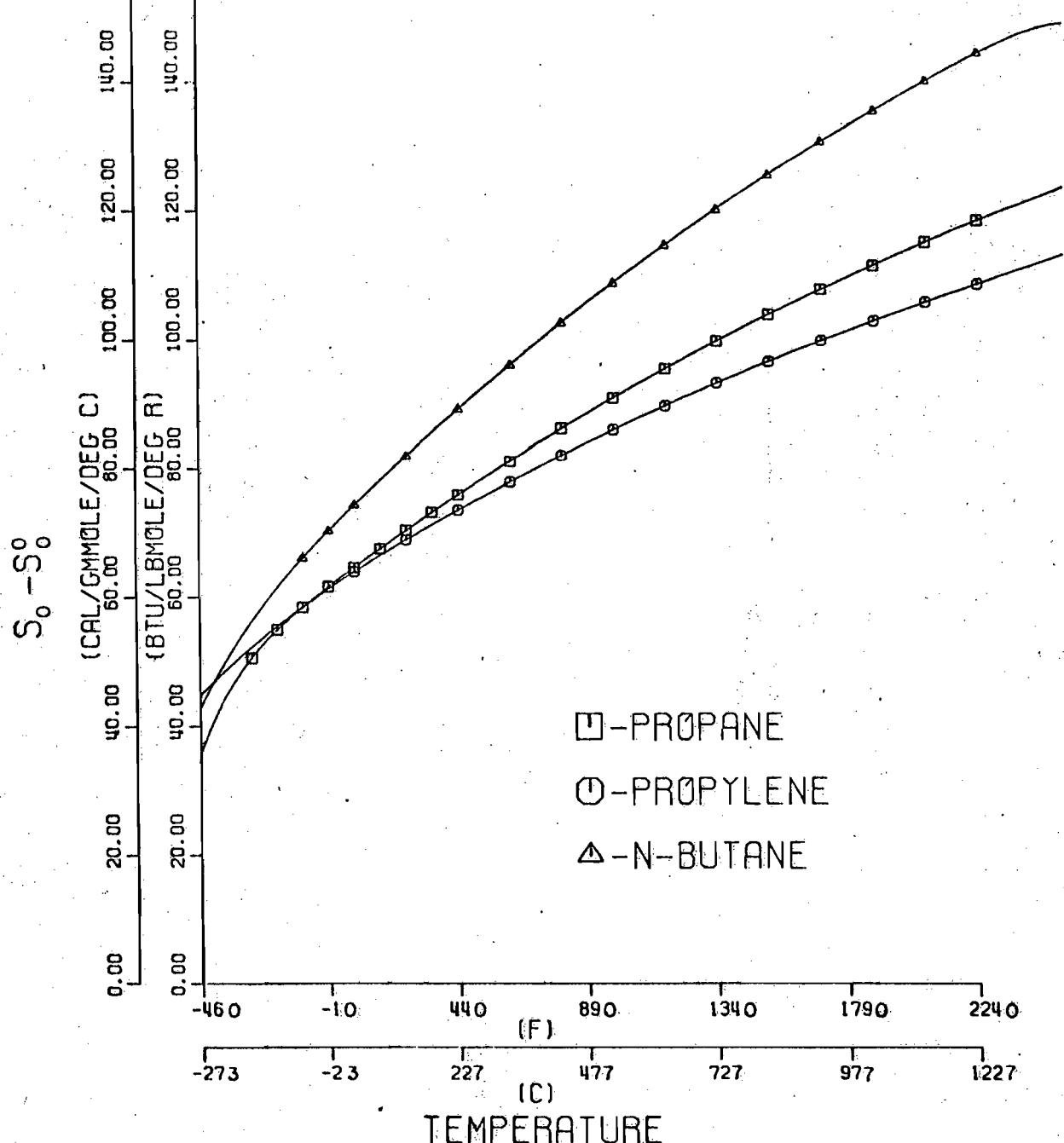


Figure 3-3b. Entropy Departures as a Function of Temperature for Propane, Propylene, and N-Butane.

THIRD ORDER CURVE  
FIT OF REFERENCE  
SPECIFIC HEAT

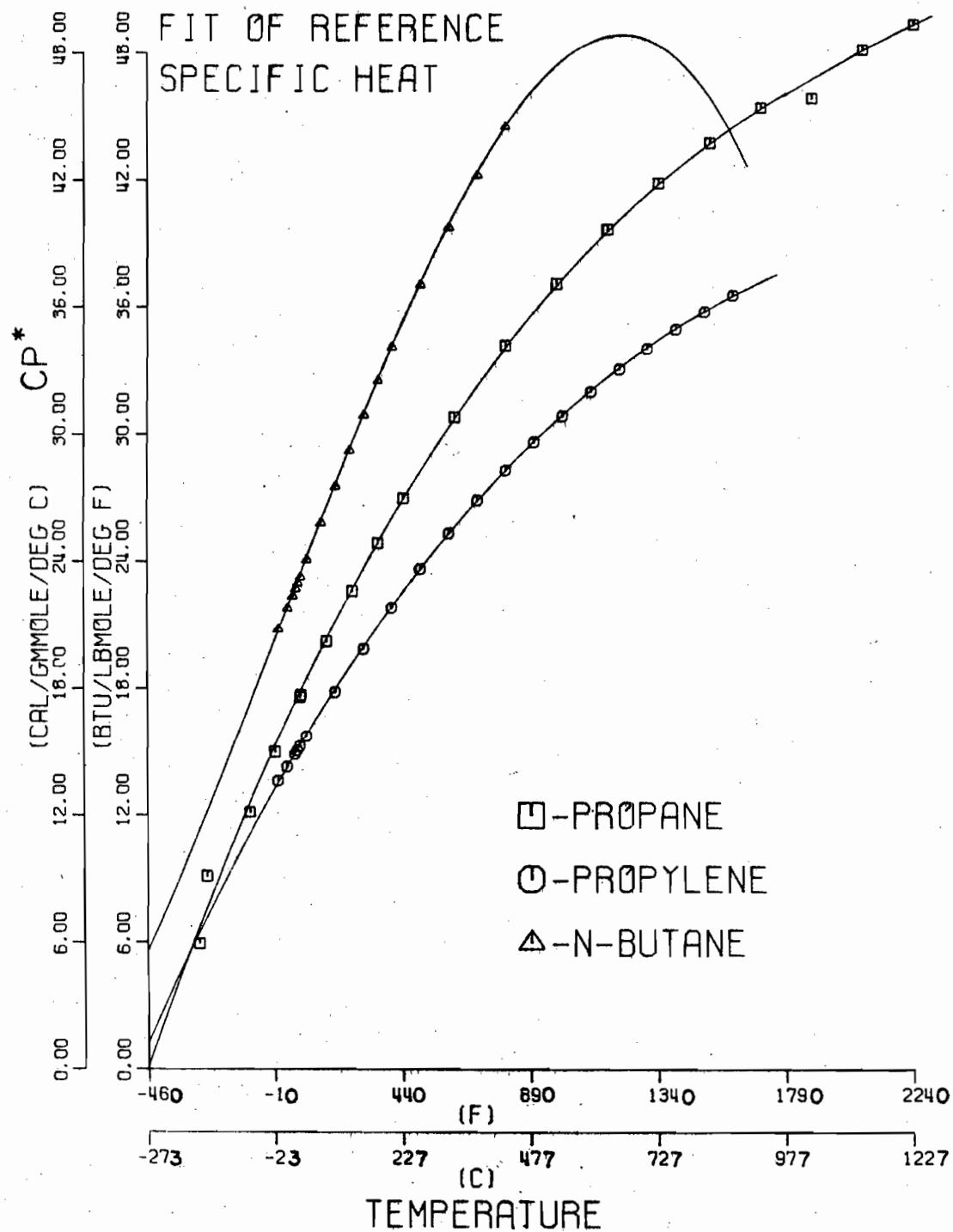


Figure 3-4a. Specific Heat Reference Values as a Function of Temperature for Propane, Propylene, and N-Butane

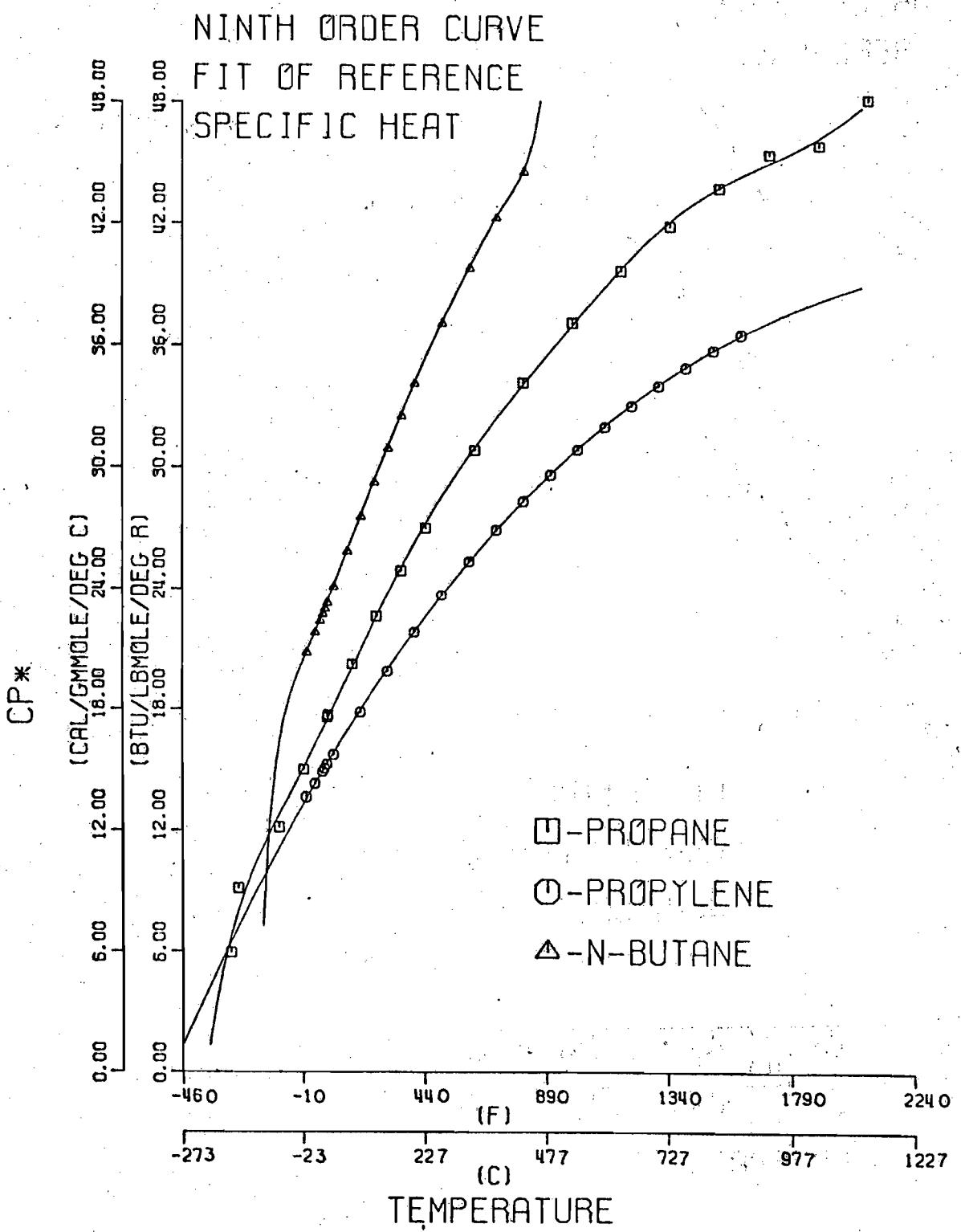


Figure 3-4b. Specific Heat Reference Values as a Function of Temperature for Propane, Propylene, and N-Butane

Figure 3-5. Temperature-Entropy Diagram for Propane  
Based on the Benedict-Webb-Rubin Equation of State

# TEMPERATURE-ENTROPY FOR PROPANE AS GIVEN BY BWR EQUATION

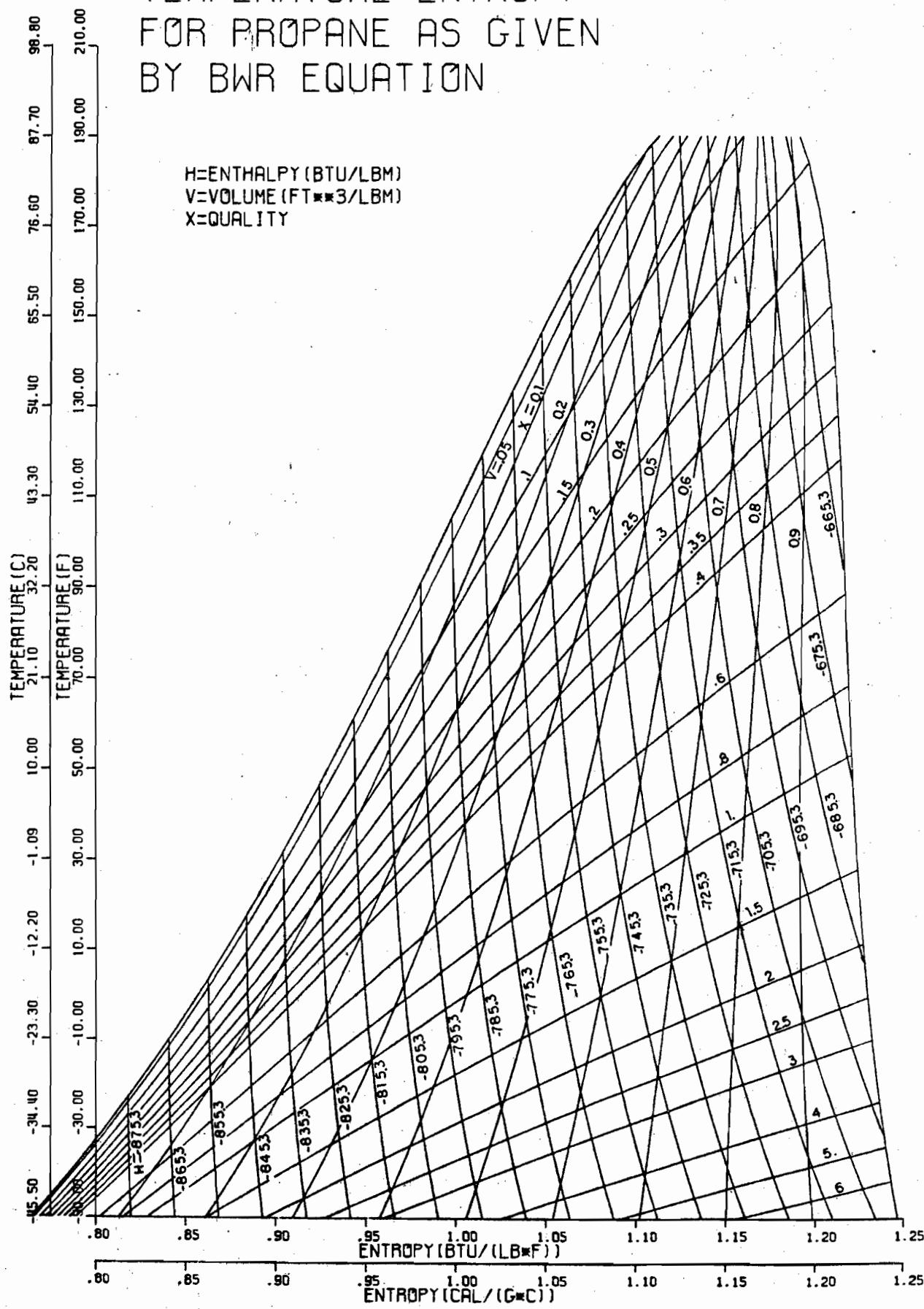


Figure 3-6. Temperature-Entropy Diagram for Propane  
Based on Starling's Equation of State

# TEMPERATURE-ENTROPY FOR PROPANE AS GIVEN BY STARLING'S EQUATION

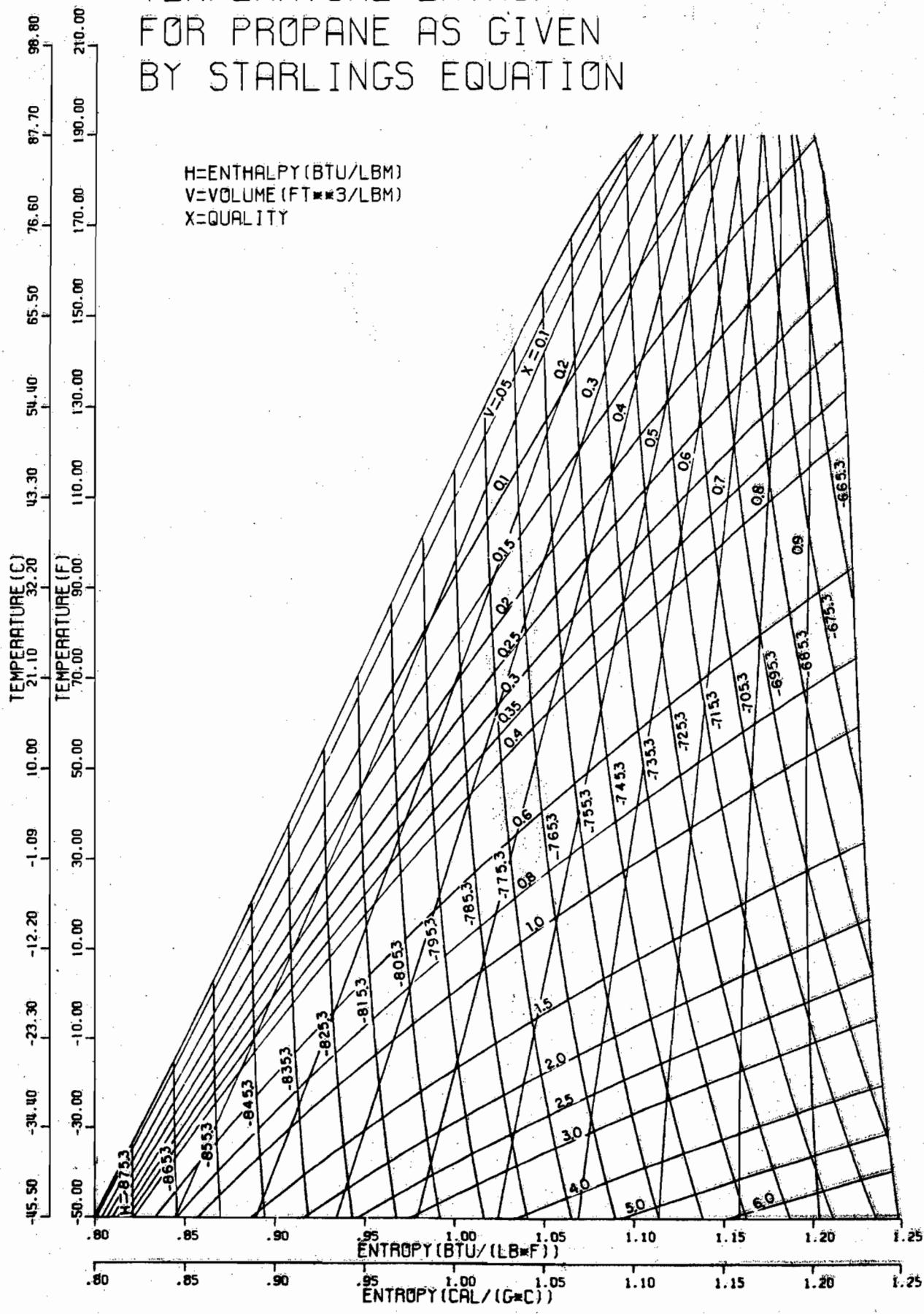


Figure 3-7. Temperature-Entropy Diagram for Propane Based on the Thermodynamic Data Given by Stearns and George

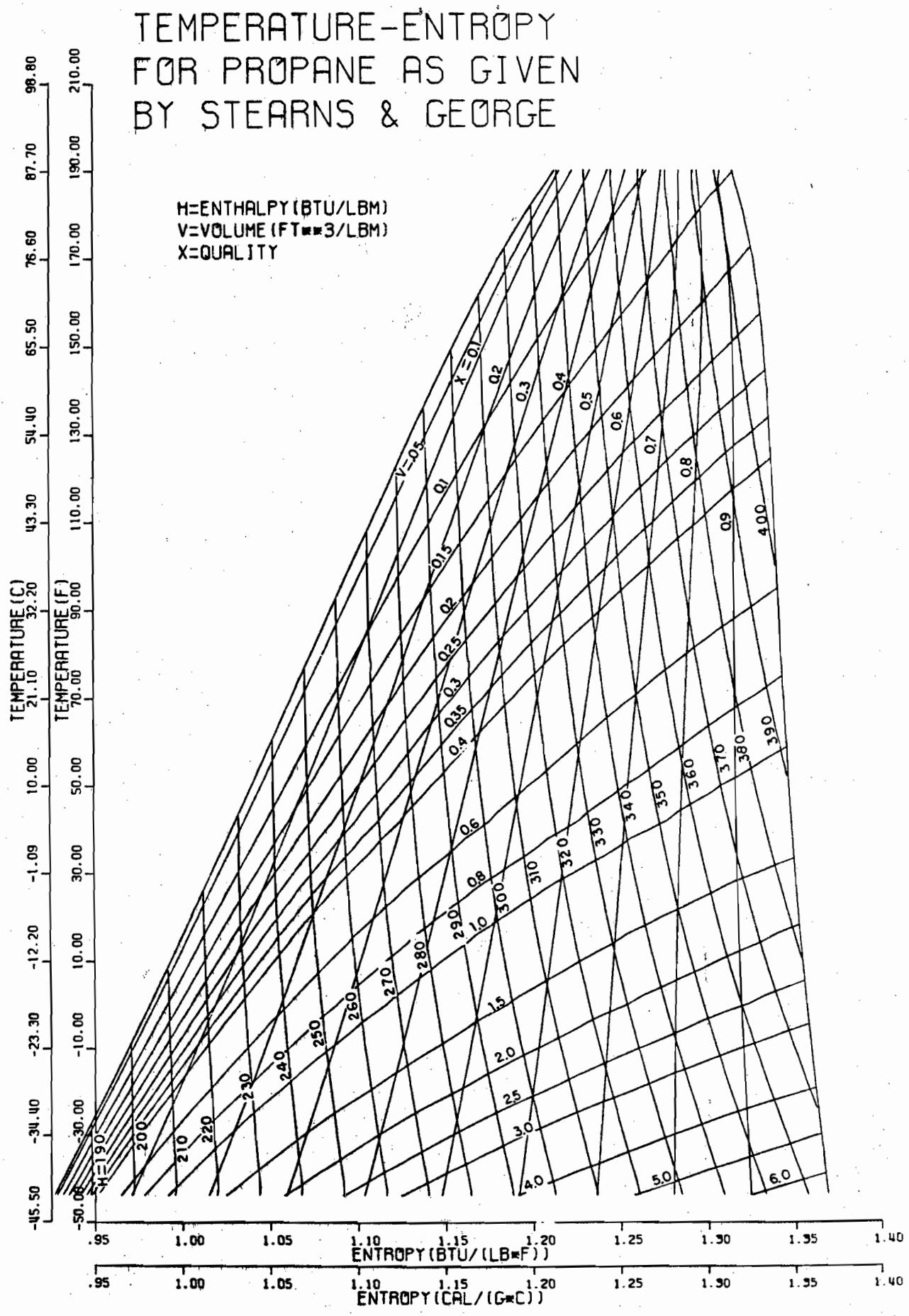


Figure 3-8. Temperature-Entropy Diagram for the Pseudo-Fluid;  
65% by Mole Propane, 25% Propylene, 10% N-Butane,  
Based on Starling's Equation of State

TEMPERATURE-ENTROPY  
FOR PROPANE-PROPYLENE-N-BUTANE  
MIXTURE, (65-25-10), AS GIVEN  
BY STARLINGS EQUATION

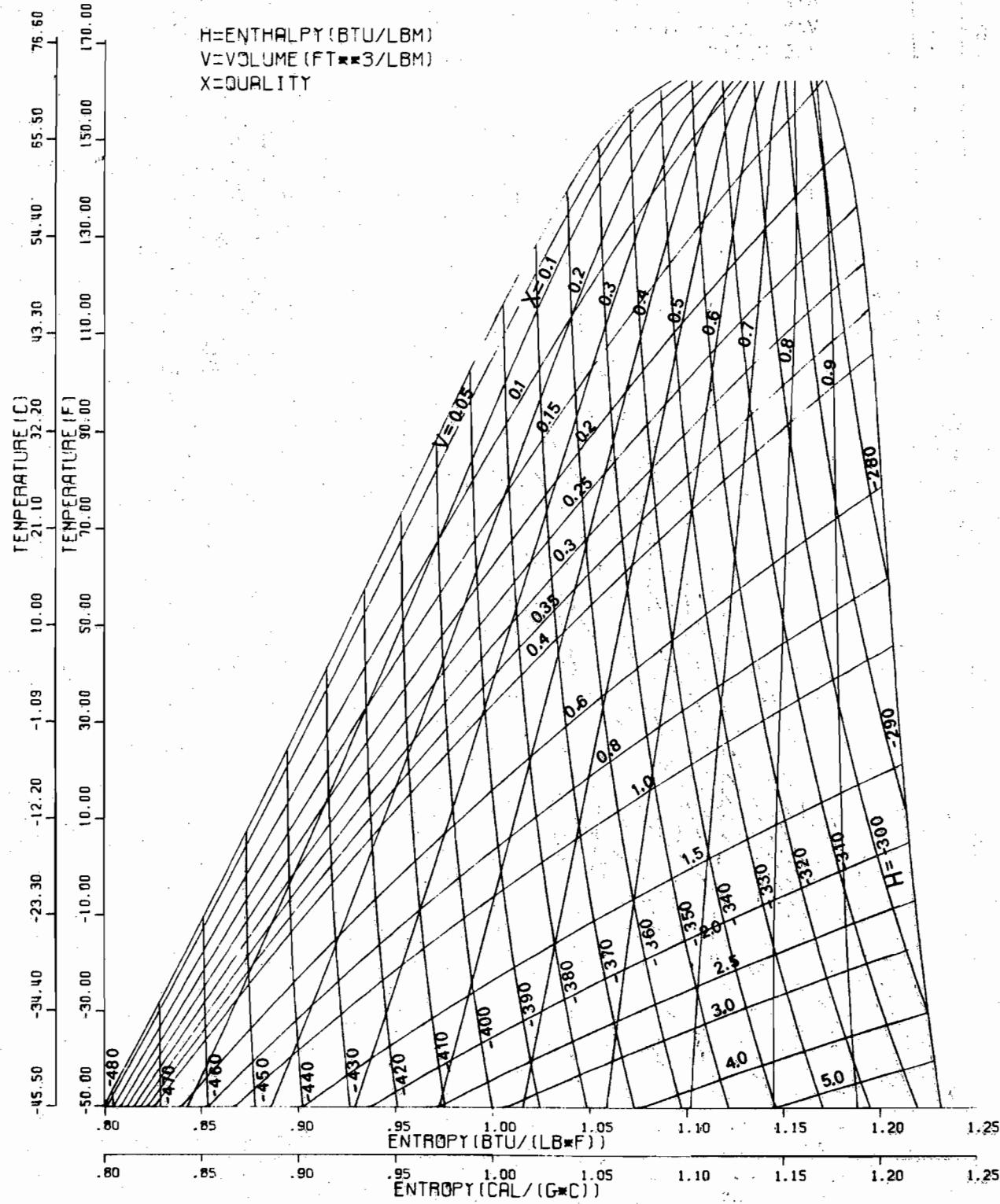
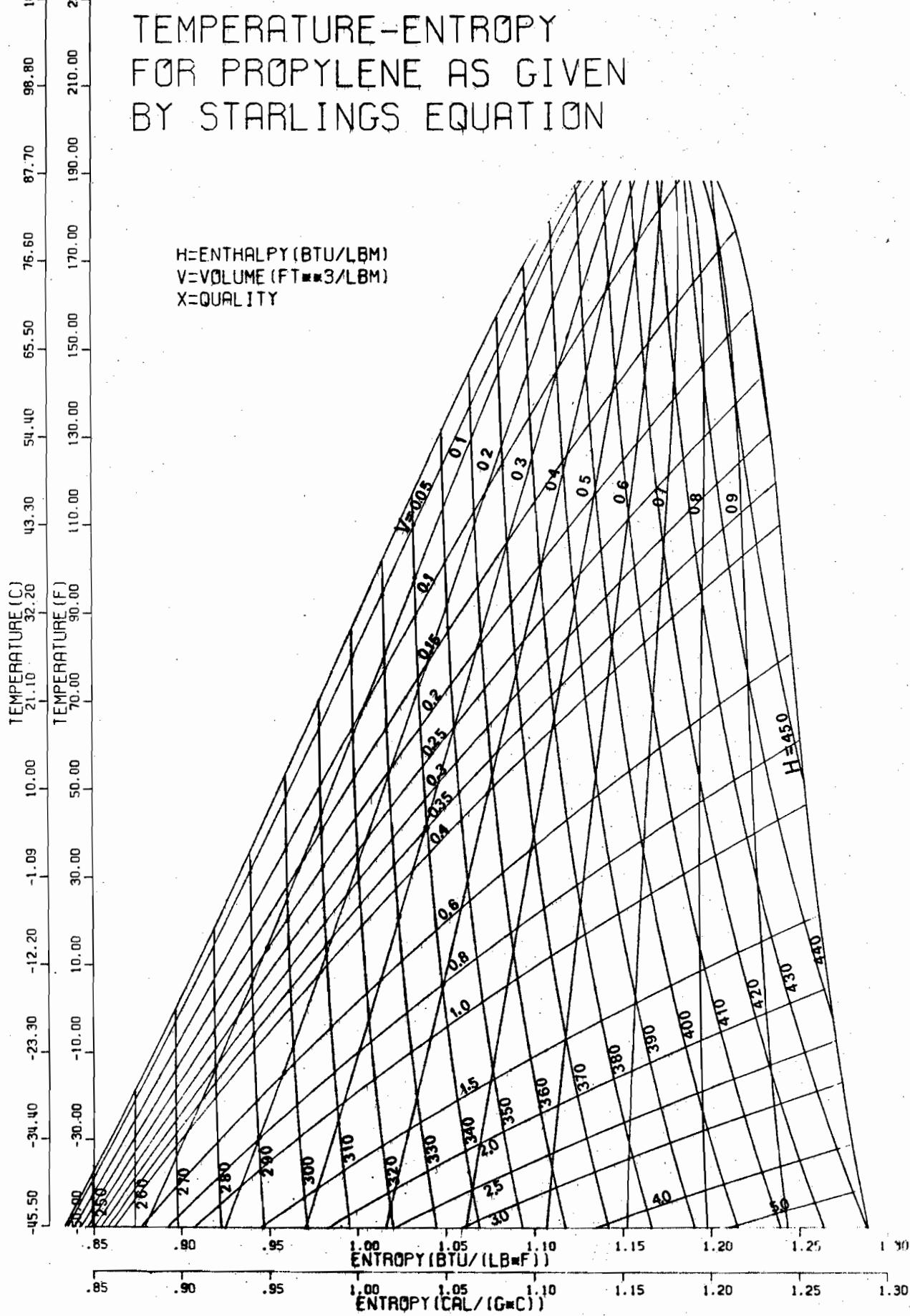


Figure 3-9. Temperature-Entropy Diagram for Propylene  
Based on Starling's Equation of State



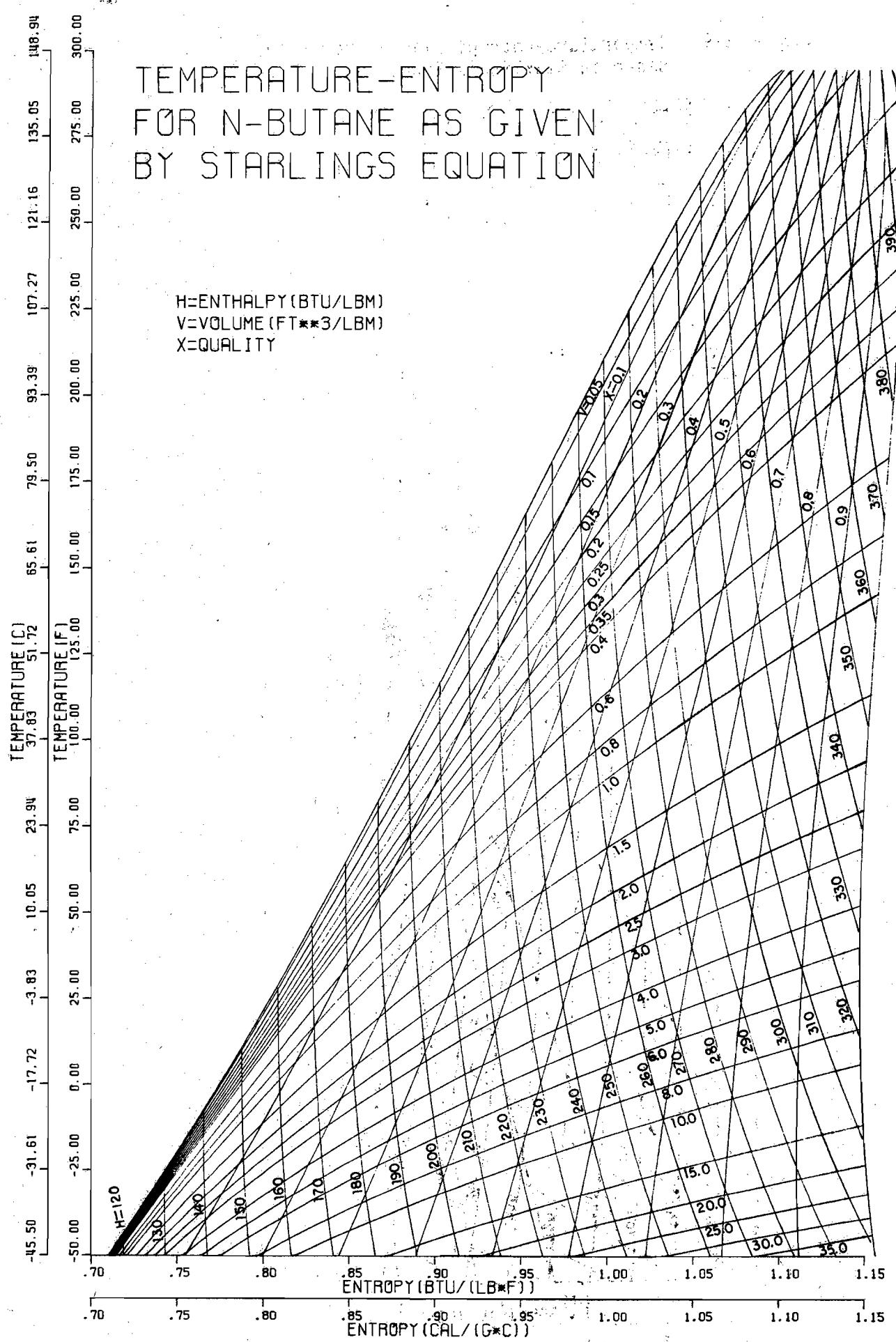


Figure 3-10. Temperature-Entropy Diagram for N-Butane Based on Starling's Equation of State

Chapter 4. Mass Flow Rates of Pure Propane --  
Homogenous Isentropic Flow

This chapter on the mass flow rates of propane was added to this report in order to demonstrate the importance of accurate thermodynamic data for the prediction of mass flow rates. This chapter is not a final report on the prediction of mass flow rates for homogenous isentropic propane flow.

The mass flow rate per unit area (mass flux) for homogenous, adiabatic flow (no slip between the phases, the phases are in thermal equilibrium) can be shown to be:

$$G_C = \sqrt{2g_C J \frac{H_0 - H}{V^2}} \quad (4-1)$$

where  $H_0$  is the stagnation enthalpy,  $H$  is the enthalpy at the critical section (in this case approximated by the smallest cross-section occurring in the valve) and  $V$  is the specific volume of the medium at the critical section. In applying equation (4-1) to calculate the mass flow rates shown in this report, an isentropic process was assumed. It should be pointed out that when slip between the liquid and vapor occurs more information about the flow is needed, such as the slip ratio  $K$ . An energy approach will then yield, for instance, the following expression for the mass flux:

$$G_C = \sqrt{\frac{2G_C J \left[ H_0 - H_\ell - \frac{H_g}{S_{\ell g}} (S_0 - S_\ell) \right]}{\left[ \frac{K(S_g - S_0)V_f}{S_{\ell g}} + \frac{(S_0 + S_\ell)V_g}{S_{\ell g}} \right]^2 \left[ \frac{S_0 - S_\ell}{S_{\ell g}} + \frac{S_g - S_0}{S_{\ell g} K^2} \right]}} \quad (4-2)$$

Figure 4-1, 4-3, 4-5, and 4-7 give predicted mass flow rates per unit area at the critical valve section (Critical Mass Flux) based on the customary thermodynamic propane data by Stearns and George, while Figures 4-2, 4-4, 4-6, and 4-8 repeat the same calculations using a virial equation of state for propane (Starling's equation with entropy and enthalpy departures reevaluated by Sallet-Wu, as discussed in Chapter 3). In all shown prediction results (Figures 4-1 to 4-8) homogenous, isentropic flow in thermal equilibrium was assumed. The upstream stagnation condition for the flow calculation shown in

Figures 4-1 through 4-4 was assumed to be saturated liquid. Comparing Figures 4-1 4-3, 4-5, and 4-7 with Figures 4-2, 4-4, 4-6, and 4-8 in general, one finds that the flow rate predictions calculated with Starling's equation is much more consistent and, reasoning with one-phase fluid dynamics, i.e., higher pressures give higher mass flow rates, appear to be correct.

Figure 4-2 shows critical mass flux as a function of critical section pressure, with the upstream (saturated liquid) pressure as a parameter. For example, for saturated liquid propane (pure propane, for mixtures see the last paragraph below) which is at a stagnation pressure of 353.22 psia the maximum critical mass flux (point 1 in Figure 4-2) is approximately  $2500 \text{ lb}/(\text{ft}^2\text{-sec})$ . This represents the maximum mass flow rate through the valve only if the pressure at the smallest cross sectional area in the valve is approximately 275 psia. If this critical section pressure is smaller or larger, the maximum mass flow rate through the valve for the given upstream stagnation condition (353.22 psia) will be smaller. For example, if the critical section pressure which establishes itself in the valve is 200 psia, then the maximum mass flux through the valve will drop to approximately  $2250 \text{ lb}/(\text{ft}^2\text{-sec})$ , as shown by point 2. The above quantitative example shows the importance of the critical section pressure.

Critical section pressure for a given valve is, however, not a constant which could be obtained from the pressure ratio across the valve for any fluid flow. The following question now becomes of practical importance: What is the maximum mass flow rate for liquid propane, assuming the appropriate critical section pressure does exist? This question can be answered by using the results plotted in Figure 4-4. For example, if the pressure in the tank is 400 psia, then the maximum liquid propane mass flow rate per unit area is  $2700 \text{ lb}/(\text{ft}^2\text{-sec})$ . Again it is pointed out that these results are obtained from homogenous isentropic, equilibrium flow theory. All of these assumptions will be carefully examined before final flow rate prediction equations will be published.

Figures 4-6 and 4-8 show how the maximum mass flow rates per unit area change if the reservoir conditions go from saturation liquid (quality equals 0.00) to saturated vapor (quality equals 1.00). Again homogenous, isentropic flow in thermal equilibrium was assumed. While the flow rates shown in Figures 4-6 and 4-8 were calculated using Starling's equation of state (as reevaluated by Sallet-Wu, see Chapter 3), the curves shown in Figures 4-5 and 4-7 are based upon the thermodynamic data by Stearns and George.

As was pointed out during the course of this discussion, the flow calculations given are only valid for pure propane. Mass flow rates of mixtures of propane, butane and propylene resembling commercial propane are currently being calculated. Preliminary results will be available by the time the reader reads this report. A detailed discussion on homogenous mass flow rates will be given in the Final Report of the Safety Valve Study.

## CALCULATED MASS FLOW RATES OF PROPANE

BASED ON THE THERMODYNAMIC PROPERTIES  
GIVEN BY STEARNS & GEORGE

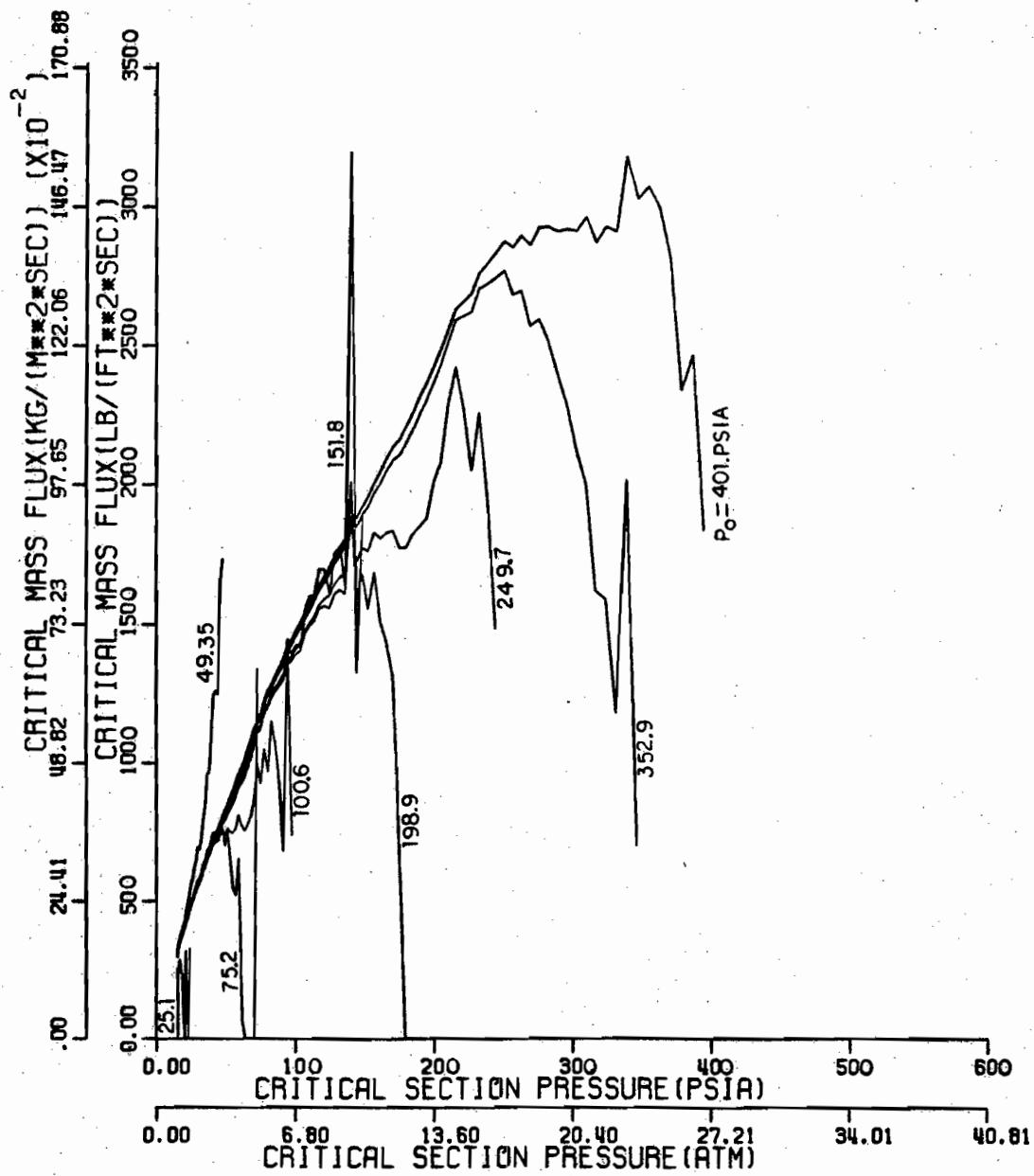


Figure 4-1. Critical Mass Flux of Propane as a Function of Critical Section Pressure (Based on Thermodynamic Data Given by Stearns and George)

CALCULATED MASS FLOW RATES OF PROPANE  
BASED ON STARLING'S EQUATION

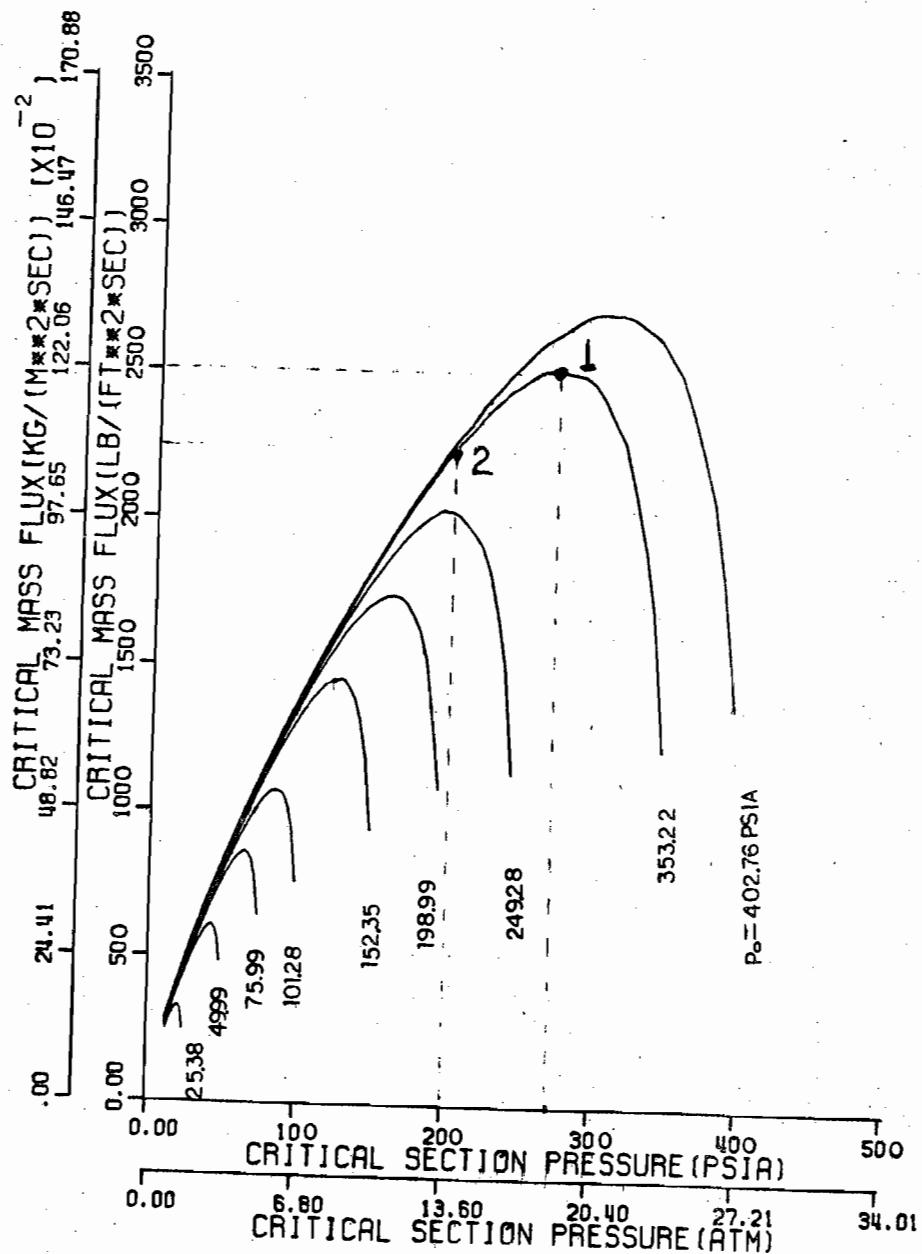


Figure 4-2. Critical Mass Flux of Propane as a Function of Critical Section Pressure (Based on Thermodynamic Data Calculated with Starling's Equation)

CALCULATED MASS FLOW RATES OF PROPANE  
BASED ON THE THERMODYNAMIC PROPERTIES  
GIVEN BY STEARNS & GEORGE

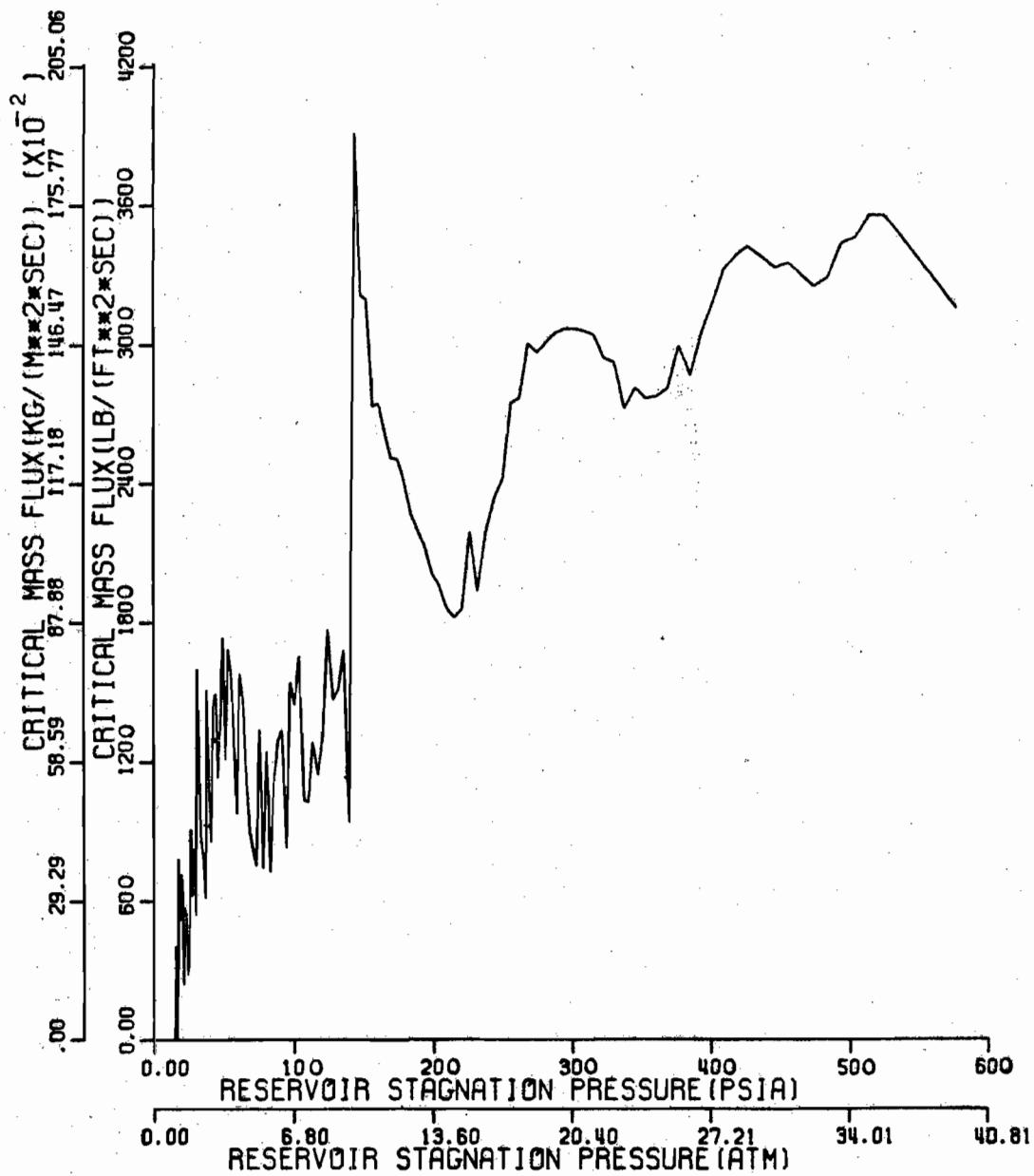


Figure 4-3. Maximum Critical Mass Flux of Propane as a Function of Reservoir Stagnation Pressure (Based on Thermodynamic Data Given by Stearns and George)

CALCULATED MASS FLOW RATES OF PROPANE  
BASED ON STARLING'S EQUATION

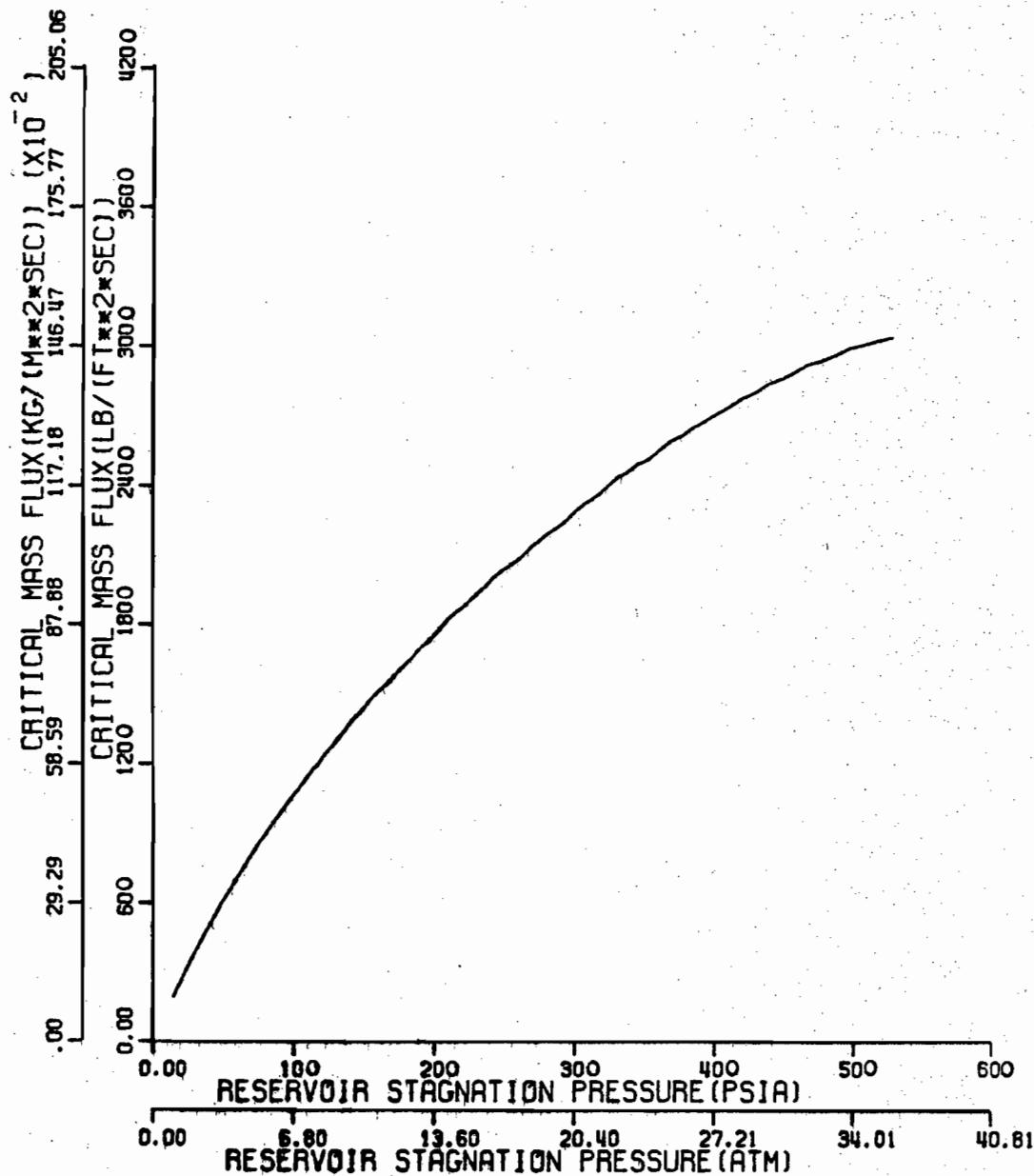


Figure 4-4. Maximum Critical Mass Flux of Propane as a Function of Reservoir Stagnation Pressure (Based on Thermodynamic Data Calculated with Starling's Equation)

CALCULATED MASS FLOW RATES OF PROPANE  
BASED ON THE THERMODYNAMIC PROPERTIES  
GIVEN BY STEARNS & GEORGE

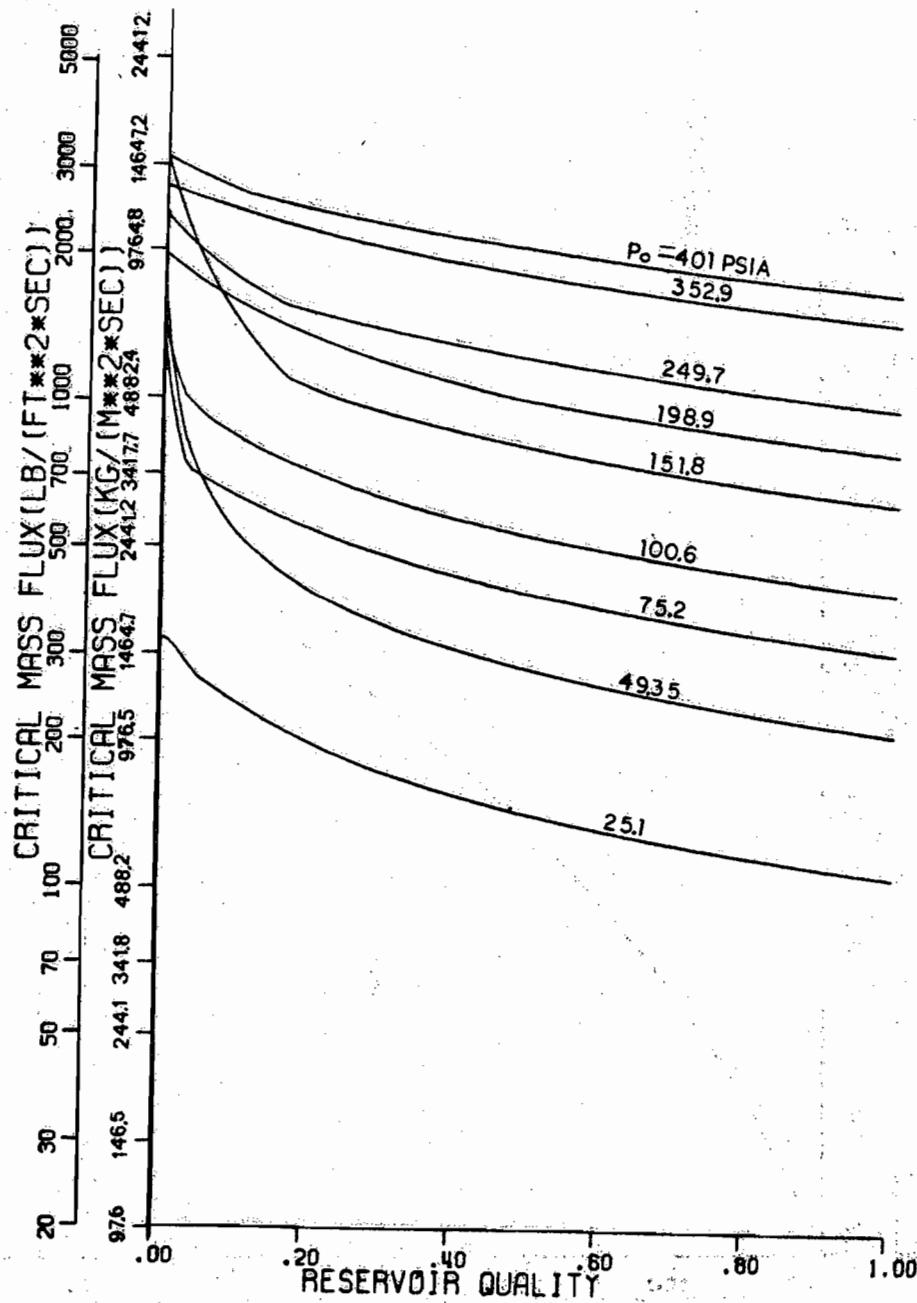


Figure 4-5. Maximum Critical Mass Flux of Propane as a Function of Reservoir Quality (Based on Thermodynamic Data Given by Stearns and George)

CALCULATED MASS FLOW RATES OF PROPANE  
BASED ON STARLING'S EQUATION

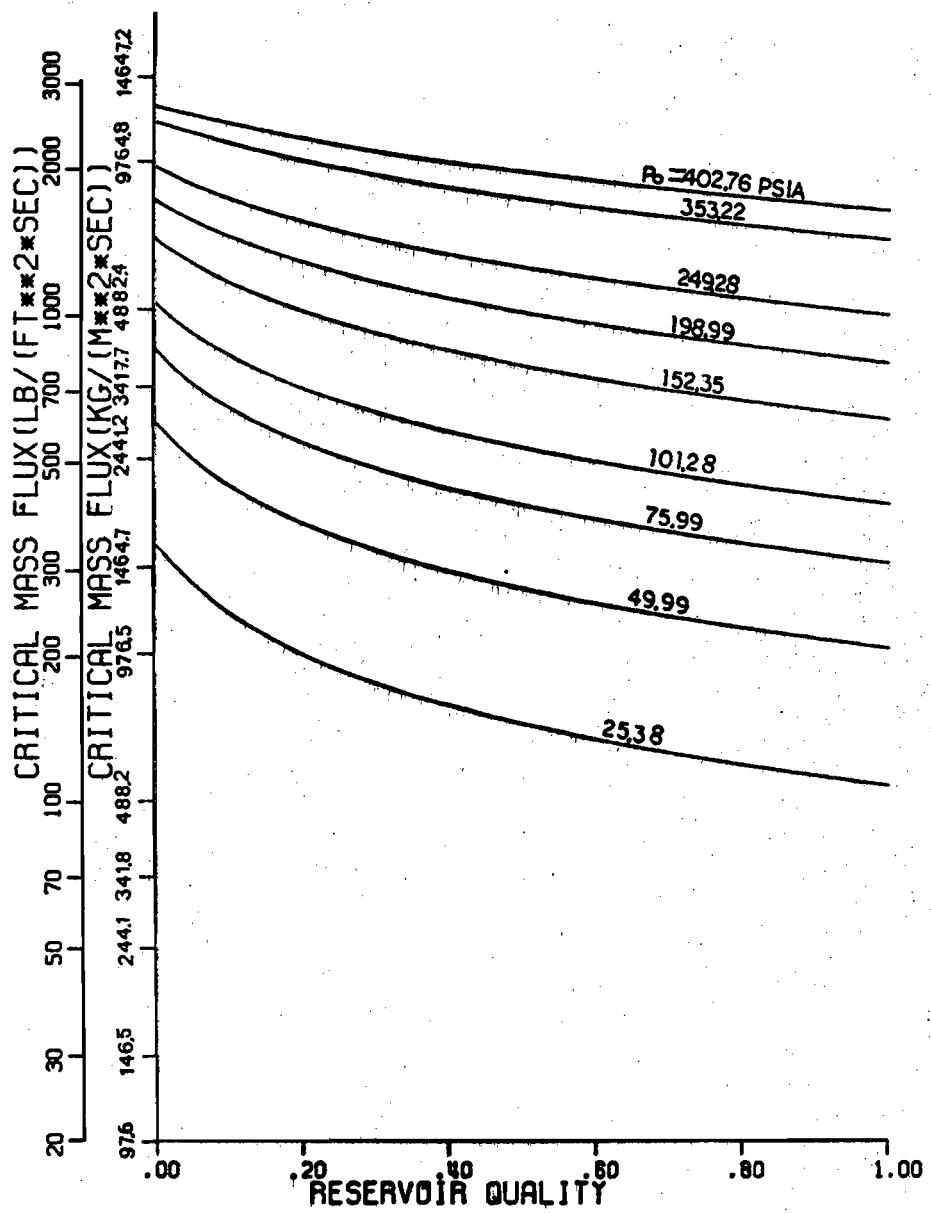


Figure 4-6. Maximum Critical Mass Flux of Propane as a Function of Reservoir Quality (Based on Thermodynamic Data Calculated with Starling's Equation)

CALCULATED MASS FLOW RATES OF PROPANE  
BASED ON THE THERMODYNAMIC PROPERTIES  
GIVEN BY STEARNS & GEORGE

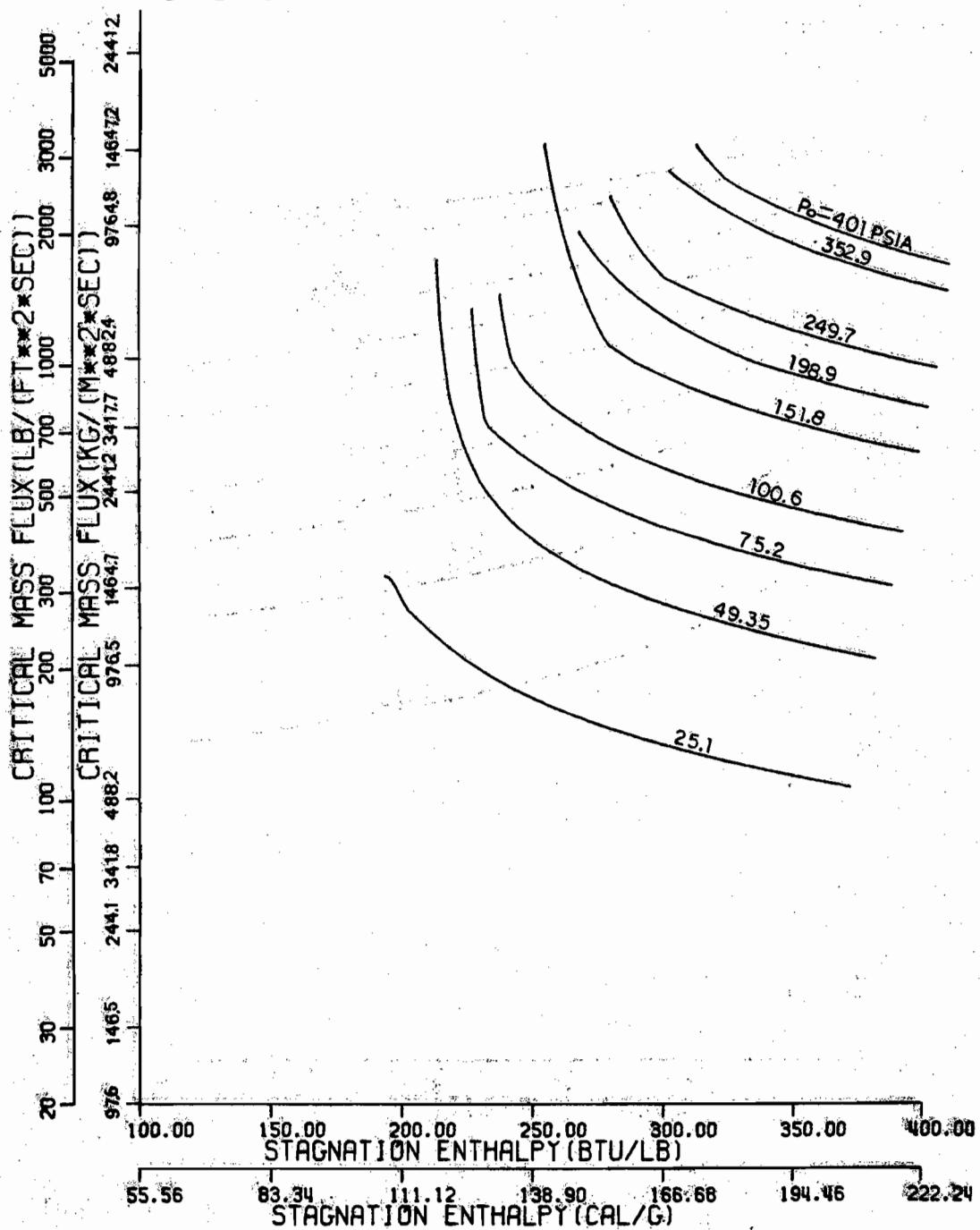


Figure 4-7. Maximum Critical Mass Flux of Propane as a Function of Stagnation Enthalpy (Based on Thermodynamic Data Given by Stearns and George)

CALCULATED MASS FLOW RATES OF PROPANE  
BASED ON STARLING'S EQUATION

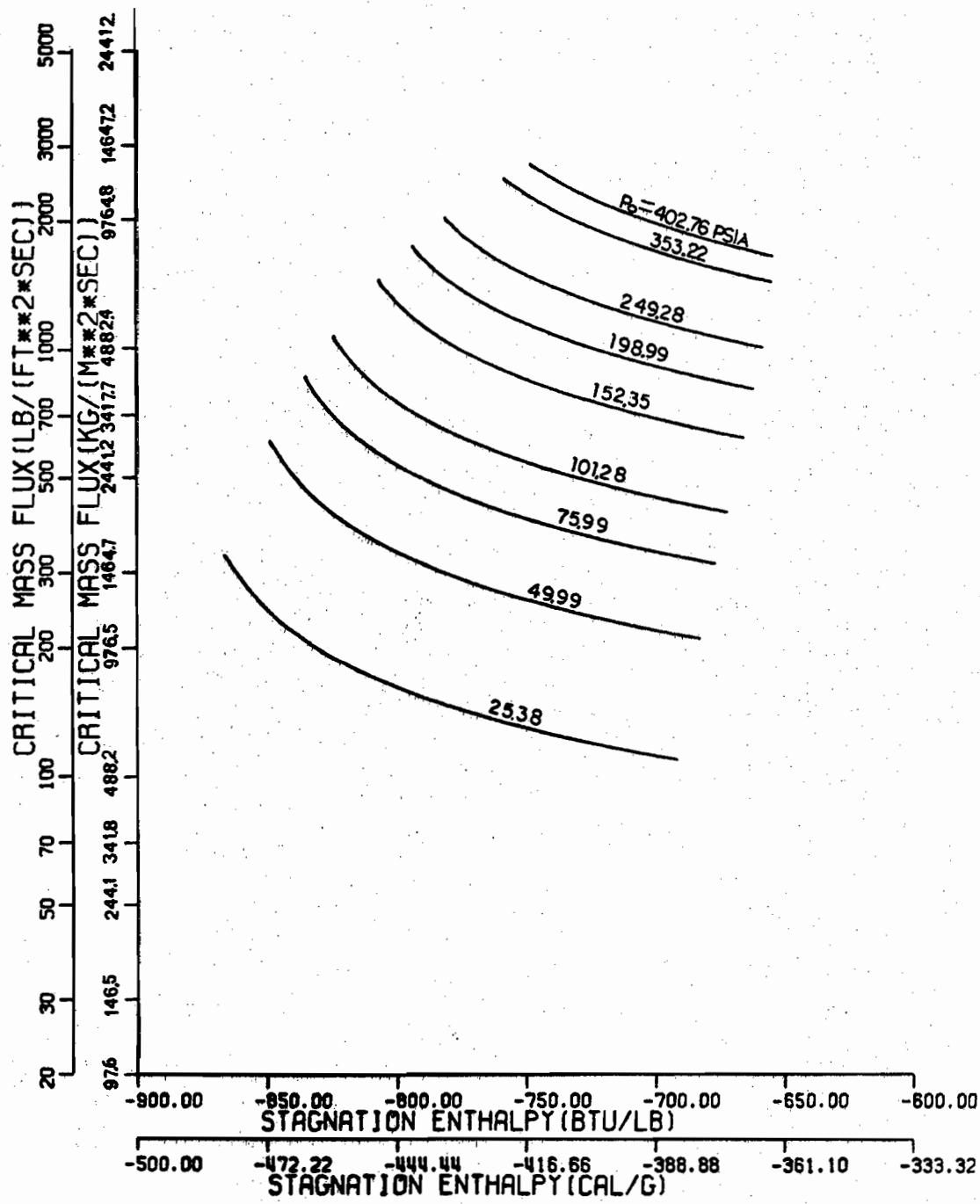


Figure 4-8. Maximum Critical Mass Flux of Propane as a Function of Stagnation Enthalpy (Based on Thermodynamic Data Calculated with Starling's Equation)

## Chapter 5. Conclusions

Mass flow rate calculations for propane are very sensitive to the thermodynamic data upon which the calculations are based. Mass flow rates predicted using Stearns and George's data differ for certain conditions by more than 100% from the predictions based on Starling's or Benedict-Webb-Rubin's equation of state. Because of its good agreement with experimentally measured values on the vapor dome as well as in the subcooled liquid region and because the consistent nature of the mass flow rates which are based upon its result the Starling equation of state should be used for the thermodynamic data of pure propane and propane mixtures.

A major difficult and source of inaccuracy in calculating thermodynamic properties from a virial equation of state such as the Benedict-Webb-Rubin equation or Starling's equation is posed by the introduction of enthalpy and entropy departures and reference values for the specific heat. Great care was taken in the present investigation to correctly interpolate between the given values by using numerical curve fitting techniques. Because of the lack of data for entropy departures of propylene below 80°F and for enthalpy departures of propylene below 32°F (other than the zero points dictated by the third law of thermodynamics) the thermodynamic data of propylene and of the propane mixture which contains propylene may be incorrect at temperatures below 80°F. The enthalpy values are likely to be accurate down to a temperature of 32°F. A continuation of the present work on the thermodynamics of propane is strongly urged.

## References

1. Rossini, F. D., Selected Values of Physical and Thermodynamic Properties of Hydrocarbons and Related Compounds, published for the American Petroleum Institute, Carnegie Press, Pittsburgh, Pennsylvania, 1953, 1050 pages.
2. Beattie, J. A., W. Kay, and J. Kaminsky, "The Compressibility of an Equation of State for Gaseous Propane," Journal of the American Chemical Society, Vol. 59 (1937), pp. 1589-1590.
3. Beattie, J. A., N. Poffenberger, and C. Hadlock, "The Critical Constants of Propane," Journal of Chemical Physics, Vol. 3 (1935), pp. 96-97.
4. Benedict, M., G. W. Webb, and L. C. Rubin, "An Empirical Equation for Thermodynamic Properties of Light Hydrocarbons and Their Mixtures," Journal of Chemical Physics, Vol. 8 (1940), pp. 334-345.
5. Burgoyne, J. H., "Two-Phase Equilibrium in Binary and Ternary Systems," Proceedings Royal Society (London), Vol. A176 (1940), pp. 280-294.
6. Dana, L. I., A. C. Jenkins, J. W. Burdick, and R. C. Timm, "Thermodynamic Properties of Butane, Isobutane, and Propane," Refrigerating Engineering, Vol. 12 (1926), pp. 387-405.
7. Mayer, J., "The Statistical Mechanics of Condensing Systems," Journal of Chemical Physics, Vol. 5 (1937), pp. 67-83.
8. Sage, B. H., J. G. Schaafama, and W. N. Lacey, "Phase Equilibrium in Hydrocarbon Systems," Industrial and Engineering Chemistry, Vol. 26, (1934), pp. 1218-1224.
9. Starling, K. E., Fluid Thermodynamic Properties for Light Petroleum Systems, Gulf Publishing Company, Houston, Texas, 1973, 270 pages.
10. Stearns, W. V. and E. J. George, "Thermodynamic Properties of Propane," Industrial and Engineering Chemistry, Vol. 35 (1943), pp. 602-607.
11. Ursell, H. D., "The Evaluation of Gibbs' Phase-Integral for Imperfect Gases," Proceedings Cambridge Philosophical Society, Vol. 23 (1927), pp. 685-697.

